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Impact of processing parameters and post-treatment on the shape accuracy of 3D-printed baking dough

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27 Running Head: Shape accuracy of 3D-printed baking dough

28 **Summary**

29 Apart from the material compositions, processing parameters of a 3D printer also
30 affect the modeling effect of printed samples. This paper presents the influence of
31 processing parameters including filament diameter (2.10, 2.30, 2.50 mm), nozzle
32 movement speed (20, 25, 30 mm/s), nozzle diameter (0.8, 1.5, 2.0 mm) and nozzle
33 height (2.10, 2.40, 2.60 mm), as well as that of post-process fast-cooling (-65 °C; 0, 5,
34 10 min), on the rheological properties and geometric accuracy of a 3D-printed food
35 construct made of baking dough (BD). Results showed that the printed object whose
36 shape best matched the target geometry could be obtained with the following
37 processing parameters: filament diameter of 2.30 mm, nozzle movement speed of 25
38 mm/s, nozzle diameter of 2.0 mm, and nozzle height of 2.40 mm during 3D printing,
39 combined with fast-cooling at -65 °C for more than 10 min after printing and before
40 baking.

41 **Keywords** 3D printing, processing parameters, post-process fast-cooling, modeling effect,
42 rheological properties.

43

44 **Introduction**

45 Three-dimensional printing (3DP) is a new technology that uses computer-
46 assisted layer-by-layer deposition of materials to produce 3D objects (Hao *et al.*,
47 2010). Unique advantages of 3DP include minimal labor and the capacity to
48 manufacture extremely intricate shapes, making it suitable for a wide range of
49 applications, especially in a fast-increasing consumer goods industries such as the
50 food industry (Drury, J. L. & Mooney, D. J., 2003; Galantucci, L., Lavecchia, F. &
51 Percoco, G., 2009; Godoi, F. C., Prakash, S. & Bhandari, B. R., 2016; Li *et al.*, 2015;
52 Tumbleston *et al.*, 2015; Khalil, S. & Sun, W., 2007; Sun *et al.*, 2015; Zoran, A. &
53 Coelho, M., 2011).

54 The demand of food printing has immense growth potential, as it can produce
55 new foods with easily-customizable recipes and complex shapes (Wegrzyn, T. F.,
56 Golding, M. & Archer, R. H., 2012; Yang, F., Zhang, M. & Bhandari, B. R., 2017).
57 The applications of 3DP in food production are fascinating for both the simple
58 production process and the design of nutritional food with innovative textures
59 (Severini, C. & Derossi, A., 2016). In recent years considerable research has focused
60 on the application of 3DP technology, using various food formulations in the design
61 and production of different types of food constructs. For example, bacon fat and
62 transglutaminase were used to enable scallop and turkey meat-puree to be printable
63 and geometrically stable after cooking (Lipton *et al.*, 2010). The possibility of printing
64 cookies that are ready for baking after printing was investigated (Sun *et al.*, 2015). In
65 addition, some groups have explored the possibility of modeling effects of printing
66 parameters on the quality of printed products. For example, a linear relationship
67 between layer height and extrusion rate in 3D chocolate printing was demonstrated
68 (Hao *et al.*, 2010). However, the relationship between different printing parameters
69 was not fully detailed in these previous studies.

70 Two conditions are primarily responsible for the quality of 3D-printed samples:
71 the extruding capacity and the shape retention (Yang, F. *et al.*, 2018). The extruding
72 behavior of 3DP is actually a shear mechanical behavior which relies on rheological
73 properties such as apparent viscosity for non-Newtonian samples, thus, it plays a vital
74 role in the modeling effect when the composition of the printing material is fixed.
75 Apparent viscosity is the shear stress applied to a fluid divided by the shear rate. Low
76 apparent viscosity would lead to the material that is easily extruded but unable to
77 adequately support the shape and structure of the 3D-printed samples, while high
78 apparent viscosity would lead to bad extruding capacity, leading to 3D-printed
79 products with poor printing accuracy and easily broken lines. Therefore, an
80 intermediate apparent viscosity is crucial for a successful 3D-printed product.

81 Baking dough (BD) for cookies is a good additive manufacturing food material.
82 Preliminary work with different compositions has already optimized the formulation
83 of this 3D printable BD (Yang, F. *et al.*, 2018). However, once the optimized
84 formulation of this BD has been found, there are four main processing parameters that
85 affect 3D-printed products: filament diameter (FD), nozzle movement speed (NMS),
86 nozzle diameter (ND) and nozzle height (NH). In practice selection of suitable

87 processing parameters is crucial for the successful 3DP of a new product (Anitha, R.,
88 Arunachalam, S. & Radhakrishnan, P., 2001). In addition, shape retention of the
89 printed products after baking is also very important, as the extruded dough still needs
90 to be baked prior to being eaten. Therefore, post-process fast-cooling (PPFC) has been
91 used in these experiments to enhance the shape retention of printed samples.

92 This paper aimed to explore different processing parameters, including FD, NMS,
93 ND and NH, as well as that of PPFC on the rheological properties and geometrical
94 accuracy of a new 3D-printed food construct of BD, and to use
95 mathematical modeling to optimize these parameters of food 3DP. This work also
96 explores variance of post-process parameters such as PPFC time, to improve the
97 geometrical stability of BD after baking. As the available literature on 3DP of food
98 products is limited, the present work may provide useful information for future studies
99 in this emerging area.

100

101 **Materials and methods**

102 **Materials**

103 *Ingredients*

104 The BD consisted of icing sugar (crystalline sucrose, moisture content 0.2% (g/g,
105 db), Sugarman Corporation, China), butter (moisture content 0.4%, Lactalis
106 Corporation, France), low-gluten flour (moisture content 14%, Wilmar International
107 Limited, Singapore), eggs (moisture content 73%, local market) and distilled water.
108 Distilled water was used for all experimental work. The standard formulation was a
109 mixture of icing sugar, butter, low-gluten flour, eggs, and water at a ratio of 6.6: 6: 48:
110 10.4: 29, based on weight. This formulation was derived from that of butter cookies
111 (Zhi, 2014), and was optimized in our previous study (Yang, F. *et al.*, 2018).

112 *Preparation of the BD*

113 The refrigerated butter was softened at room temperature for 15 min, then mixed
114 thoroughly with icing sugar in a blender (IKA Co., Ltd, Germany), followed by the
115 addition of egg and further blending until the composition was well mixed.

116 Subsequently, low-gluten flour and distilled water were blended into the mixture, until
117 a homogenous composition was obtained (Zhi, 2014).

118 *3DP*

119 FD is the diameter of the cylindrical line of material extruded by the printer, i.e.
120 the monolayer height. In the printing process, the nozzle moves on the XYZ axis to
121 constantly adjust its position in relation to the platform, and NMS is the speed of
122 nozzle. ND is the diameter of the nozzle. NH is the distance between the nozzle and
123 the printing platform.

124 To investigate the effect of such processing parameters on the 3DP properties of
125 the BD, three levels of FD, NMS, ND and NH were tested. FD was set at 2.1, 2.3 and
126 2.5 mm, respectively. NMS was set at 20, 25 and 30 mm/s, respectively. ND was set
127 at 0.8, 1.5 and 2.0 mm, respectively. NH was set at 2.10, 2.40 and 2.60 mm,
128 respectively. Unless otherwise specified, the standard settings of FD, NMS, ND and
129 NH were 2.3 mm, 25 mm/s, 2.0 mm and 2.40 mm, respectively. The experimental
130 temperature and relative humidity were 24.8 °C and 51%, respectively (Anitha, R.,
131 Arunachalam, S. & Radhakrishnan, P., 2001).

132 An extrusion-based 3D printer (PORIMY Co. Ltd, Kunshan, China) was used in
133 this study. Both FD and NMS which are options in the setup of the controlled
134 software Repetier can be adjusted by the Repetier coupled software. In this
135 experiment, if the printed objects could maintain their shape and structure for at least
136 20 min, they were considered successfully printed.

137 *PPFC and baking*

138 The 3D-printed samples were fast-cooled in an ultra-low temperature
139 refrigerator, -65 °C, for 0, 5, 10 min, to ensure geometric stability. Once fully frozen
140 (except for the ones with 0 min fast-cooling), all products were baked in an oven at
141 190 °C for 10 min after which they were ready to be eaten (Zhi, 2014).

142 *Determination of samples quality*

143 *3D structure analysis*

144 The 3D-printed shapes in this experiment were a mouse and a square frame. The
145 printed products were measured for their length, width and height by using a vernier
146 caliper. In this experiment, the mouse target design had a length of 95.00 mm, a width
147 of 94.00 mm and a height of 35.00 mm, whereas the square frame target design had a
148 length & width of 100.00 mm and a height of 5.50 mm. The best 3D-printed BD was
149 selected by comparing its dimensions to those of the target designs. The less absolute
150 value of the difference between the dimensions of printed products and the ones of
151 target design that the printer makes, the better shape accuracy of printed products we
152 gets. For each processing parameters, samples were printed in triplicate and measured
153 in triplicate.

154 *Rheological property measurements*

155 The rheological properties were characterized using an AG-G2 Rheometer (AG-
156 1000, Co. TA, USA) with a parallel plate (cone diameter 20 mm, angle 0° and gap 2
157 mm), at 25 °C. For determination of steady shear viscosities, shear rate (SR) was
158 ramped from 0.1 to 100 s⁻¹. SR and apparent viscosity (η) were recorded by RheoWin
159 4 Data Manager (Rheology Software, Thermo Fisher Scientific, Waltham, MA).

160 A creep and recovery test was used, with creep strain of 0.1 Pa and recovery
161 strain of 0 Pa. The measure was done by creep test time of 75, 150 and 300 s,
162 followed by recovery time of 150, 300 and 600 s (Moreira, R., Chenlo, F. & Torres,
163 M. D., 2013). Each sample with different formulations was tested in triplicate.

164 Data analysis

165 All equations used for data analysis are presented below:

$$166 \quad PS = \frac{dL}{dt} \quad (1)$$

167 where PS is the printing speed (mm/s), dL is the extruded sample length when
168 printing (mm), and dt is the time used for printing (s).

$$169 \quad SR = \frac{d\mu}{dy} \quad (2)$$

170 where SR is the rate at which a progressive shearing deformation is applied to
171 certain material, $d\mu$ is the instantaneous printing speed (mm/s) which equals to the PS
172 value, and d_y is the diameter of the tube that connects the electric motor and the
173 extruder (mm).

$$174 \quad \text{Re} = \frac{\rho \mu L}{\eta} \quad (3)$$

175 where Re equals the Reynolds number, ρ is the density (g/mm^3), and L is the
176 diameter of the tube which connects the electric motor and the extruder (mm).

$$177 \quad \text{PS} = \frac{k \cdot 1}{\text{FD}^2} \quad (4)$$

178 where k is the rate empirical parameter.

179 Supposing that the trust caused by the direct-current electrical machine is
180 constant, all the materials are well-proportioned and printable. Thus, the volume of
181 the feeding material is also constant. In theory, the volume of the printing material per
182 second is equal to the volume of the feeding material per second. Consequently, the
183 PS is inversely proportional to the squared FD. Hence, the model equation was
184 obtained, and written as **Equation (5)**.

$$185 \quad h_c = \frac{V_d}{\text{NMS} \cdot \text{ND}} \quad (5)$$

186 where h_c is the theoretical superior NH (mm), V_d is the volume of extruded
187 material per second (extrusion rate, mm/s) (Wang, J. & Shaw, L.L., 2005).

188 Experimental data were analyzed using the SPSS 20.0 software (IBM, Chicago,
189 IL, USA), using one-way ANOVA and the Duncan test for pair-wise comparisons, to
190 determine significant differences among the means at 95% confidence level (Gunst, R.
191 F., 1998).

192

193 **Results and discussion**

194 3DP modeling effect

195 The printed products with the best shape accuracy are those which most closely
196 resemble what they are designed to. **Fig 1** and **Table S1** showed that the shape

197 accuracy of the printed products varies inversely with the difference between the
198 length, width and height of the printed products and those of the target designs. The
199 best 3D-printed mouse-shaped BD had a length of 94.62 mm, a width of 94.13 mm
200 and a height of 34.67 mm, whereas the best baked 3D-printed square-frame-shaped
201 BD had a length of 100.35 mm, a width of 100.35 mm and a height of 5.27 mm,
202 indicating the closest length, width and height to the ones of the target design.

203 Fluid behavior of the extruded materials

204 This extrusion-based 3D printing process is a kind of mechanical shearing
205 process. Regarding the complex mouse design, the use of different processing
206 parameters resulted in different lengths of sample and printing time, as measured by
207 the Repetier software. Therefore, the PS of each product can be calculated by
208 **Equation (1)**.

209 SR can then be calculated by **Equation (2)**. All the SR in this experiment were
210 between 0.1 and 2 s⁻¹. From **Fig S1**, with the SR between 0.1 and 2 s⁻¹, **Equation (6)**
211 which is a model based on experimental data can be fitted as follows:

$$212 \quad \eta = 3.1315r^{-0.623}, R^2 = 0.9991 \quad (6)$$

213 where η equals the apparent viscosity. Therefore, the apparent viscosities of
214 extruded materials, according to the value of the SR, can be calculated by **Equation**
215 **(6)**. In a previous study, researchers explored the rheological and extrusion behavior
216 of dental porcelain slurries for rapid prototyping applications, and deduced **Equation**
217 **(6)**, involving optimized NH and the volume of printed material per second (Wang, J.
218 & Shaw, L.L., 2005).

219 In addition, the fluid behavior could be considered as either laminar flow or not
220 by the Reynolds number. If the Reynolds number was below 2100, the corresponding
221 fluid behavior was laminar flow, which is known as steady flow (Tian, S. & Barigou,
222 M., 2016). Thus, the Reynolds number was calculated by **Equation (4)**. As shown in
223 **Table S2**, the Reynolds numbers for all samples were below 2100, indicating that all
224 fluid behaviors in this experiment were laminar flow.

225

226 Effect of variation of FD on the 3D-printed samples

227 As shown in **Fig 1**, printed products had the most intact shapes when using FD of
228 2.30 mm. The FD of 2.50 mm gave the second best print resolution. In contrast, the
229 products generated using a FD of 2.10 mm exhibited the most irregular shapes.

230 This phenomenon could be due to changes in apparent viscosity between
231 different samples. The PS and apparent viscosities of BD with different FD are
232 presented in **Table S2**. They indicate that, in this printing system, the printing
233 material with FD of 2.10 mm had a relatively lower apparent viscosity (2.84 Pa's)
234 compared with other FD values, which could be problematic for maintaining shape
235 and structure after printing (**Table S1**). However, when FD was increased to 2.50 mm,
236 the apparent viscosity was also higher (3.52 Pa's), which might be too difficult to be
237 extruded from the printer, causing lower printing accuracy. This explanation is also
238 supported by **Table S1**, where comparing with the best-shaped sample (obtained with
239 a FD of 2.30 mm), the printed sample with a lower FD (2.10 mm) was longer, wider
240 and thinner, while the printed sample with a higher FD (2.50 mm) was shorter,
241 narrower and thicker.

242

243 Effect of different NMS on the 3D-printed samples

244 As shown in **Fig 1**, printed products had the best intact shape when using an
245 NMS of 25.00 mm/s. An NMS of 30.00 mm/s gave the next best printed objects,
246 whereas the product obtained using an NMS of 20 mm/s exhibited the most irregular
247 shape.

248 This phenomenon could also be due to changes in apparent viscosity among the
249 samples. The PS and apparent viscosities of BD with different NMS were presented in
250 **Table 2S**. As shown in **Table 1S** and **Table 2S**, compared to products printed at the
251 NMS of 25.00 mm/s, which had the best intact shape, products printed at NMS of
252 20.00 and 30.00 mm/s respectively. Both of these samples had relatively higher
253 apparent viscosities (4.71 Pa's and 3.88 Pa's) and lower accuracy of printed samples
254 matching with target designs. Also, when the NMS was relatively higher (30.00
255 mm/s), the corner parts of the printed products could not be adequately printed, which
256 contributed to poor accuracy of the 3D-printed objects compared with the target
257 design. Additionally, high NMS (30 mm/s) might cause dragging of extruded material
258 by the nozzle which might lead to broken surface of printed samples.

259

260 Effect of variation of ND on the 3D-printed samples

261 The surface smoothness and printing precision of an object are primarily affected
262 by the size of the printer nozzle (Yang, F. *et al.*, 2018). As shown in **Fig 1**, printed

263 products had the best intact shape with a ND of 2.0 mm, followed by the ND of 1.5
264 mm, whereas the product obtained using a ND of 0.8 mm exhibited the most irregular
265 shape.

266 This phenomenon could be due to that relatively higher apparent viscosities
267 occurred at smaller values of ND (0.8 mm and 1.5 mm) (**Table 2S**), which led to the
268 lower printing accuracy.

269 The PS and apparent viscosities of BD with different ND are presented in **Table**
270 **2S**. As shown in **Table 2S**, in this printing system, as the ND is increased, the PS also
271 increased, but the apparent viscosity decreased. The smoothness and dimensional
272 accuracy could be enhanced by a smaller nozzle size, but this would cause an increase
273 the pressure or shear experienced by the material at the nozzle, having a negative
274 influence on extrusion behavior. This would lead to lower geometric accuracy when
275 the printed object matching to the target design. Therefore, in this printing system,
276 both 9.44 Pa's (0.8 mm FD) and 4.40 Pa's (1.50 mm FD) apparent viscosities might be
277 too high for extrusion, and 3.17 Pa's (2.0 mm FD) apparent viscosity might be suitable
278 for extrusion.

279

280 Effect of different NH on the 3D-printed samples

281 Attala (2016) indicated that NH significantly affects the geometric shape of
282 printed samples (Attalla, R., Ling, C. & Selvaganapathy, P., 2016). As shown in **Fig 1**,
283 printed products had the best intact shape at a NH of 2.40 mm, followed by the
284 product obtained using the NH of 2.60 mm, whereas the product obtained using a NH
285 of 2.10 mm exhibited the most irregular shape.

286 By substituting the PS and FD in the **Equation (5)**, we calculated that $k = 93.218$,
287 and $V_d = 4k/\pi = 118.689 \text{ mm}^3/\text{s}$. And $D_n = 2.0 \text{ mm}$ and $v_n = 25 \text{ mm/s}$, thus $h_c = 2.37$
288 mm. In **Fig 1**, the NH which had the best modeling effect was 2.40 mm, which was
289 the closest to 2.37 mm in the NH group. As the NH of 2.60 mm was also relatively
290 closer to the NH of 2.37 mm, the modeling effect of the product obtained using the
291 NH of 2.60 mm was better than that of the product obtained using the NH of 2.10 mm.

292 When the NH was lower than h_c , the extruded lines were much thicker, thus
293 leading to the geometric inaccuracy of printed products. When the NH was higher
294 than h_c , the feeding BD might not reach the print platform when the nozzle turned to a
295 corner, thus also leading to geometric inaccuracy of the printed products. Therefore,
296 when the NH was very close to h_c , the shape of the printed products should be the

297 closest to the target design. Also, as a result of dough swelling/spreading upon
298 extrusion, the optimum NH should be slightly higher than h_c .

299 In an ideal printing process, under the condition of matched extrusion rate and
300 PS, the NH value was supposed to be the same with the ND value (Wang, J. & Shaw,
301 L.L., 2005). However, due to elasticity of material, expansion of extruded material
302 occurred. Thus monolayer height (FD) of material would be slightly higher than the
303 ND. On the other hand, the NH also should be as low as possible to make sure that the
304 extruded material could be fused with earlier printed layers and have no inaccuracy
305 caused by delayed deposition. Thus the theoretical superior NH (h_c) should be very
306 close to FD. Therefore, the optimized NH was selected to 2.40 mm, which was the
307 closest one to h_c considering allowable error of dough swelling upon extrusion.

308

309 Effect of variation of PPFC time on the 3D-printed samples

310 In general, a high baking temperature would cause a certain level of damage to
311 the shapes and structures of 3D-printed food products. For example, cookie dough
312 which initially lost its shape when baked was printed, thus the cookies were chilled in
313 a freezer following extrusion to ensure geometric stability (Lipton *et al.*, 2010).
314 Preliminary experiments of the dough used in this experiment had been confirmed
315 that $-65\text{ }^\circ\text{C}$ for greater than 10 min provide the best result. In this experiment, all
316 products were frozen except for the products with PPFC time of 0 min, and then all
317 the samples were baked immediately after PPFC.

318 A creep and recovery test was performed, in which a shear stress was forced
319 upon the material. In a creep recovery experiment a stress is applied for a certain
320 duration and then is removed and the recovery is monitored for another certain
321 duration. Less strain during the test indicates a stronger ability of the material to
322 maintain the shape and structure of the printed products. As shown in **Fig 2** and **Table**
323 **1S**, with increasing PPFC time, the baked products had better shapes and structures
324 matching with the target design. This corresponds to these samples also exhibiting
325 less change during the creep and recovery test (**Fig 2S**). With no PPFC before baking
326 (0 min), the samples were seriously collapsed and could not keep their shapes (**Fig 2**).
327 Thus, if 3D-printed food products are to be produced have desired shapes and
328 structures, they should be fast-cooled to $-65\text{ }^\circ\text{C}$ for more than 10 min.

329

330 **Conclusion**

331 The properties and composition of materials ready for printing are considered as
332 important factors in the 3DP process. These materials should be homogenous and
333 have appropriate flow properties for extrusion as well as can support its structure
334 during and after printing process. Besides physical properties of different composition,
335 the results of process optimization for 3DP confirmed that FD, NMS, ND and NH
336 also affect the shape accuracy of printed samples. It was found that FD (2.30 mm),
337 NMS (25 mm/s), ND (2.0 mm), NH (2.40 mm) were optimal parameters for 3DP BD.
338 PPFC (-65 °C; more than 10 min) after printing and before baking was beneficial to
339 maintain the structure and shape of samples after baking. This corresponded to
340 3.17 Pa's apparent viscosity when extruded. Moreover, the success of the 3DP BD
341 provided beneficial guidance for other food material in 3DP.

342

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352

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403

404 **Figure captions:**

405 **Fig 1.** Representative photos of printed samples with different processing parameters,
406 in different groups: (a) FD; (b) NMS; (c) ND; (d) NH

407 **Fig 2.** Representative photos of baked printed samples with different PPFC time
408 before baking

409

410 **Supplementary information captions:**

411 **Fig 1S.** Apparent viscosity and SR of samples

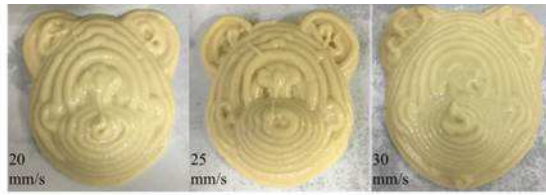
412 **Fig 2S.** Creep and recovery curve of samples with different PPFC time: (a) 0 min; (b)
413 5 min; (c) 10 min

414 **Table 1S.** 3D structure analysis for the mouse design (FD, NMS, ND and NH group)
415 or the square frame design (PPFC time group)

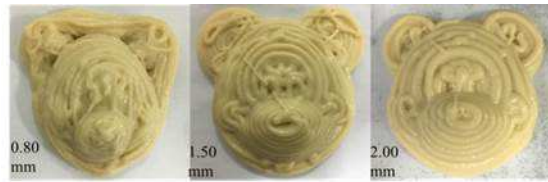
416 **Table 2S.** Printing speeds and apparent viscosities of samples, in different groups: FD;
417 NMS; ND; NH



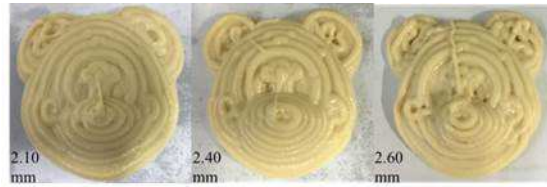
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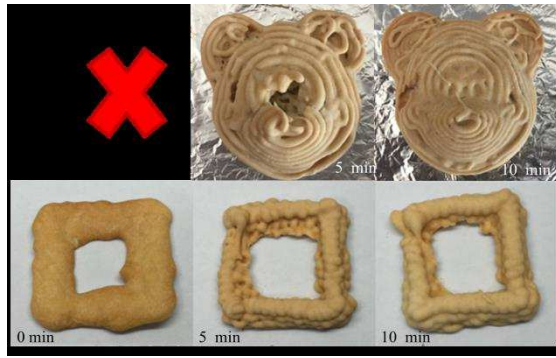
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