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**Fe(III)-catalyzed degradation of persistent textile dyes by chlorine at slightly acidic conditions: the crucial role of  $\text{Cl}_2^{\bullet-}$  radical in the degradation process and impacts of mineral and organic competitors**

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## Abstract

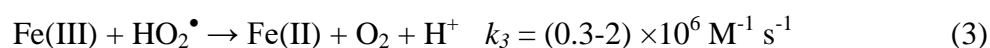
In this work, we have explored for the first time the potential application of trace-Fe(III)/chlorine system as an innovative oxidation technology for the degradation of persistent textile dyes. Fe(III)/chlorine combination improved the dye removal by ~ 40% within 30 s, as compared with chlorination alone, mainly through a radical pathway induced by the catalytic activation of chlorine in the presence of Fe(III). A chemical probe method was used for identifying the main reactive species.  $\text{Cl}_2^{\bullet-}$  was found to be the key species responsible of huge abatement of dyes in the Fe(III)/chlorine system, whereas  $\bullet\text{OH}$  and  $\text{Cl}^\bullet$  can participate with only ~ 5% in the overall removal efficiency. At pH 3, 77% of reactive green 12 (RG12) was removed after 30 s, and then the removal efficiency diminished to 60% at pH 4, 20% at pH 5 and ~ 10% at pH 6 and 7. However, the best implication of free radicals was achieved at pH 4, at which the degradation rate was 3.3 times higher than that of chlorination alone. The dye removal efficiency increased with an increase in chlorine and iron loads up to certain optimums (~50  $\mu\text{M}$  of iron and ~ 250  $\mu\text{M}$  of chlorine), but detrimental effect was observed at higher dosage levels. An increase in the solution temperature notably accelerated the removal yield (i.e. 81% of RG12 was removed at 50 °C against 67% at 30 °C and 57% at 10 °C).  $\text{NO}_2^-$  and  $\text{HSO}_3^-$  as well as the cationic surfactant Adogen 464 showed strongest inhibiting effect on the performance of the process. Based on these findings, the Fe(III)/chlorine process is highly efficient in removing dyes from wastewaters.

*Keywords:* Fe(III)/chlorine process; Innovative oxidation technology; Textile dyes; Degradation;  $\text{Cl}_2^{\bullet-}$  radical; Mineral anions

## 1. Introduction

Dyes are one of the most hazardous chemical compound classes found in industrial effluents and need to be treated since their presence in water bodies reduces light penetration, precluding the photosynthesis of aqueous flora<sup>1,2</sup>. They are also aesthetically objectionable for drinking and other purposes and can cause dermatitis, allergy, skin irritation and also provoke cancer and mutation in humans.<sup>1,3,4</sup>

Advanced oxidation processes (AOPs) which involve the generation of highly reactive and non-selective hydroxyl radical ( $\bullet\text{OH}$ ,  $E^0 = 2.8 \text{ V}$ ) are of interest for the destruction of persistent and non-biodegradable organic pollutants in wastewater.<sup>5</sup> Among these techniques, Fenton's ( $\text{Fe(II)}/\text{H}_2\text{O}_2$ ) and Fenton-like ( $\text{Fe(III)}/\text{H}_2\text{O}_2$ ) reagents have been the subject of extensive studies in order to examine the efficiency of the process for the removal of organic pollutants<sup>6,7</sup>. In Fenton process,  $\bullet\text{OH}$  is produced from the direct catalytic action of iron(II) on  $\text{H}_2\text{O}_2$  as in Eq. 1. The Fenton process can be efficiently applied when the pH optimum value of the polluted aqueous medium is about 2.8–3.0.<sup>7,8</sup> Indeed, in these conditions, the Fenton's reaction can be propagated by the catalytic behavior of the  $\text{Fe}^{3+}/\text{Fe}^{2+}$  couple, in which  $\text{Fe}^{2+}$  ion is regenerated from the so-called Fenton-like reaction between  $\text{Fe}^{3+}$  and  $\text{H}_2\text{O}_2$  as well as  $\text{Fe}^{3+}$  and  $\text{HO}_2\bullet$  radical (Eqs. 2 and 3)<sup>6,9</sup>. It has been reported that the Fenton-like reaction (3) is much slower than the Fenton's reaction itself (Eq. 1)<sup>10</sup>



However, all Fenton-based process have several operating limitations such as (i) iron precipitation as  $\text{Fe}(\text{OH})_3$  at  $\text{pH} > 3$ , (ii) the use of relatively high dosages of iron and  $\text{H}_2\text{O}_2$  and (iii) the high cost of  $\text{H}_2\text{O}_2$  and its facile thermal decomposition at room temperature.<sup>9</sup> Nowadays, the substitution of  $\text{H}_2\text{O}_2$  by  $\text{NaClO}$  in Fenton process has become an interesting task due to (i) the very low cost and the marked stability of  $\text{NaClO}$ , (ii) the very fast reaction between  $\text{Fe}(\text{II})$  and chlorine ( $k \sim 10^4 \text{ M}^{-1} \text{ s}^{-1}$ ), which is suspected to generate strong reactive species and (iii) the use of very low concentration of reagents.<sup>11,12</sup> Behin et al.<sup>12</sup> have reported that sodium hypochlorite may be an alternative to hydrogen peroxide in Fenton process. The degradation of simulated petroleum wastewater was performed by Fenton and  $\text{Fe}(\text{II})/\text{NaClO}$  at various oxidants and iron loads for  $\text{pH} \leq 4$ .<sup>12</sup> Their results showed strong similarities between the two processes, but higher oxidation efficiency was obtained with Fenton system. Kaluzna-Czaplinska et al.<sup>13</sup> have compared the efficiency of chlorine with  $\text{Fe}(\text{II})/\text{chlorine}$  at  $\text{pH} 3.5$  by varying iron load in the range of 5-30 mg/L and keeping  $\text{NaClO}$  at 0.5 mg  $\text{NaClO}$  per mg of Acid Brown 349. It was found that efficient COD removal was obtained by the combined process. More recently, our research group has studied in detail the effect of  $\text{Fe}(\text{II})/\text{chlorine}$  process on the degradation of several textile dyes under various experimental conditions. A drastic acceleration in the degradation rate of all dyes was obtained.<sup>11</sup>

The underlying reactions mechanism for the  $\text{Fe}(\text{II})/\text{chlorine}$  system is until now under debate. Candeias<sup>14</sup> showed that hydroxyl radical was implicated in the system with 27%, as predicted from the hydroxylation of benzoate. The other portion was attributed to non-determined reactive species.  $\bullet\text{OH}$  radical was also determined recently in the sludge conditioned with  $\text{Fe}(\text{II})/\text{Ca}(\text{ClO})_2$ . In contrast, Folkes et al.<sup>15</sup> reported that the reaction of

iron(II) with HClO yielded reactive intermediates distinguishable from hydroxyl radicals (i.e., presumably, chlorinated reactive species (CRS)). In our recent study,<sup>11</sup> based on thermodynamic analysis, a chain reaction mechanism was proposed for the Fe(II)/chlorine system and the reactive species involved in this system were identified using specific radical scavengers. It was found that  $\text{Cl}_2^{\bullet-}$  radical plays the dominant role in the oxidative event of Fe(II)/chlorine system, although other reactive radicals such as  $\bullet\text{OH}$ ,  $\text{Cl}^\bullet$  and  $\text{ClO}^\bullet$  may have also contributed to the degradation process.

In the present work, a new approach based on combining chlorine with Fe(III) rather than Fe(II) has been explored for the first time. The degradation of several textile dyes by the Fe(III)/chlorine was investigated at various experimental conditions. A reaction mechanism has been proposed and the main radical species responsible for the oxidation are identified. Additionally, the impact of several organic and mineral additives was assessed to evaluate the process efficacy if the process was to be applied in treating real textile effluents.

## 2. Experimental section

### 2.1. Reagents

All solutions were prepared using reagent-grade chemicals and deionized water. Basic fuchsin (abbreviation: BF; CAS number: 569-61-9; molecular formula:  $\text{C}_{20}\text{H}_{20}\text{ClN}_3$ , molecular weight:  $337.84 \text{ g mol}^{-1}$ ), toluidine blue (abbreviation: TB; CAS number: 6586-04-5, molecular formula:  $\text{C}_{15}\text{H}_{16}\text{ClN}_3\text{S}\cdot 0.5\text{ZnCl}_2$ , molecular weight:  $373.97 \text{ g mol}^{-1}$ ), chlorazol black (abbreviation: CB, molecular formula:  $\text{C}_{34}\text{H}_{25}\text{N}_9\text{Na}_2\text{O}_7\text{S}_2$ ), C.I. reactive green 12 (abbreviation: RG12; CAS number: 12225-80-8; molecular formula:  $\text{C}_{60}\text{H}_{29}\text{Cl}_3\text{N}_{16}\text{NiO}_{21}\text{S}_7\cdot\text{H}_2\text{O}$ , molecular weight:  $1837.7 \text{ g mol}^{-1}$ ) and sodium hypochlorite

(NaOCl) solution (available chlorine ~15%) were purchased from Sigma-Aldrich. All other reagents (t-butanol, sodium azide, benzoic acid, phenol, nitrobenzene, ferric sulfate, sulfate ferrous, sodium hydroxide, sulfuric acid, sodium chloride, sodium sulfate, sodium nitrite, sodium nitrate, potassium bromide, sodium sulfite, surfactants and humic acid) were also supplied by Sigma- Aldrich and used as received.

## 2.2. Experimental procedure

Experiments were performed under magnetic stirring in a cylindrical water-jacketed glass reactor (capacity: 300 mL,  $\phi_{\text{int}} = 6$  cm) to control the solution temperature through circulating water, i.e. provided from a RC6 Lauda thermo-cryostat, in the cell-jacket at controlled flux. Stock solutions of dyes (1 g/L, pH 5), chlorine (10 mM, pH 5) and iron (5 mM, pH 3) were prepared using deionized water and preserved in the dark at 5 °C. Oxidative trials were conducted using a 200 mL of air-equilibrated solutions (the reactor was open to air). For each experiment, the solution of dye and iron was firstly prepared at desired concentrations, pH and temperature. After that, chlorine was added and the chronometer was turned on, this was the time zero for the reaction. Samples aliquots (3 mL) were withdrawn at different time interval using a glass syringe and transferred to a quartz cell (1 cm optical path length) of a UV–vis. spectrophotometer (Jenway 6405) to measure the absorbance of dyes at their maximum absorption wavelengths (region ( $\lambda_{\text{max, RG12}} = 614$  nm,  $\lambda_{\text{max, TB}} = 628$  nm,  $\lambda_{\text{max, CB}} = 578$  nm,  $\lambda_{\text{max, BF}} = 543$  nm)). Calibration curves, established based on Lambert-Beer law, were used for determining the concentration of dyes during the oxidation runs. The solution pH was adjusted using NaOH or H<sub>2</sub>SO<sub>4</sub> and displayed by a Jenway 3505 pH-meter. All experiments were repeated at least three times and data were reported as averages.

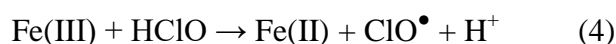
### 3. Results and discussion

#### 3.1. Efficiency of the Fe(III)/chlorine process

Fig. 1(a) shows the effect of Fe(III) concentration in the range of 0-100  $\mu\text{M}$  on the removal kinetics of RG12 (30 mg/L) in the presence of 250  $\mu\text{M}$  of chlorine at pH 4 and temperature of 20  $^{\circ}\text{C}$ . As clearly seen, the dye removal efficiency increased significantly with increasing Fe(III) from 15 to 50  $\mu\text{M}$ , after which a further increase in iron concentration did not show notable change in the RG12 removal. In the absence of iron, chlorine eliminated 19% of RG12 within 30 s; the removal efficiency increased to 30%, 42% and 60% when Fe(III) was present at 15, 25 and 50  $\mu\text{M}$ , respectively. After 5 min, Fe(III)/chlorine process eliminated 80% of RG12 against 56% for chlorine alone. The removed amount of the dye upon chlorine and Fe(III)/chlorine processes as well as the resulted enhancement index (EI) are shown in Fig. 2(b) for different iron doses. The EI is defined as the ratio of RG12 removal by Fe(III)/chlorine process to that of chlorination alone (both evaluated after 30 s of reaction). The EI increased from 1.6 for 15  $\mu\text{M}$  of Fe(III) to 2.2 for 25  $\mu\text{M}$ , 3.3 for 50  $\mu\text{M}$  and 3.5 for 100  $\mu\text{M}$ . The viability of the Fe(III)/chlorine process was not only limited to the RG12 dye degradation but similar efficient removal rates were obtained for toluidine blue (TB), chlorazol black (CB) and Basic fuchsin (FB), as can be seen in Fig. 2. Significant enhancement indexes of 5, 3.66 and 2.4 were obtained for TB, CB and BF, respectively. All these improvements by the Fe(III)/chlorine system was mainly attributed to the formation of reactive species generated by the catalytic activation of chlorine. It should be noted that the iron doses used in this study were much lower than those used in the Fenton-like reaction.

#### 3.2. Proposed mechanism for Fe(III)/chlorine system

We have recently demonstrated that the Fe(II)/chlorine process yields huge enhancements in the degradation of several synthetic dyes, as compared with chlorination alone.<sup>11</sup> It was confirmed through radicals probing technique that some reactive species such as  $\bullet\text{OH}$  and other chlorinated reactive species ( $\text{Cl}\bullet$ ,  $\text{ClO}\bullet$  and  $\text{Cl}_2\bullet^-$ ) may be formed *via* direct catalytic action of iron(II) on chlorine.<sup>11</sup> A reaction mechanism consisting on 19 reactions involving initiation, propagation and termination steps has been proposed for the system Fe(II)/chlorine.<sup>11</sup> To explain the obtained results for the case of Fe(III)/chlorine system, the earlier mechanism has been partially modified by including the initial reactions required for the generation of Fe(II), like in the Fenton-like process.<sup>6,8</sup> The first step consists on the reduction of Fe(III) into Fe(II) by chlorine as in Eq. (4). Then the process described previously (Ref. 11) will be triggered. The overall reaction scheme is shown in Table 1.



Eq. 4 has been proposed by complete analogous to the Fenton-like reaction (Eq. 2) in which Fe(III) was firstly reduced into Fe(II) by  $\text{H}_2\text{O}_2$ . Thermodynamically, both  $\text{H}_2\text{O}_2$  and HClO are strong oxidants of comparable oxidation potentials (1.77 V for and 1.49 for HClO)<sup>16</sup>. The Fenton-like reaction has been completely accepted with the chemistry community even through  $\text{H}_2\text{O}_2$  and Fe(III) exists also at higher oxidation state exactly like our case (HClO and Fe(III)). In the Fenton-like system, Eq. 2 acts only as precursor of Fenton system (Fe(II)/ $\text{H}_2\text{O}_2$ ). Correspondingly, Eq. 4 proposed for the system Fe(III)/HClO may also act as precursor of the system Fe(II)/chlorine, which has proven their high efficiency in degrading organic pollutants via radical pathway involving  $\bullet\text{OH}$ ,  $\text{ClO}\bullet$  and  $\text{Cl}_2\bullet^-$  radicals.<sup>11</sup>

According to the proposed mechanism, the efficiency of Fe(III)/chlorine process should be lower than that of Fe(II)/chlorine as a part of chlorine will initially be used to generate Fe(II), which is one of the precursor of the Fe(II)/chlorine system. This speculation was tested by conducting RG12 degradation experiment by Fe(II)/chlorine in the same conditions as that of Fe(III)/chlorine process (Fig. 3). From Fig. 3, it is seen that 87% of RG12 was removed by Fe(II)/chlorine at the first 30 s, instead 60% for the case of Fe(III)/chlorine. The loss in the removal efficiency by Fe(III)/process (~ 27%) can be associated to the contribution of reaction (4) in the overall consumption of chlorine to yield Fe(II).

### 3.3. Probing of reactive species

Efforts were made to identify the involvement and contribution of different reactive species derived from the Fe(III)/chlorine reaction in the oxidation of RG12. According to the mechanism shown in Table 1, several radical species, *i.e.*, principally  $\bullet\text{OH}$ ,  $\text{Cl}\bullet$ ,  $\text{ClO}\bullet$  and  $\text{Cl}_2\bullet^-$  may be created in the Fe(III)/chlorine system. These species are the most expected oxidants as they have higher redox potentials (2.43 V for  $\text{Cl}\bullet$ , 2.13 V for  $\text{Cl}_2\bullet^-$  and 1.5-1.8 V for  $\text{ClO}\bullet$ ) and are mostly implicated in the photoactivated chlorine process.<sup>17,18</sup> Additionally, these radicals react with organic matters practically with the same mechanisms (H-atom abstraction, electron transfer or addition to unsaturated bands).<sup>18</sup> The second-order rate constants for reactions involving these radicals varies in the order  $\sim 10^8$ - $10^{10} \text{ M}^{-1}\text{s}^{-1}$  for  $\bullet\text{OH}$  and  $\text{Cl}\bullet$ ,  $\sim 10^7$ - $10^9 \text{ M}^{-1}\text{s}^{-1}$  for  $\text{ClO}\bullet$  and  $10^2$ - $10^6 \text{ M}^{-1}\text{s}^{-1}$  for  $\text{Cl}_2\bullet^-$ .<sup>17,18</sup>

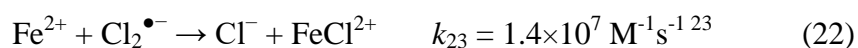
The contribution of the above radicals as well as direct chlorination in the degradation of RG12 by the Fe(III)/chlorine was evaluated using the following scavengers: nitrobenzene

(NB), benzoic acid (BA), t-butanol (TBA), phenol (Ph), sodium azide ( $\text{NaN}_3$ ) and ascorbic acid (AscA). Table 2 shows the reactivity of NB, BA, Ph,  $\text{N}_3^-$  and TBA with  $\bullet\text{OH}$ ,  $\text{Cl}\bullet$ ,  $\text{ClO}\bullet$  and  $\text{Cl}_2^{\bullet-}$ . Traditionally, ascorbic acid as a classical reducing agent was mostly used as a common scavenger for both free radicals and chlorine.<sup>19-21</sup> It has been used to confirming the contribution of both free radicals and chlorine in the degradation process.  $\text{N}_3^-$  and phenol can rapidly scavenge all radicals. Therefore, they were used for approximating the contribution of direct chlorination in the Fe(II)/chlorine oxidative process. NB only reacts with  $\bullet\text{OH}$  and it is resistance to CRS and chlorine.<sup>22</sup> Hence, NB was used as radical selective probe to differentiate the role of  $\bullet\text{OH}$  and CRS+chlorine. BA can scavenge  $\bullet\text{OH}$  and  $\text{Cl}\bullet$  but its scavenging effect on  $\text{ClO}\bullet$ ,  $\text{Cl}_2^{\bullet-}$  and chlorine is negligible. It has been then used to determine indirectly the contribution of  $\text{Cl}\bullet$ . TBA can scavenge  $\bullet\text{OH}$ ,  $\text{Cl}\bullet$  and  $\text{ClO}\bullet$  and its scavenging effect on  $\text{Cl}_2^{\bullet-}$  is negligible. TBA was used for appreciating the plausible role of  $\text{Cl}_2^{\bullet-}$ .

The effect of all above scavengers on the removal kinetics of RG12 is shown in Fig. 4. The used initial concentrations of NB, BA, Ph, AscA and  $\text{NaN}_3$  were 10 mM, but that of TBA was 100 mM. These high concentrations were selected to ensure that radical scavengers are in excess in the solution. It is clearly observed from Fig. 4 that ascorbic acid suppressed 98% of the dye removal, indicating that both reactive radicals and molecular chlorine were involved in the degradation process. Azide ions and phenol diminished the removal efficient by ~ 95% and 98%, meaning that direct chlorination of RG12 contributed only ~ 5 to 8% to the degradation efficiency of the dye upon Fe(III)/chlorine treatment. The addition of NB as a selective quencher of  $\bullet\text{OH}$  reduced the RG12 removal from 60% to 55%. Thus,  $\bullet\text{OH}$  contributes by only ~ 5% in the overall removal rate of RG12 by Fe(III)/chlorine process.

Besides, BA which quenches both  $\bullet\text{OH}$  and  $\text{Cl}\bullet$  resulted in only 12% reduction in the dye removal, indicating that  $\text{Cl}\bullet$  contributes about 7% (because  $\bullet\text{OH}$  sole contributed by 5 %). Therefore,  $\text{Cl}_2^{\bullet-} + \text{ClO}\bullet$  may have contributed the major part (~ 80%) to the overall effect of Fe(III)/chlorine system. However, given that TBA, which could quench all radicals except  $\text{Cl}_2^{\bullet-}$ , shows a similar influence as that of BA (~ 10% reduction, as compared with the non-quenched system), it could be concluded that  $\text{ClO}\bullet$  has an insignificant role whereas  $\text{Cl}_2^{\bullet-}$  could be the dominant reactive species in the degradation of the dye by the system Fe(III)/chlorine. This conclusion is quantitatively in agreement with that obtained for the system Fe(II)/chlorine.<sup>11</sup>

Based on this analysis, the detrimental effect of high Fe(III) dosage (Fig. 1) may only be due to the quenching of  $\text{Cl}_2^{\bullet-}$  radical by the excess of iron as given in the following reaction:



### 3.4. Effect of chlorine dosage

Different amounts of chlorine were used to investigate the effect of chlorine dosage on RG12 oxidation at pH 4 and  $[\text{Fe(III)}]_0 = 50 \mu\text{M}$ . The results presented in Fig. 5(a), indicate that RG12 oxidation increases with an increase in chlorine concentration up 1000  $\mu\text{M}$  for the case of Fe(II)/chlorine system<sup>11</sup>. Eliminations of 37%, 45%, 60% and 73% were recorded for 25, 100, 250 and 1000  $\mu\text{M}$  of chlorine. As shown in Table 1, the concentration of free radical might have increased with an increase in chlorine concentration, which improved the degradation rate of the dye. However, the generated radicals can be scavenged by chlorine itself when it is used at much higher concentration.<sup>11</sup> This case was not observed in this study,

probably because the highest chlorine dose used herein (1000  $\mu\text{M}$ ) did not reach the critical level to slow down the degradation process. Candeias et al.<sup>14</sup> have studied the reaction between ferrocyanide, as source of Fe(II), and chlorine at pH 7. They found that the rate of ferrocyanide decomposition increased linearly with increasing chlorine dosage up to 1000  $\mu\text{M}$ . Similarly, no detrimental effect of high chlorine dose was observed by Kong et al.<sup>24</sup>, Fang et al.<sup>25</sup> and Qin et al.<sup>26</sup> who investigated the degradation of several organic contaminants by UV/chlorine process.

Importantly, the beneficial effect of Fe(III)/chlorine, as compared to chlorination alone, increased with an increase in  $[\text{chlorine}]_0$  in the range 25-250  $\mu\text{M}$ , as can be seen in Fig. 5(b). After 30 s of reaction, chlorine alone at 25  $\mu\text{M}$  eliminated 1 mg/L of RG12, but in the presence of iron the removal increased to 11 mg/L. At 250  $\mu\text{M}$ , the combined process removed 19 mg/L of RG12 against 5.7 mg/L for chlorination alone. However, the enhancement index showed the best value, 10.57, at 25  $\mu\text{M}$  of chlorine and then decreased to 6 at 100  $\mu\text{M}$ , 3.5 at 25  $\mu\text{M}$  and 2.2 at 1000  $\mu\text{M}$ .

### **3.5. Effect of pH**

In iron-based treatment techniques of wastewater, the pH is probably one of the most important and crucial parameters that should always be taken into consideration. In our case, the process sensitivity to the initial solution pH was investigated at Fe(III) and chlorine dosages of 50  $\mu\text{M}$  and 250  $\mu\text{M}$ , respectively. The concentration of RG12 was kept at 30 mg/L. The obtained results are presented in Fig. 6(a) whereas Fig 6(b) show the amount of dye removed after 30 s by chlorination and Fe(III)/chlorine process as well as the resulted enhancement index. As can be seen, the solution pH affected strongly the RG12 degradation

by Fe(III)/chlorine. The degradation rate decreased markedly with pH rise in the range 3-7. At pH 3, 77% of RG12 was removed after 30 s, and then the removal efficiency diminished to 60% at pH 4, 20% at pH 5 and ~ 10% at pH 6 and 7. Correspondingly, chlorine alone eliminated 53% of RG12 at pH 3, 19% at pH 4 and ~ 10% for pH > 4 (Fig. 5(b)). The enhancement index varies as 1.44 at pH 3, 3.3 at pH 4, 2.4 at pH 5 and practically ~1 for pH > 5.

The solution pH affects both iron(III) and chlorine speciations. The pKa values of chlorine are ~ 1 and 7.6.<sup>18</sup> Chlorine species are predominately distributed as: Cl<sub>2</sub> at pH < 3, hypochlorous acid (HClO) at 4 < pH < 6.5 and hypochlorite (ClO<sup>-</sup>) at pH pH ≥ 8.<sup>18</sup> The chemical activity of chlorine species decreases in the order Cl<sub>2</sub> < HClO < ClO<sup>-</sup>.<sup>27</sup> Additionally, the reactivity of HClO with organics is much higher at slightly acidic condition, *i.e.*, pH 4, than that at near neutral pHs (5–6).<sup>27</sup> On the other hand, the speciation diagram of Fe(III) indicated that Fe<sup>3+</sup> ions is predominated for pH < 2, Fe(OH)<sup>2+</sup> predominated at pH 4 and Fe(OH)<sub>2</sub><sup>+</sup> predominated at pH 4-6.<sup>8,28</sup> However, the Fe(III) precipitates as Fe(OH)<sub>3</sub> at pH 6, and at pH 7, the fraction of Fe(OH)<sub>3</sub> is about 10%.<sup>8,28</sup> The best efficacy of the Fenton-like process (Fe(III)/H<sub>2</sub>O<sub>2</sub>) was observed at ~ pH 3 when Fe(OH)<sup>2+</sup> is the predominant species. Sanz et al.<sup>28</sup> have reported that in Fenton-like system the Fe(OH)<sup>2+</sup> is responsible for the generation of hydroxyl radicals process and not the Fe<sup>3+</sup> itself.

Based on these specification, the effect of pH on the degradation of RG12 by Fe(III)/chlorine process can be explained as follow: the higher degradation at pH 3 is due to a combination of direct chlorination and free radical reaction. It has been estimated that chlorination contributed in the Fe(II)/chlorine by 37% rather than < 10% for pH > 3.<sup>11</sup>

Additionally, ~2% of  $\text{Cl}_2$  exists at pH 3. This species is much active than other chlorine species and makes the reaction faster even at very low concentrations.<sup>27</sup> At pH 4, chlorine retained the form  $\text{HClO}$  but  $\text{Fe(III)}$  exists as a mixture of  $\text{Fe(OH)}^{2+}$  (25%) and  $\text{Fe(OH)}_2^+$  (75%). The degradation rate of dye decreased by 17% compared to that at pH 3, revealing that, as in Fenton- like system,  $\text{Fe(OH)}^{2+}$  is more reactive with  $\text{HClO}$  than  $\text{Fe(OH)}_2^+$ . Therefore, an increase in the fraction of  $\text{Fe(OH)}_2^+$  with an increase in pH to 5 and 6 is likely the reason of the continuous drop in RG12 removal efficacy at these pH levels. At pH 7, chlorine exists as a mixture of  $\text{HClO}$  (80%) and  $\text{ClO}^-$  (20%). Thus, in addition to the reasons of pH 5 and 6, 10% of iron is as  $\text{Fe(OH)}_3$  and all  $\text{Fe(II)}$  species is unreactive with  $\text{ClO}^-$ . Consequently, it is recommended that the  $\text{Fe(III)}$ /chlorine process should be applied at pH 4 to avoid (i) strong acidification (as at pH 3), (ii) lower degradation performance (i.e. for pH > 4), and (iii) sludge formation during the treatment.

### **3.6. Effect of liquid temperature**

The effect of solution temperature on the efficiency of RG12 removal by chlorine and  $\text{Fe(III)}$ /chlorine process was investigated for 50  $\mu\text{M}$  of  $\text{Fe(III)}$  and 250  $\mu\text{M}$  of chlorine and the obtained results are summarized in Fig. 7. This data clearly shows that higher temperatures favor higher removal rate of the dye by the combined system. 81% of RG12 was removed at 50 °C against 67% at 30 °C and 57% at 10 °C. Additionally, the removed efficiency increased linearly with temperature rise for both chlorination and  $\text{Fe(III)}$ /chlorine process, as indicated in Fig. 7(b). However, the ratio between the removal with  $\text{Fe(III)}$ /chlorine to that with chlorine alone decreased from 6.34 at 10 °C to 3.3 at 20 °C and then to 1.81 at 50 °C. This is due to the fact that the slope of the removal rate of the dye with chlorination alone is greater

than that obtained by Fe(III)/chlorine system, as showed the data of Fig. 7(b). Nevertheless, higher level of elimination were always obtained with Fe(III)/chlorine process.

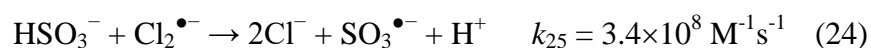
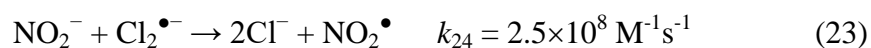
### **3.7. Effect initial dye concentration**

RG12 degradation study by chlorine and Fe(III)/chlorine was carried out at concentration range of 10-100 mg/L, keeping other parameters constant ( $[\text{Fe(III)}]_0 = 50 \mu\text{M}$ ,  $[\text{chlorine}]_0 = 250 \mu\text{M}$  and pH 4). It can be seen from Fig. 8(a) that the initial concentration of the pollutant and the removal efficiency are inversely related. Removals of 68%, 63 % and 30% was reached for  $C_0 = 10, 30$  and  $100 \text{ mg/L}$ , respectively. On the other hand, the removed amount at 30 s augmented significantly from 7 mg/L for  $C_0 = 10 \text{ mg/L}$  to 19 and 32 mg/L for, respectively,  $C_0 = 30$  and  $100 \text{ mg/L}$  (Fig. 8(b)), indicating higher degradation rate at higher initial dye concentration. All these observations are exactly similar to those reported by Meghlaoui et al.<sup>11</sup> for the degradation of RG12 by Fe(II)/chlorine system. In general, at fixed dosage of Fe(III) and chlorine, the generation rate of free radicals is constant. Increasing  $C_0$  in the reacting medium results in limiting the radical-radical recombination and overleaping the radicals-dye reaction. Thus, higher conversion rates would be associated to higher  $C_0$ .<sup>29</sup> It can also be observed from Fig. 8(b) that the enhancement index increased with an increase in  $C_0$  up to  $\sim 30 \text{ mg/L}$  and declined beyond this concentration. Therefore, the best useful effect of the Fe(III)/chlorine system was obtained at moderate concentration of pollutants.

### **3.8. Effect of mineral salts**

As inorganic ions constitute a major part of the water matrix, the degradation of RG12 by Fe(III)/chlorine system was accomplished in selected aqueous electrolyte solutions. The effect of different salts (NaCl,  $\text{Na}_2\text{SO}_4$ ,  $\text{NaNO}_2$ ,  $\text{NaNO}_3$ , KBr and  $\text{Na}_2\text{SO}_3$ ) was studied at pH

4 by adding each salt at 1, 10 and 50 mM under constant dosages of iron (50  $\mu\text{M}$ ) and chlorine (250  $\mu\text{M}$ ) (Fig. 9). As can be seen  $\text{Cl}^-$ ,  $\text{SO}_4^{2-}$ ,  $\text{NO}_3^-$  and  $\text{Br}^-$  have no influence at 1 mM while nitrite and sulfite drastically inhibited the degradation of the dye (RG12 removal was suppressed at 83% for sulfite and 95% for nitrite). In fact, among the above anions,  $\text{HSO}_3^-$  and  $\text{NO}_2^-$  have shown a strong reactivity toward  $\text{Cl}_2^{\bullet-}$  radical (Eqs. 23 and 24).<sup>23</sup>



Above 1 mM, chloride enhanced the degradation of the dye mainly through increasing the concentration of  $\text{Cl}_2^{\bullet-}$  (Eq. 6). This is another confirmation of the responsibility of this radical in the degradation of RG12 in the Fe(III)/chlorine system. For  $\text{SO}_4^{2-}$ ,  $\text{NO}_3^-$  and  $\text{Br}^-$ , their partial inhibiting effects (*i.e.* 20% inhibition max.) was observed only at higher concentration (50 mM); the concentration at which sulfite and nitrite completely suppress the degradation of the dye.

### 3.9. Effect of organic competitors

The effect of humic acids (HA: 5-20 mg/L) as natural organic matter and four surfactants (SDS, Tween 20, Tween 80 and Adogen 464) on the degradation of RG12 by Fe(III)/chlorine was investigated at pH 4 by fixing iron and chlorine concentration at 50 and 250  $\mu\text{M}$ , respectively (Fig. 10). The surfactants concentrations were selected to be lower than their critical micelle concentration (CMC). HA reduced the RG12 removal by 26% at 1 mg/L and 42% at 20 mg/L, showing a significant retarding in the degradation rate. On the other hand, non-ionic and anionic surfactants (triton X-100 and SDS, respectively) did not show significant reduction in the degradation rate of the dye (at max. 15% reduction was recorded)

whereas adogen 464 (cationic surfactant) decreases significantly the treatment yield by 24% at 1  $\mu\text{M}$  and 72% at 100  $\mu\text{M}$ . It seems that the reactivity of  $\text{Cl}_2^{\bullet-}$  is strongly affected by the charge of surfactants. In fact, this radical is very selective for olefins and aromatics containing hydroxyl or amino groups.<sup>22</sup>

#### 4. Conclusion

The system Fe(III)/chlorine could produce reactive species capable of degrading textile dye at much higher rates than the chlorine alone. The principal advantages of this developed process are that is very easy to manipulate, not expensive, highly efficient in removing dyes and may be operated at pH relatively higher than that of Fenton-like system. The process is strongly sensitive to operational conditions. Optimum concentrations of chlorine and iron(III) have been obtained for the best performance of the process. Operating at higher temperature generated higher concentration of reactive species which accelerated markedly the degradation of pollutants. Analysis of the process efficacy in the presence of several mineral anions and organic additives indicated that some anions, i.e., nitrite and sulfite, and surfactants, i.e. adogen 464, drastically suppressed the chemical activity of the Fe(III)/chlorine process toward the degradation of pollutants. Beside, based on using some specific radical scavengers, the species involved in the degradation system were found to be mainly  $\text{Cl}_2^{\bullet-}$  radical. This radical is very selective and have longer lifetime than all other radicals formed in the system. Based on their properties,  $\text{Cl}_2^{\bullet-}$  reacts efficiently with textile dyes inducing higher removal rates. However, further analysis such as the identification of the degradation by-products is still necessary for the process viability. This task, together with the COD, TOC and toxicity analysis, will be conducted in the future.

We would like to notice that the initial objective of the present study was not to deepen into the reaction mechanism between Fe(III) and HClO and process cost, but to show for the first time that the system Fe(III)/chlorine has a potential application in the degradation of persistent organic dyes in aqueous media. Nevertheless, the reaction mechanism merits further deepening studies that will be conducted together with the economic analysis of the process (including process-cost comparison with Fe(II)/chlorine and Fe(III)/H<sub>2</sub>O<sub>2</sub>) in the near future.

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**Table 1.** Reaction mechanism for Fe(III)/chlorine system (Ref. 11, except reaction 1 and 2).

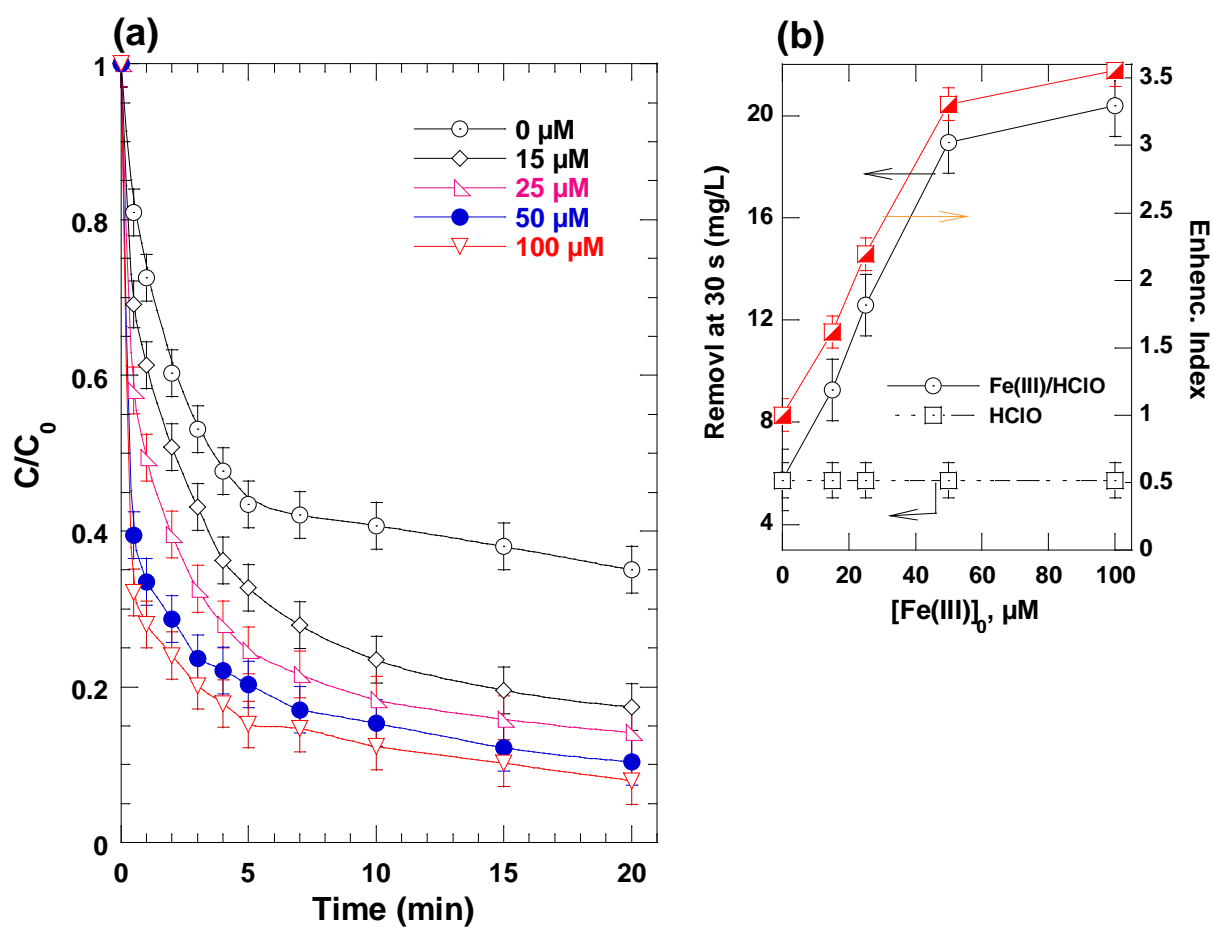
n°	Reaction	Rate constants (M <sup>-1</sup> s <sup>-1</sup> )
1	Fe(III) + HClO → Fe(II) + ClO• + H <sup>+</sup>	-
2	Fe(II) + HClO → Fe(III) + •OH + Cl <sup>-</sup>	~ 10 <sup>4</sup>
3	Fe(II) + HClO → Fe(III) + Cl• + OH <sup>-</sup>	~ 10 <sup>4</sup>
4	•OH + HClO → ClO• + H <sub>2</sub> O	2×10 <sup>9</sup>
5	Cl• + HClO → ClO• + H <sup>+</sup> + Cl <sup>-</sup>	3×10 <sup>9</sup>
6	Cl• + Cl <sup>-</sup> ⇌ Cl <sub>2</sub> • <sup>-</sup>	$k_7 = (0.65-2.1) \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$ , $k_{-7} = 6 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$
7	Cl• + H <sub>2</sub> O → HClO• <sup>-</sup> + H <sup>+</sup>	2.5×10 <sup>5</sup>
8	HClO• <sup>-</sup> ⇌ •OH + Cl <sup>-</sup>	$k_8 = 6.1 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ , $k_{-8} = 4.3 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$
9	HClO• <sup>-</sup> + H <sup>+</sup> → Cl• + H <sub>2</sub> O	2.1×10 <sup>10</sup>
10	HClO• <sup>-</sup> + Cl <sup>-</sup> → Cl <sub>2</sub> • <sup>-</sup> + OH <sup>-</sup>	1×10 <sup>5</sup>
11	Cl <sub>2</sub> • <sup>-</sup> + H <sub>2</sub> O → Cl <sup>-</sup> + HClO• <sup>-</sup> + H <sup>+</sup>	1×10 <sup>5</sup>
12	Cl <sub>2</sub> • <sup>-</sup> + •OH → Cl <sup>-</sup> + HClO• <sup>-</sup>	1×10 <sup>5</sup>
13	Fe <sup>2+</sup> + •OH → Fe <sup>3+</sup> + OH <sup>-</sup>	3.2×10 <sup>8</sup>
14	Fe <sup>2+</sup> + Cl <sub>2</sub> • <sup>-</sup> → Cl <sup>-</sup> + FeCl <sup>2+</sup>	1.4×10 <sup>7</sup>
15	Cl <sub>2</sub> • <sup>-</sup> + Cl <sub>2</sub> • <sup>-</sup> → Cl <sub>2</sub> + 2 Cl <sup>-</sup>	6.3×10 <sup>8</sup>
16	•OH + •OH → H <sub>2</sub> O <sub>2</sub>	5.5×10 <sup>9</sup>
17	Cl <sub>2</sub> • <sup>-</sup> + •OH → HClO + Cl <sup>-</sup>	1×10 <sup>9</sup>
18	Cl <sub>2</sub> • <sup>-</sup> + Cl• → Cl <sub>2</sub> + Cl <sup>-</sup>	2.1×10 <sup>9</sup>
29	Cl• + Cl• → Cl <sub>2</sub>	8.8×10 <sup>7</sup>
20	ClO• + ClO• → Cl <sub>2</sub> O <sub>2</sub>	7.5×10 <sup>9</sup>
21	ClO• + Cl• → HCl + HClO <sub>3</sub>	-

**Table 2.** Reactivity between scavengers and radicals in the Fe(II)/chlorine system.

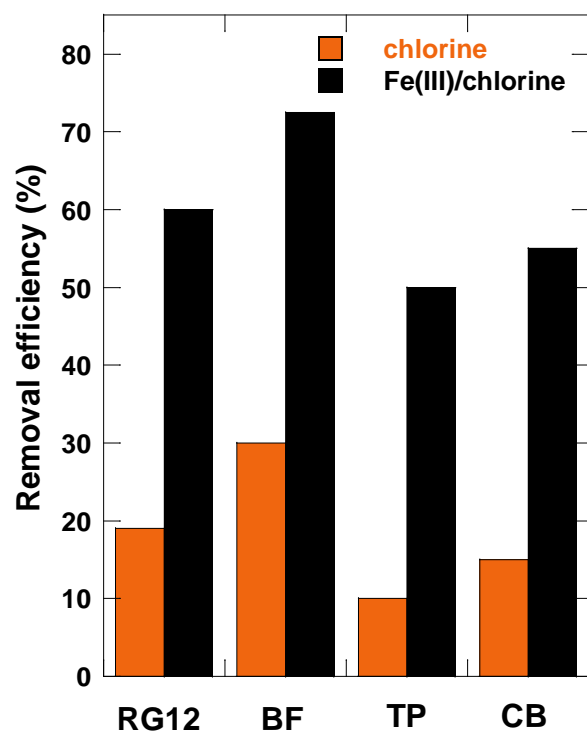
Scavenger	Rate constants $k$ ( $M^{-1} s^{-1}$ )			
	$\bullet OH$	$Cl\bullet$	$Cl_2\bullet^-$	$ClO\bullet$
Nitrobenzene (NB)	$3.9 \times 10^9$ <sup>a</sup>	<i>neg.</i> <sup>a</sup>	<i>neg.</i> <sup>a</sup>	<i>neg.</i> <sup>b</sup>
Benzoic acid (BA)	$1.8 \times 10^9$ <sup>a</sup>	$1.8 \times 10^{10}$ <sup>a</sup>	$(0.2-1.8) \times 10^6$ <sup>a,b</sup>	$< 3 \times 10^6$ <sup>c</sup>
Azide ions ( $N_3^-$ )	$1.4 \times 10^{10}$ <sup>d</sup>	$5.2 \times 10^9$ <sup>e</sup>	$(0.5-1.2) \times 10^9$ <sup>d,f</sup>	$2.5 \times 10^8$ <sup>c</sup>
t-butanol	$6 \times 10^8$ <sup>d</sup>	$3 \times 10^8$ <sup>d</sup>	0-700 <sup>g</sup>	$1.3 \times 10^7$ <sup>d</sup>
Phenol	$6 \times 10^8$ <sup>h</sup>	$(0.8-2.5) \times 10^9$	$(2.5-5) \times 10^{8b}$	NA*

a) Ref. <sup>17</sup>, b) Ref. <sup>18</sup>, c) Ref. <sup>30</sup>, d) Ref. <sup>22</sup>, e) Ref. <sup>31</sup>, f) Ref. <sup>23</sup>, g) Ref. <sup>32</sup>, Ref. <sup>33</sup>

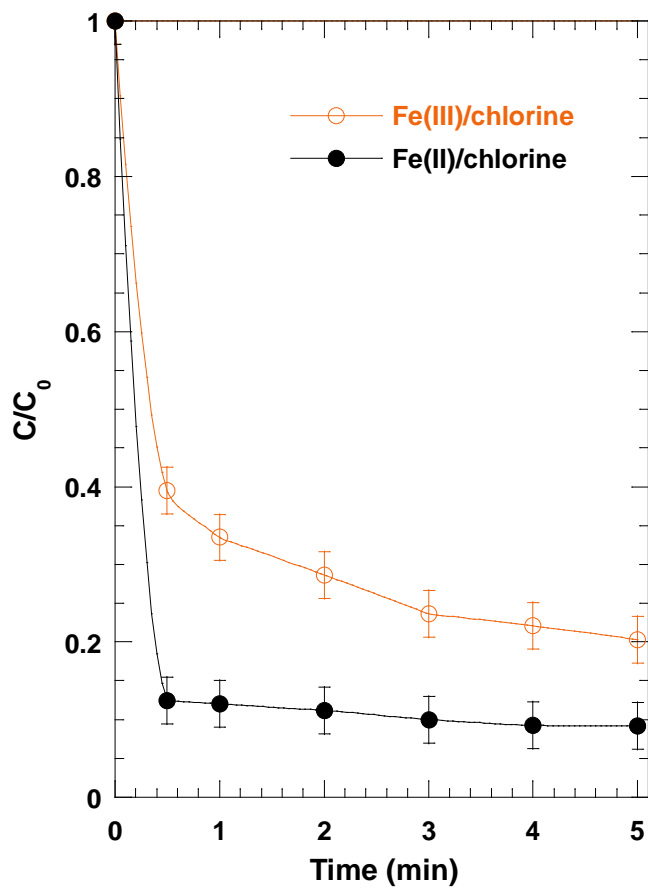
\* Not available, but phenol mostly reacts with all radicals with high rate constant <sup>23</sup>



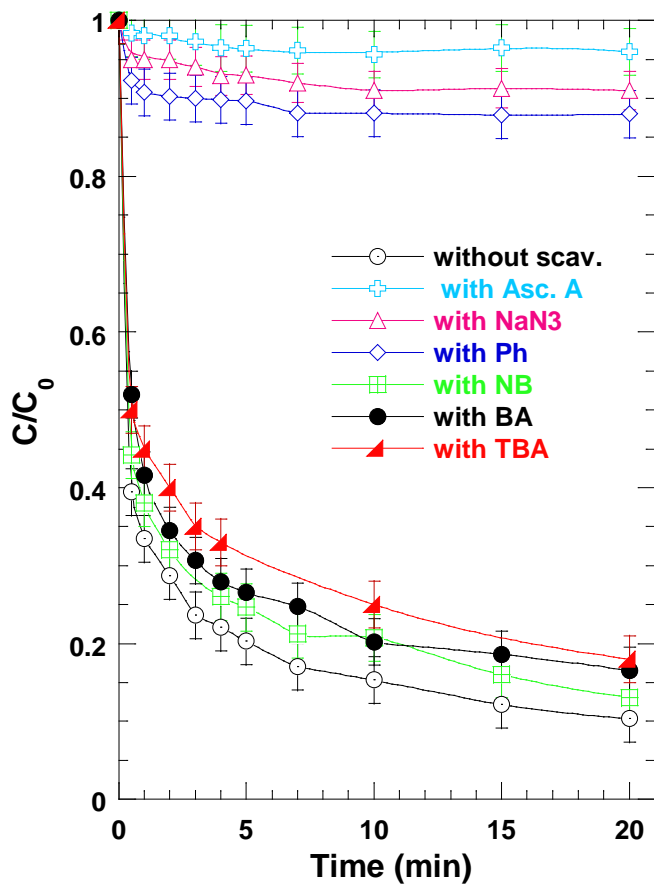
**Fig. 1.** Effect of initial Fe(III) concentration on the removal kinetics of RG12 with Fe(III)/chlorine system (conditions:  $V = 200$  mL,  $C_0 = 30$  mg/L ( $16.32 \mu\text{M}$ ),  $[\text{chlorine}]_0 = 250 \mu\text{M}$ ,  $[\text{Fe(III)}]_0 = 0\text{-}100 \mu\text{M}$ , pH 4, temperature =  $20 \pm 2$  °C). The insert represents the removed amount (in mg/L) after 30 s upon chlorine and Fe(III)/chlorine treatments as well as the enhancement index vs. initial Fe(III) dosage.



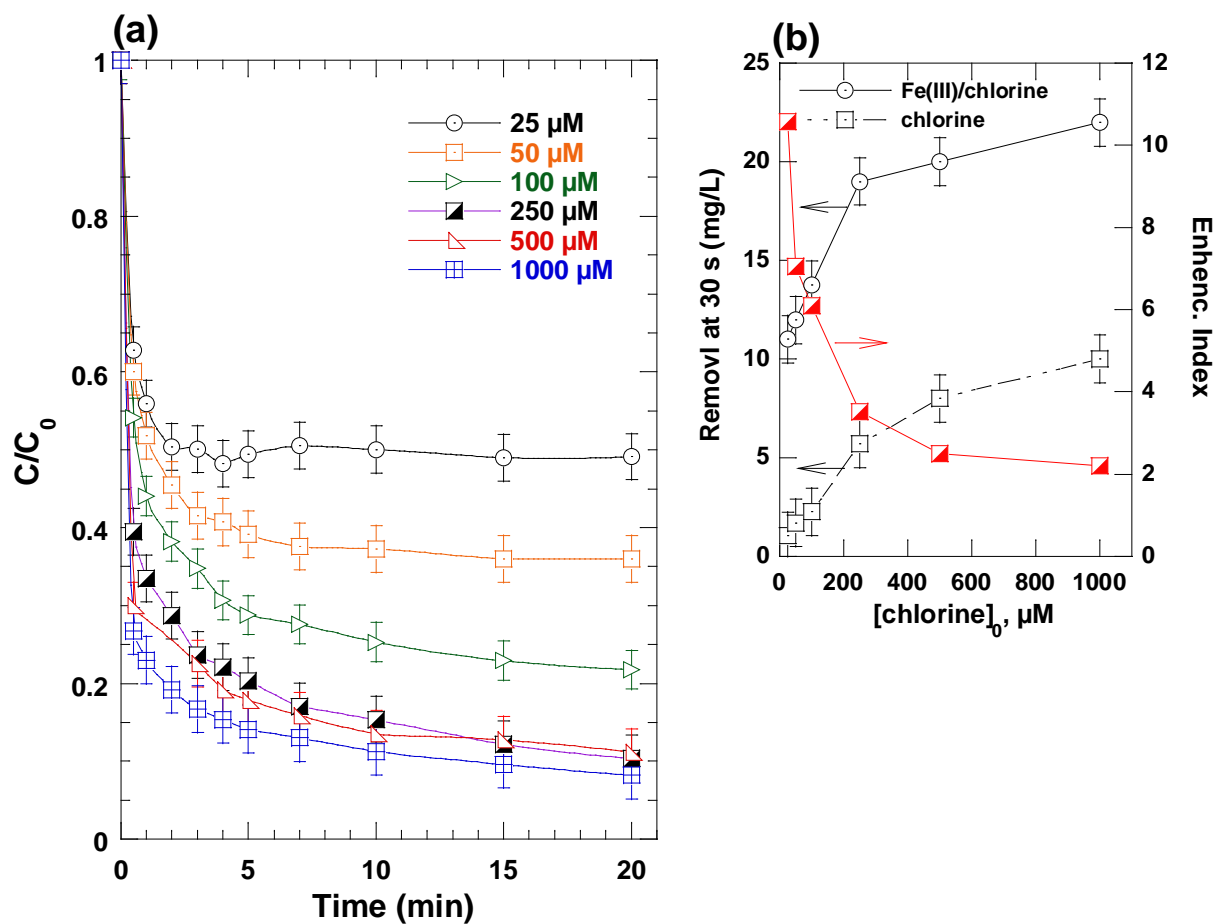
**Fig. 2.** Removal efficiency at 30 s for several dyes under chlorine alone and Fe(III)/chlorine process (conditions:  $C_0 = 16.32 \mu\text{M}$ ,  $[\text{Fe(III)}]_0 = 50 \mu\text{M}$ ,  $[\text{chlorine}]_0 = 250 \mu\text{M}$ , pH 4, temperature:  $20 \pm 2 \text{ }^\circ\text{C}$ ).



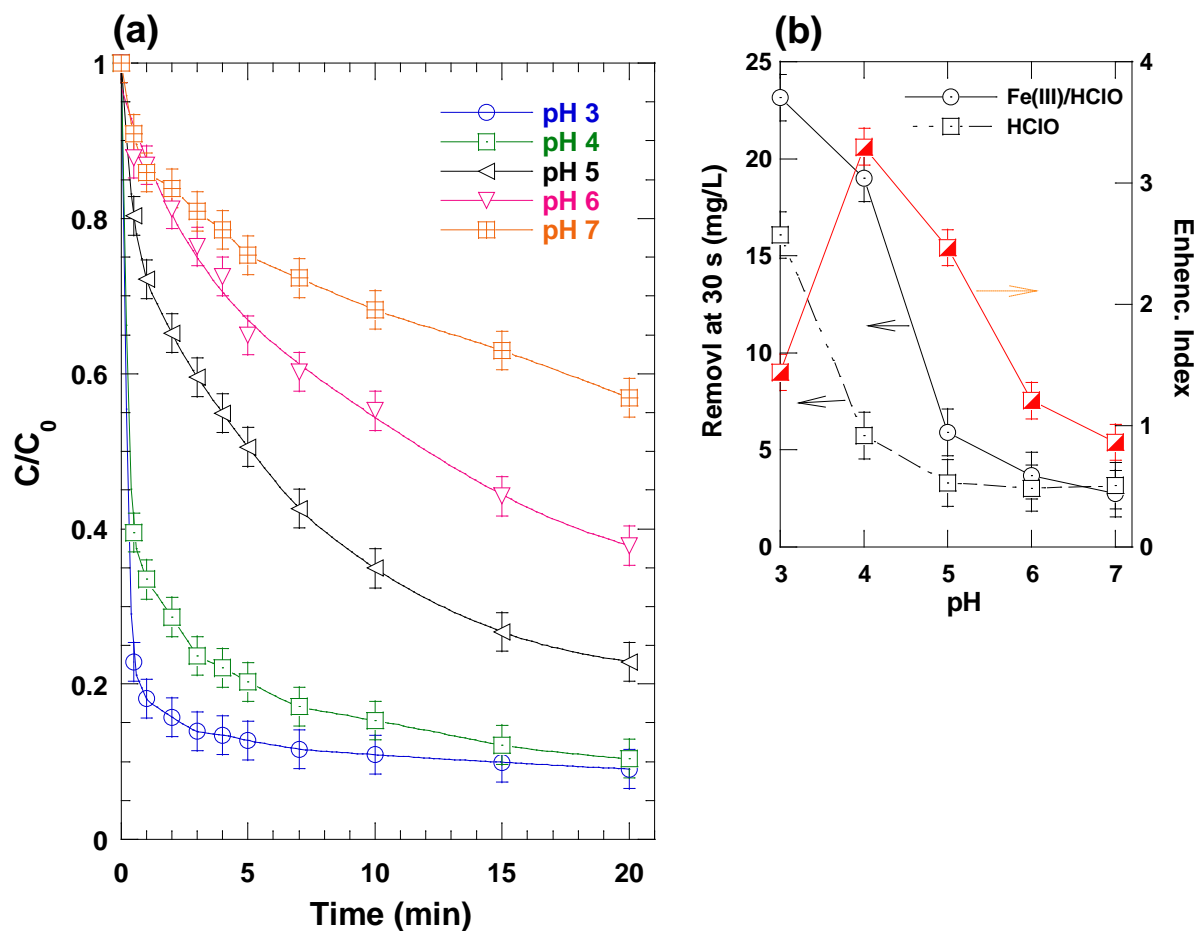
**Fig. 3.** Comparison of the effect of Fe(III)/chlorine and Fe(II)/chlorine treatments on the removal kinetics of RG12 (conditions:  $V = 200$  mL,  $C_0 = 30$  mg/L ( $16.32 \mu\text{M}$ ),  $[\text{Fe(III)}]_0 = [\text{Fe(II)}]_0 = 50 \mu\text{M}$ ,  $[\text{chlorine}]_0 = 250$  mM, pH 4, temperature:  $20 \pm 1$  °C).



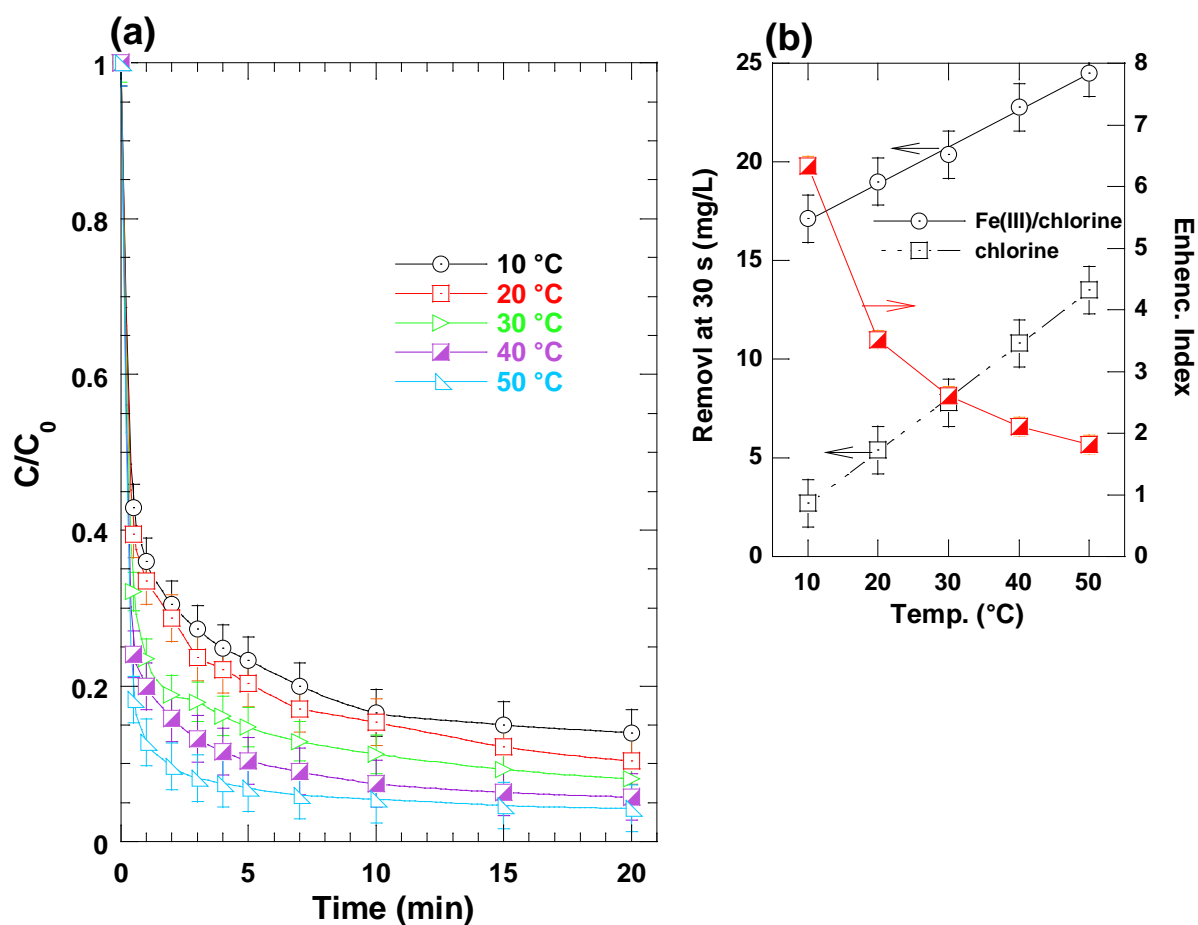
**Fig. 4.** Influence of specific radical scavengers on the degradation kinetics of RG12 by Fe(III)/HClO process (conditions:  $V = 200$  mL,  $C_0 = 30$  mg/L ( $16.32 \mu\text{M}$ ),  $[\text{chlorine}]_0 = 250 \mu\text{M}$ ,  $[\text{Fe(III)}]_0 = 50 \mu\text{M}$ , pH 4, temperature =  $20 \pm 2$  °C).



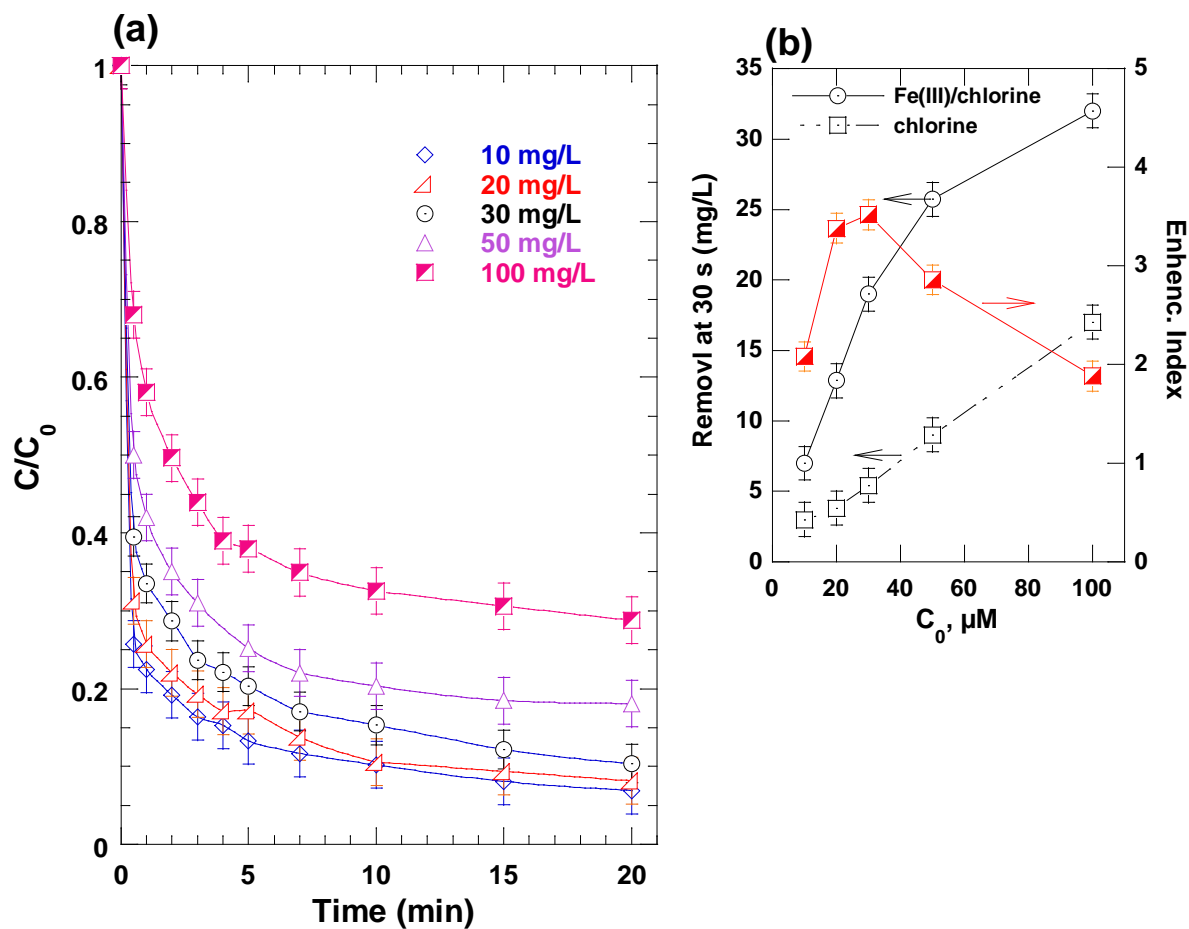
**Fig. 5.** Effect of initial chlorine concentration on the removal kinetics of TB upon Fe(III)/chlorine system (conditions:  $V = 200$  mL,  $C_0 = 30$  mg/L ( $16.32 \mu\text{M}$ ),  $[\text{chlorine}]_0 = 25$ - $1000 \mu\text{M}$ ,  $[\text{Fe(III)}]_0 = 50 \mu\text{M}$ , pH 4, temperature =  $20 \pm 2$  °C). The insert (Fig. 5b) represents the removed amount (in mg/L) after 30 s upon chlorine and Fe(III)/chlorine treatments as well as the enhancement index vs. initial chlorine dosage.



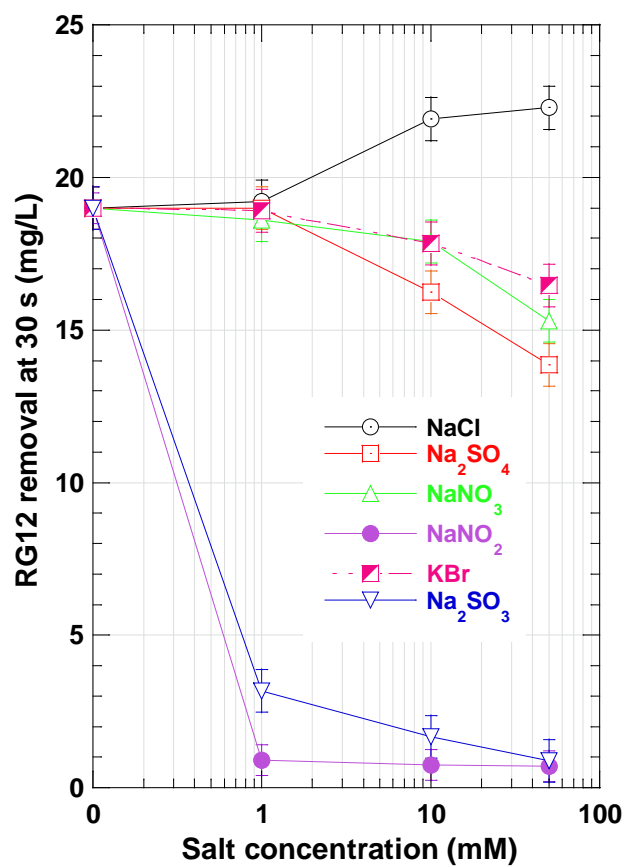
**Fig. 6.** Effect of initial solution pH on the removal kinetics of RG12 upon Fe(III)/chlorine system (conditions:  $V = 200$  mL,  $C_0 = 30$  mg/L ( $16.32 \mu\text{M}$ ),  $[\text{Fe}^{2+}]_0 = 50 \mu\text{M}$ ,  $[\text{chlorine}]_0 = 250 \mu\text{M}$ , pH 3–7, temperature:  $20 \pm 1$  °C). The insert (Fig. b) represents the removed amount (in mg/L) after 30 s upon chlorine and  $\text{Fe}^{2+}$ /chlorine treatments as well as the enhancement index vs. initial solution pH.



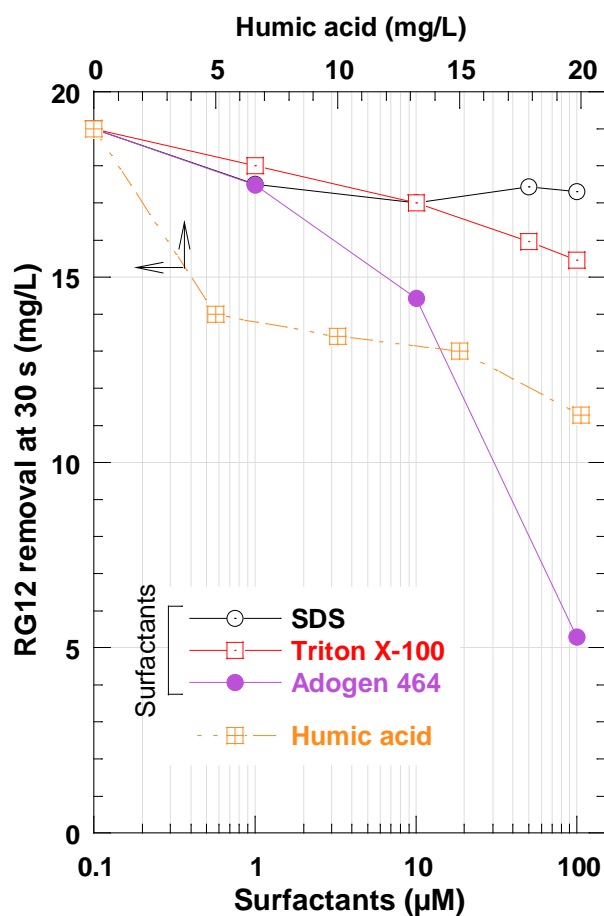
**Fig. 7.** Effect of liquid temperature on the removal kinetics of RG12 upon Fe(III)/chlorine system (conditions:  $V = 200$  mL,  $C_0 = 30$  mg/L ( $16.32 \mu\text{M}$ ),  $[\text{chlorine}]_0 = 250 \mu\text{M}$ ,  $[\text{Fe(III)}]_0 = 50 \mu\text{M}$ , pH 4, temperature = 10-50 °C). The insert represents the removed amount (in mg/L) after 30 s upon chlorine and  $\text{Fe}^{2+}$ /chlorine treatments as well as the enhancement index vs. liquid temperature.



**Fig. 8.** Effect of initial RG12 concentration on the removal kinetics upon Fe(III)/chlorine system (conditions:  $V = 200$  mL,  $C_0 = 30$  mg/L ( $16.32 \mu\text{M}$ ),  $[\text{chlorine}]_0 = 250 \mu\text{L}$ ,  $[\text{Fe(III)}]_0 = 50 \mu\text{M}$ , pH 4, temperature =  $20 \pm 1$  °C). The insert represents the removed amount (in mg/L) after 30 s upon chlorine and Fe(III)/chlorine treatments as well as the enhancement index vs. initial RG12 concentration.



**Fig. 9.** Salts effect on RG12 removal after 30 s of treatment with Fe(III)/chlorine (conditions:  $C_0 = 30 \text{ mg/L}$  ( $16.32 \mu\text{M}$ ),  $[\text{HClO}]_0 = 250 \mu\text{L}$ ,  $[\text{Fe}^{2+}]_0 = 50 \mu\text{M}$ ,  $[\text{salts}]_0 = 0\text{-}50 \text{ mM}$ , pH 4 except for  $\text{NaHCO}_3$  (pH 8.5), temperature =  $20 \pm 2 \text{ }^\circ\text{C}$ ).



**Fig. 10.** Impact of humic acid and surfactants on RG12 removal after 30 s of treatment with Fe(III)/chlorine (conditions:  $C_0 = 30$  mg/L (16.32  $\mu$ M),  $[\text{HClO}]_0 = 250$   $\mu$ L,  $[\text{Fe}^{2+}]_0 = 50$   $\mu$ M,  $[\text{surf}]_0 = 1$ -100  $\mu$ M,  $[\text{HA}]_0 = 5$ -20 mg/L, pH 4 except for  $\text{NaHCO}_3$  (pH 8.5), temperature =  $20 \pm 2$   $^\circ\text{C}$ ).