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**Author/s:**

Ren, J;Zhang, L;San Nicolas, R

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# Degradation of alkali-activated slag/fly ash mortars under different aggressive acid conditions

Jie Ren<sup>1</sup>, Lihai Zhang<sup>1</sup>, Rackel San Nicolas<sup>1\*</sup>

<sup>1</sup> Department of Infrastructure Engineering, the University of Melbourne, Victoria, 3010, Australia

## Abstract

Acidic environments constitute serious chemical threats to concrete-like cementitious materials. The purpose of this study is to experimentally investigate the degradation of alkali-activated slag/fly ash mortars with different slag/fly ash ratios: 80/20, 60/40 and 40/60 in acidic environments. Mortar samples were exposed to three different types of aggressive acidic solutions: phosphoric acid, sulphuric acid and a mixture of phosphoric acid and sulphuric acid maintained at a constant pH value of  $2.5 \pm 0.5$  for a period of 150 days. Results showed that in the case of alkali-activated mortars, the aggressivity of the phosphoric acid alone is greater compared to the other acidic solutions. An optimum ratio of slag/fly ash was identified as a higher resistance against the three types of acidic environments studied here. Further, the degradation process of alkali-activated mortars seems to be different than the one observed on OPC, there are two clear stages. By using a combination of the Hill function and the Fick's second law a first model of degradation is proposed in this study. Finally, the results of theoretical analysis predicted that the degradation depth of alkali-activated slag/fly ash mortars exposed to sulphuric acid environment for 50 years could be reduced by about 52% - 60% compared to that of an OPC-based mortars.

**Key words:** Degradation depth, Alkali-activated slag/fly ash blended mortar, Sulphuric acid, Phosphoric acid, phosphoric and sulphuric acid mixture, Diffusion coefficient; Hill function

## 1. Introduction

A vast amount of Ordinary Portland cement (OPC)-based concrete has been used as construction materials for sewer and wastewater systems. However, the exposure of alkaline building materials such as OPC concretes to acid-rich aggressive environments leads to severe degradations [1, 2]. In the acid-rich environments, hydronium ions ( $H_3O^+$ ) penetrate alkaline materials such as OPC-based concrete, inducing a significant pH reduction of pore solutions [3]. If the exposition continues, further dissolution and/or decomposition of various components such as Portlandite and C-S-H gel in the bulk materials

50 would occur and some calcium salts such as gypsum would be formed, worsening many mechanical  
51 properties, such as reduced compressive and flexural strength [4-7]. Thus the service life of concretes  
52 is reduced and considerable expenditure for repair and maintenance occurs as a result of degradations.  
53 It was predicted that it may cost the United States 390 billion dollars over the next two decades to repair  
54 current-in-service wastewater infrastructures [8] and the annual cost of operation and maintenance  
55 related to the wastewater infrastructure is more than 25 billion dollars [9].

56 Among all different types of concrete degradation caused by acid-laden sewer environments such as  
57 silage effluent, the degradation of various cementitious materials resulting from chemical and  
58 biochemical sulphuric acid has been extensively investigated in the last few decades [8, 10-14].  
59 However, phosphoric acid induced degradation of concretes due to the coexistence of hydroniums  
60 ( $H_3O^+$ ) released from various acids and large concentration of phosphates has not been much  
61 investigated and the relevant research in this area is quite limited [8, 15-17]. The available literature  
62 compared the aggressiveness of phosphoric acid and citric acid but without exploring related  
63 mechanisms of phosphoric acid degradation process [16]. In addition, almost all of the current literature  
64 focuses on the effect of one single acid, e.g. sulphuric or nitric acid, on the degradation performances  
65 of alkaline cementitious materials without considering the possible different **effects** of mixed acids [18-  
66 24]. However, different acids usually coexist in sewage systems due to the presence of different anions  
67 such as sulphates, phosphates, nitrate etc. and hydroniums in acidic conditions [17]. Thus, an  
68 investigation of the degradation performance of cementitious materials exposed to mixed acid solutions  
69 which is closer to real-life situations is required **to** draw a more convincing conclusion.

70 Alkali-activated materials (AAMs) are a class of binders prepared using different precursors as **raw**  
71 **materials** instead of using OPC [25]. These precursors are mixed together with **various alkaline**  
72 **activators** to provide necessary strong alkaline conditions for dissolution of precursors and the  
73 condensation catalysing processes [26]. Currently, AAMs are considered as an appealing alternative  
74 to OPC-based materials **due to their much lower carbon footprint and comparable mechanical**  
75 **properties [15, 27, 28] as compared to OPC-based binders**. In addition, both the activation of calcium-  
76 rich slag or low-calcium materials, such as fly ash **(FA) and metakaolin**, can provide **higher** resistance  
77 to aggressive environments such as acid attacks **than** that of OPC-based binders [29, 30] due to their  
78 distinctive chemical compositions and microstructures [31, 32]. The major components for slag-based  
79 and fly ash (FA)-based binders are C-(A)-S-H ( $CaO-Al_2O_3-SiO_2-H_2O$ )-type gel and N-A-S-H ( $Na_2O-$

80 Al<sub>2</sub>O<sub>3</sub>-SiO<sub>2</sub>-H<sub>2</sub>O)-type gel, respectively. It was showed that slag-based AAMs had a better performance  
81 compared to OPC-based peers under sulphuric acid and acetic acid attacks [33, 34]. The authors [33,  
82 34] attributed this relatively high durability mainly to the lower Ca/Si ratio of the binder matrix because  
83 of the absence of Ca(OH)<sub>2</sub> (Portlandite) in the composition of this type of AAMs and an extremely low  
84 permeability. For FA-based AAMs, the main reaction product (N-A-S-H) is a three-dimensional highly  
85 crosslinking network with low Ca content, contributing to higher resistance in acid solutions as  
86 compared to OPC-based binders [34-37]. Furthermore, alkali-activated slag/fly ash (AASF) binders are  
87 becoming more appealing due to some favourable combinations of the properties that cannot be  
88 achieved by the activation of one single precursor [38-43]. A high degree of cross-linked binder  
89 displaying a coexistence of C-(A)-S-H and N-A-S-H [44], either present as a single phase or a hybrid-  
90 type gel known as C-(N)-A-S-H gel in some studies, was observed when slag and fly ash were mixed  
91 together [45]. According to Lloyd et al.[46], the addition of slag into the FA-based AAMs increased the  
92 resistance towards the sulphuric acid attack with a pH at 1.0. However, another literature [23] found  
93 that increasing slag contents has a negative impact on the resistance of FA-based AAMs due to a  
94 higher content of calcium which is unfavourable regarding the acid resistance. The seemingly  
95 controversial outcomes can be explained by considering different roles the C-A-S-H and N-A-S-H play  
96 in terms of acid resistance. C-A-S-H has a space-filling effect in the binder, leading to a reduced porosity  
97 as slag content increases [23, 47]. However, C-A-S-H contains more Ca than N-A-S-H type gel which  
98 makes it more susceptible towards acid attacks via decalcification process. Therefore, a trade-off  
99 between the amount of slag and FA used for making AASF samples is required to optimise the durability  
100 performance of AASF binders.

101 Currently, a main hurdle preventing AAMs from wider applications is the lack of data and reports on  
102 the long-term behaviour of these materials that can prove satisfactory durability throughout their overall  
103 life-cycles [48, 49]. In order to allow more rapid adoption of AAMs as an alternative to OPC-based  
104 binders, to get reliable results which can be used for the quantification of AAMs' long service life is  
105 critical [6, 14, 23, 24, 46, 50, 51]. Among many parameters, degradation depth provides useful  
106 information on rate-controlling processes of concrete materials. Therefore it is often used as a reliable  
107 indicator for corrosion kinetics and long-term risk predictions [46]. In some studies, degradation depth  
108 is also considered as 'altered depth', 'neutralization depth' or even 'corrosion depth' [52-55].  
109 'Degradation depth' is used in this study for consistency.

110 A few studies have been conducted to measure the degradation depths of OPC-based binder or  
111 AAMs after immersion in various acidic solutions and related degradation mechanisms were also  
112 proposed [3, 46, 53, 56-59]. The experiment work of Lloyd et al. [46] revealed that the degradation  
113 depth is a more reliable method to assess the degradation kinetics, particularly for AAMs compared to  
114 mass loss. According to the experimental results, a linear relationship between the degradation depth  
115 and exposure time indicates a chemical reaction-controlled process [60] whereas a linear increase in  
116 the degradation depth over the square root of time implies that the degradation is mainly controlled by  
117 diffusion [46].

118 Earlier, Kawai et al. [58] exposed OPC-based concrete to sulphuric acid solution with pH at 1.0 and  
119 2.0 respectively to investigate the degradation of concrete specimens under acid fluid flow over sample  
120 surfaces. Their results showed that there is a positive linear relationship between the degraded depth  
121 and exposure time, indicating a chemical-controlled process. This is due to the removal of the degraded  
122 layer and calcium salts by fluid flow. Other relevant experimental studies also reported that, when  
123 immersed in nitric acid, a highly porous degraded layer providing little protection for acid ingress led to  
124 a higher degradation rate (almost linear increase in the degradation depth over time when the pastes  
125 were completely dissolvable). In comparison, a compact and dense layer rich in silica after degradation  
126 resulted in a lower rate of degradation [56].

127 In conclusion, the initial stage of degradation is usually a chemical-reaction controlled process due  
128 to direct reactions between cementitious binders and exposed acids. However, the later process can  
129 be either reaction-controlled (porous/no intact degraded layer or degraded layer erased by external  
130 forces) or diffusion-controlled (dense and intact degraded layer). It is clear that based on the  
131 experimental results and general trends provided by degradation depth development, long-term  
132 behaviours of cementitious binders subjected to acid attacks could be predicted [51]. However, related  
133 research on studying the degradation depth of AAMs or OPC-based binders exposed to phosphoric  
134 acid solutions and predicting their long-term performances [16, 61, 62] is quite rare.

135 Therefore, the purpose of this study is to investigate the degradation processes of different mixtures  
136 of AAMs, specifically AASF, with three slag/FA ratios under various acid conditions: phosphoric acid,  
137 sulphuric acid and a mixture of phosphoric acid and sulphuric acid. Degradation depth was used as the  
138 parameter to assess the degradation process and kinetics. A series of theoretical simulations were then

139 carried out to further predict the long-term degradation behaviours of AASF binders and to compare  
140 their behaviours with those of OPC-based peers.

## 141 2. Experimental methods

### 142 2.1. Materials

143 The chemical compositions and properties of the slag, specifically ground granulated blast furnace  
144 slag (denoted as 'GGBFS' hereafter) and fly ash both from Australia are shown in Table 1. GGBFS  
145 used has a specific gravity of 2,800 kg/m<sup>3</sup> and Blaine fineness of 410 ± 10 m<sup>2</sup>/kg. The particle size  
146 range, determined by laser granulometric analysis, was 0.1–74 µm, with a d<sub>50</sub> of 14 µm. The specific  
147 gravity and d<sub>50</sub> of fly ash is 2200 kg/m<sup>3</sup> and 25 µm, respectively. The silica sand (milled quartz) as fine  
148 aggregate with a specific gravity of 2550 kg/m<sup>3</sup> and water absorption of 0.90 % was used. Commercial  
149 solid anhydrous sodium metasilicate powder (Na<sub>2</sub>SiO<sub>3</sub>) with a chemical composition of 49.1 % wt.%  
150 SiO<sub>2</sub> and 50.9 wt.% Na<sub>2</sub>O (a molar ratio of SiO<sub>2</sub>/Na<sub>2</sub>O at 1.0) is supplied by Zeobond Pty. Ltd.

151  
152 Table 1. Chemical compositions of the FA and GGBFS used, as determined by X-ray fluorescence.

Oxide (wt %)	SiO <sub>2</sub>	TiO <sub>2</sub>	Al <sub>2</sub> O <sub>3</sub>	Fe <sub>2</sub> O <sub>3</sub>	MnO	MgO	CaO	K <sub>2</sub> O	P <sub>2</sub> O <sub>5</sub>	SO <sub>3</sub>	LOI
GGBFS	31.00	0.49	13.96	0.32	0.33	6.33	40.92	0.31	0.01	2.17	2.11
FA	42.09	1.44	25.13	13.16	0.18	1.27	13.56	0.41	1.10	0.41	0.81

153 LOI is loss on ignition at 1,000 °C.  
154

155 Three sets of alkali-activated mortars were produced with different GGBFS/FA ratios, as shown in  
156 Table 2. The mortar samples were formulated using different water-to-binder ratios (w/b) and amounts  
157 of alkaline activator to reach similar target compressive strengths (around 60 ± 5 MPa) after 56-day  
158 curing before immersion in acidic solutions to obtain a meaningful comparison. These dosages have  
159 been identified as the most suitable formulation to promote acceptable setting times and desirable  
160 structural evolutions [44, 63]. The sand to binder ratio is 2:1 by weight for all sample mixes. The water  
161 used for mixing the mortar and preparing activator solutions was purified distilled water. The activator,  
162 anhydrous sodium metasilicate (Na<sub>2</sub>SiO<sub>3</sub>), was weighed and dissolved completely in distilled water  
163 followed by cooling down to room temperature at 23 ± 2 °C before addition. Mortar samples were cast  
164 and compacted into cylinder moulds (Φ 27.5 mm × H 55 mm) in two layers of equal height using a  
165 tamping rod followed by being vibrated via a vibrating table for another 2 minutes to release air bubbles.  
166 The specimens namely, 80Slag\_20FA, 60Slag\_40FA, were cured at room temperature (23 ± 2 °C) with  
167 a plastic film covered on them for 24 hours before they were demoulded to minimize moisture loss. The

168 40Slag\_60FA sample was cured under hydrothermal water bath conditions (temperature at 70 °C, RH  
 169 = 95 ± 5 %) in a laboratory-grade oven wrapped with a vacuum plastic bag for seven days. After that,  
 170 they were taken out of the oven, cooled down at room temperature (23 °C) and demoulded. After  
 171 demoulding, all samples were sealed tightly and kept in ambient conditions (room temperature 23 ± 2  
 172 °C) until the next stage of the experiment. The modified curing regime used for the 40Slag\_60FA sample  
 173 was employed to reach the **target strength** after 56 days [61]. A fully cured cylindrical sample is  
 174 presented in Fig. 1(a).

175 Table 2. Mixture designs of the mortar samples tested in the study.

Sample ID	Specifications (Mix proportions)			
	GGBFS/FA ratio (%) <sup>a</sup>	Activator/Binder ratio (%) <sup>a</sup>	Water/Binder ratio <sup>a</sup>	Sand/Binder ratio <sup>a</sup>
80Slag_20FA	80:20	7.0	0.40	2:1
60Slag_40FA	60:40	7.5	0.38	2:1
40Slag_60FA	40:60	8.5	0.34	2:1

176 <sup>a</sup>All values are given as mass ratios.

177  
 178 Three aggressive acid solutions, namely phosphoric acid (diacid in aqueous solution), sulphuric acid  
 179 (strong diprotic acid) and the phosphoric acid and sulphuric acid mixed solution were made by adding  
 180 laboratory grade acids into distilled water. The pH of the three different acids was all manually controlled  
 181 at around 2.5 ranging between 2.0 and 3.0. The phosphoric acid solution was made by diluting 1,000  
 182 times of the original analytical reagent phosphoric acid provided by Chem-supply (85% w/w, 1.71 g/mL)  
 183 to 14.82 mM (0.085%, 0.015 mol/L). The sulphuric acid solution was prepared by diluting the original  
 184 reagent grade sulphuric acid supplied by Scharlau, UN (95-97% w/w, 1.84 g/mL) with a 4,000-fold to  
 185 4.69 mM (0.005 mol/L, 0.024% w/w). The mixed acid was made by mixing the prepared phosphoric  
 186 acid and sulphuric acid solution together with a 1:1 ratio in volume. The initial pH of the phosphoric and  
 187 sulphuric mixed acid was slightly higher than the other two single acid solutions because phosphoric  
 188 acid is partially ionised and its ionization would be, to some extent, inhibited by the complete  
 189 dissociation of sulphuric acid. However, the hydronium ions which can be dissociated from the  
 190 phosphoric and sulphuric mixed acid with volume ratio of 1:1 are readily available. Therefore, the  
 191 phosphoric and sulphuric mixed acid can represent the scenario where phosphoric and sulphuric acid  
 192 are mixed together with similar pH as the other two pre-mixed single acids. The details of the three acid  
 193 solutions are shown in Table 3.

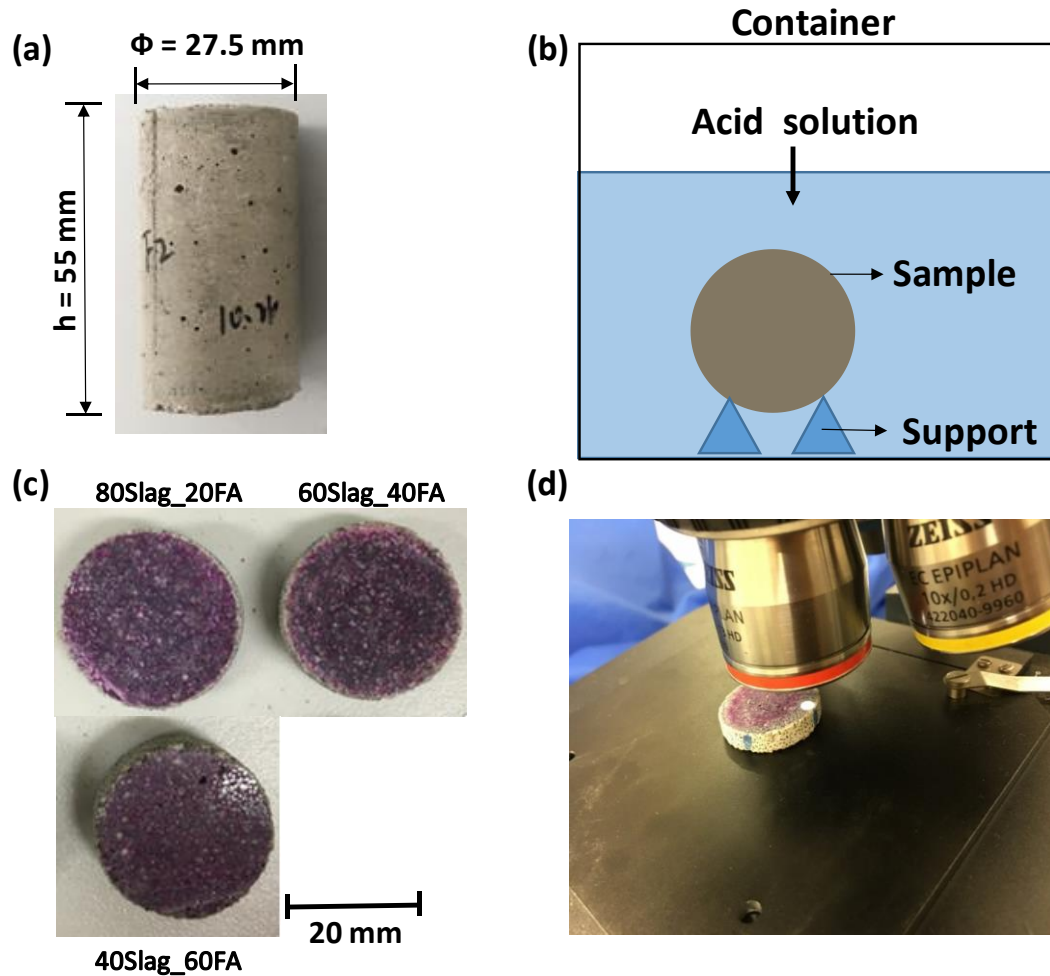
194 Table 3. The **detailed information** on the **three aggressive** acid solutions in which the samples were  
 195 immersed for 150 days.

Sample ID	Acid solution types (pH = 2.5 ± 0.5)		
	Phosphoric acid	Sulphuric acid	Phosphoric + sulphuric acid
80Slag_20FA	14.83 mM	4.69 mM	7.42 mM (P) + 2.35 mM (S)
60Slag_40FA	14.83 mM	4.69 mM	7.42 mM (P) + 2.35 mM (S)
40Slag_60FA	14.83 mM	4.69 mM	7.42 mM (P) + 2.35 mM (S)

196 Note: 'P' and 'S' stands for reagent-grade phosphoric acid and sulphuric acid, respectively. Notation  
197 (mM: mmol/L).

198  
199 **2.2. Methods**

200 Samples after 56 days of curing were fully immersed in the three acid solutions while keeping the  
201 solid surface/liquid volume ratio constant at 0.30 cm<sup>-1</sup>. The vertical distance between liquid levels of the  
202 acid solution and top surfaces of the samples was kept no less than 10 mm to ensure a complete  
203 immersion which can minimize possible carbonation induced by CO<sub>2</sub> from the air. Each sample was  
204 supported on two plastic holders to maximize the contact area between the sample surface and acid  
205 solution shown in Fig. 1(b). To keep the pH of all acid solutions constant, the pH values were monitored  
206 using a portable pH-meter (PHM210 Radiometer, Australia) and solutions were renewed every day in  
207 the first 7 days followed by a gradually decreased frequency of renewals until the end of the experiment  
208 (after 7 days, the solutions were replaced every second day for 21 days and every 3 days for another  
209 21 days. After 49 days, the acid solutions were renewed every 7 days until the end of the immersion  
210 period). The renewal frequency was pre-determined based on previous preliminary studies which  
211 indicated that the number of pH adjustment could be reduced as the immersion period proceeds [54].  
212 Each time when the solutions were renewed, samples were also rinsed slightly with distilled flowing  
213 water for a few seconds to represent the actual practical conditions that construction materials might  
214 encounter in sewage systems [64]. The acid solutions were allowed to stand without any mixing to  
215 simulate the static environments observed in tanks and sewer pipes containing agro-industrial effluents  
216 [65].



217

218 **Fig. 1. The detailed experimental procedures: (a) A cylindrical sample used for the acid immersion; (b) A**  
 219 **schematic representation of the experimental setups; (c) Cross sections of all sample mixes after 90-day**  
 220 **immersion in sulphuric acid; (d) Measurement of degradation depths using an optical video-microscope after**  
 221 **7, 28, 56, 90, 120 and 150 days of immersion.**

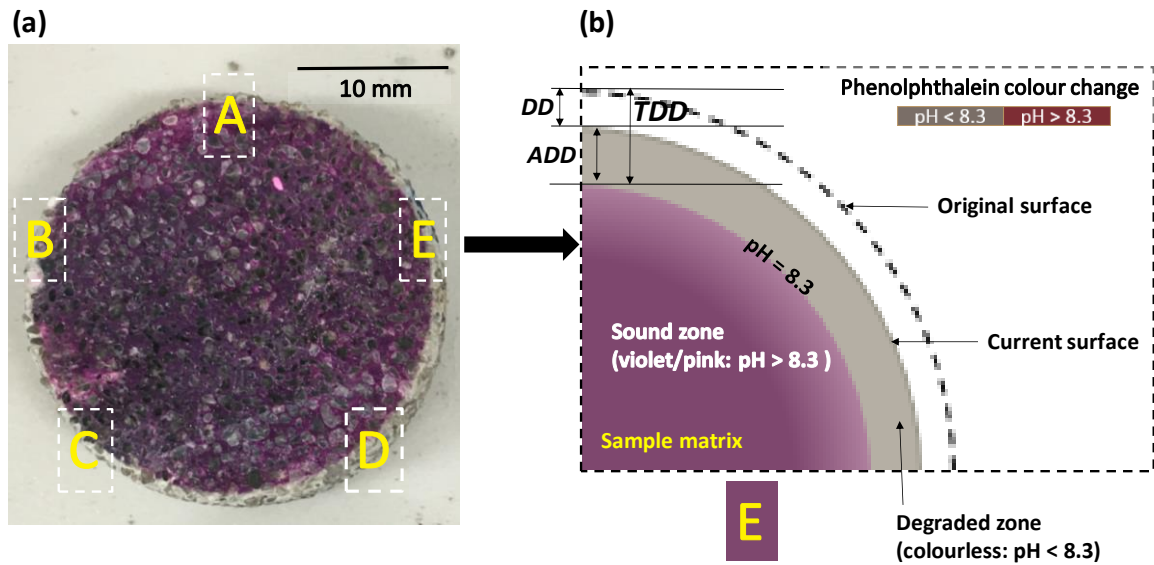
222 A simple description of all experimental details is shown in Fig. 1. Fig. 1(a) represents a cylindrical  
 223 mortar sample after 56 days of curing. Fig. 1(b) shows the sample orientations for acid immersion test.  
 224 Fig. 1(c) and (d) give information about the procedures of degradation depth measurements.

225 Compressive strength test was performed on cubic mortar samples (50 × 50 × 50 mm) in triplicates  
 226 according to ASTM C109M [66] after 56-day curing prior to acid exposure.

227 The initial water absorption (%), volume of permeable voids (%) (VPV) and capillary sorptivity  
 228 (mm/min<sup>0.5</sup>) of all samples were obtained by taking related tests according to ASTM C642-06 [67] and  
 229 ASTM C1585-04 [68]. All tests were conducted on cylinder samples (27.5 mm in diameter and 55 mm

230 in height) right after 56-day curing regime. Due to the preconditioning drying effect [69] on the alkali-  
231 activated binders, 70 °C was selected for oven-drying of the specimens until a constant mass was  
232 obtained. This process took about 4-5 days before reaching a constant mass. The 70 degree oven-  
233 drying temperature was used based on the study of Ismail et al.[69] because possible microstructural  
234 changes of AAM samples could happen under a relatively high temperature (e.g. 110 °C) suggested by  
235 the ASTM C642-06 [69]. Water absorption and VPV provide information about total volumes of various  
236 voids. Capillary sorptivity is one of the most important microstructural properties that characterises the  
237 durability of materials because it reflects the tendency of binders to absorb and transmit water or other  
238 liquids by capillary action [6] during the initial stage of absorption. In this study, hydroniums in water  
239 penetrate into the samples along with the water ingress.

240 Degradation depth was measured using an optical microscope along the immersion process after 7,  
241 28, 56, 90, 120 and 150 days of exposure, as an indicator of degradation kinetics. Three cylinders of  
242 each formulation were used to obtain the final averaged degradation depth. A disk of samples was cut  
243 perpendicularly to its axis by a diamond saw and then the disks were cleaned with water. In order to  
244 get a flat surface, each sample was polished on a sanding belt for 2 minutes with 120 grit sand paper  
245 and then dried in ambient environment with compressed air. A phenolphthalein solution (1 g  
246 phenolphthalein dissolved in 70 mL 95 % ethanol solution mixed with 100 mL distilled water) was then  
247 sprayed onto the newly-cut flat plane sections as an indicator of the degradation depth. The colourless  
248 area indicates that the pH dropped to below 8.3 and is considered as degraded [28]. The magenta-  
249 coloured region indicating a pH higher than 10.0 is considered as no damage occurred. There are some  
250 areas with light magenta/pink colour referring to a pH between 8.3-10.0. In this study, only the  
251 uncoloured area is regarded as the degraded part. Pictures were then taken by the optical-video  
252 microscope and processed in MATLAB to precisely calculate the apparent degradation depth (*ADD*).  
253 The diameter was also measured at the same time for each testing interval as the diameters of cross  
254 section was decreased due to partial dissolution of samples during the acid deterioration process [54].  
255 The dissolved depth (*DD*) can be deduced from the formula:  $DD = (\varphi_{ini} - \varphi_t)/2$  where  $\varphi_{ini}$  is the  
256 initial diameter of the samples and  $\varphi_t$  is the diameter at each time interval  $t$ . The total degradation depth  
257 (*TDD*) is a numerical sum of *ADD* and *DD*. A presentation of the identification of different depths is  
258 shown in Fig. 2.



259

260 **Fig. 2. Definitions of different parts involved in the degradation depth measurement. (a) A slice cut from a**  
 261 **sample after 120-day immersion in the phosphoric and sulphuric mixed acid with phenolphthalein sprayed on**  
 262 **the surface; (b) A schematic representation showing the identification of degradation depth at region 'E' (TDD**  
 263 **- Total Degradation Depth, ADD - Apparent Degradation Depth, DD - Dissolved Depth). 'A'-'E' are several**  
 264 **points selected around the peripheries of the sample for ADD measurements.**

265

### 266 3. Results and Discussion

#### 267 3.1. Properties before immersion

268 All compressive strengths after 56 days of curing were around 60 MPa as the results shown in Table  
 269 4. Based on the similar compressive strength, a meaningful comparison of the acid resistance of  
 270 different sample mixtures was carried out. The results of water absorption, VPV and capillary sorptivity  
 271 test prior to acid immersion are also shown in Table 4.

272 Table 4. The compressive strength and porous properties of the mortar samples prior to the exposition  
 273 to acid solutions.

Sample ID	Compressive strength (MPa)	Water absorption (%)	VPV (%)	Capillary sorptivity (mm/min <sup>0.5</sup> )
80Slag_20FA	57.7	9.2	19.4	0.33
60Slag_40FA	57.7	7.3	17.3	0.17
40Slag_60FA	61.4	6.6	13.3	0.09

274

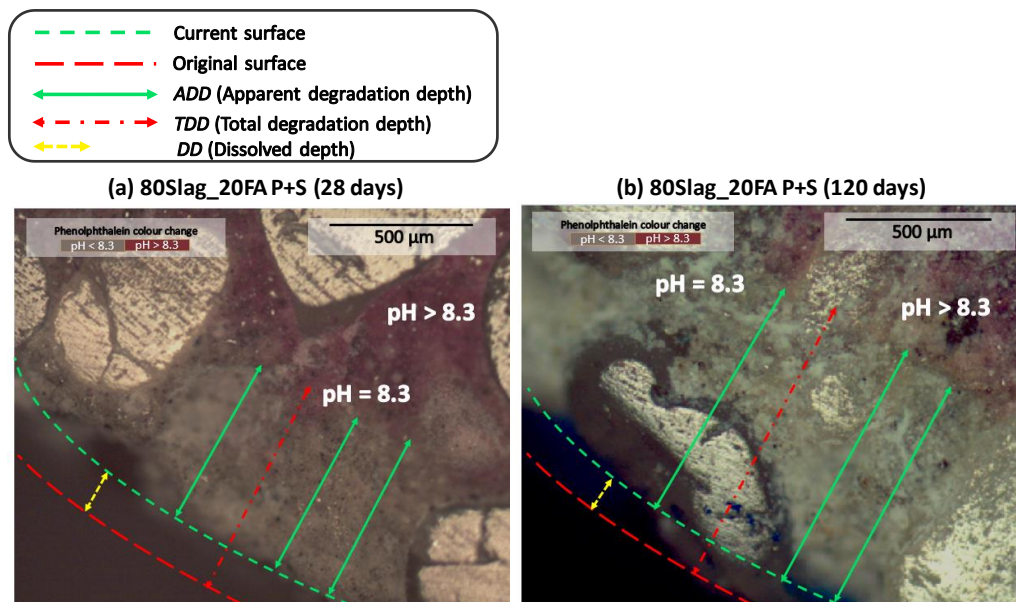
275 In terms of pore-related properties, the largest water absorption, VPV and capillary sorptivity are  
 276 reported for the 80Slag\_20FA mortar followed by the 60Slag\_40FA and 40Slag\_60FA samples. This

277 can be attributed to the different amount of water used for mixing the binders in which procedure a  
 278 higher water/binder ratio usually leads to more pores left after the evaporation of excessive water (Table  
 279 2). In terms of porous structures without considering the chemical compositions in different binder  
 280 matrix, it is reasonable to assume that 80Slag\_20FA would have the highest degradation kinetic  
 281 because the porous properties indicate that more acid solution **could** get easy ingress into the sample  
 282 matrix with the largest amount of pores and highest tendency to absorb water via capillary sorptivity [6].  
 283 In comparison, it seems that 40Slag\_60FA sample should obtain the highest resistance towards **acid**  
 284 **attacks** because it had the smallest porosity, VPV and lowest capillary sorptivity. **It is also noteworthy**  
 285 **that different alkalinities in different AASF mortar samples because of the different alkali-activator**  
 286 **dosages may also influence their performance in acidic environments [23]. However, degradation depth**  
 287 **is considered as the only direct method for degradation performance assessment and the influences of**  
 288 **all these factors can be reflected on degradation depths.**

289

### 290 3.2. Kinetics of degradation over immersion period

291 Fig. 3 provides an example of the increase in the degradation depth from 28-day to 120-day  
 292 immersion period for 80Slag\_20FA mortar exposed to the phosphoric and sulphuric mixed acid. The  
 293 degradation depth (mm) as a function of exposure time for all samples is then shown in Fig. 4.

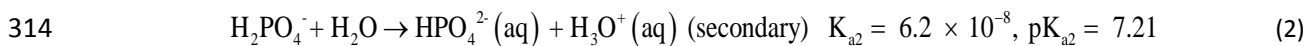
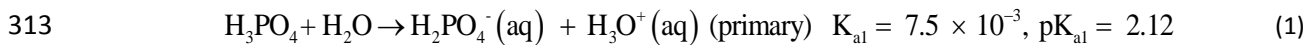


294

295 **Fig. 3. Optical-microscope measurement results of the sample (80%Slag\_20%FA) after being exposed to the**  
 296 **phosphoric + sulphuric (simplified as 'P+S' in the Fig. 3) mixed acid for different periods, polished and spayed**  
 297 **with phenolphthalein. (a) 28 day-immersion; (b) 120 day-immersion.**

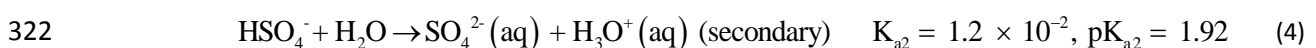
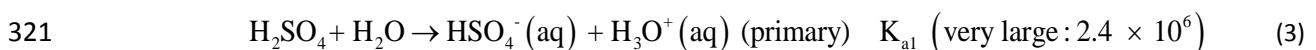
298 A time-dependent degradation depth evolution was obtained for all mixes of the mortar samples  
 299 regardless of different acid immersion conditions, as shown in Fig. 4(a)-(c). It is found that the TDD of  
 300 all samples after immersion in phosphoric acid for 150 days were greater than those either immersed  
 301 in the sulphuric acid or the phosphoric and sulphuric mixed acid in this study. In contrast, the samples  
 302 after the exposure to sulphuric acid had the least TDD. The degradation depth of the samples after  
 303 immersion in the phosphoric and sulphuric mixed acid exhibited an intermediate performance.  
 304 Therefore, there is no obvious extra effect, such as a synergistic manner proposed by Adam Neville  
 305 [70], for the phosphoric and sulphuric mixed acid compared to the single acid. The different  
 306 aggressiveness of the three types of acid solutions can be related to the concentration of hydronium  
 307 ions  $H_3O^+$  that the acid can release in an aqueous solution depending on acid types and concentrations  
 308 [71]. In this study, phosphoric and sulphuric acid are both bi-acid in aqueous acid solution ( $pH < 7$ )  
 309 which means that they both can release two hydronium ions in two successive dissociation reactions  
 310 which are shown below.

311 In the case of the phosphoric acid, at  $pH = 2.5$ , there is two acid functions left ( $pK_{a1} = 2.12 < pK_{a2} =$   
 312  $7.21 < pK_{a3} = 12.32$ ). The two involved dissociation reactions are as follows:



315 Therefore, it is apparent that at  $pH$  around 2.5 which is slightly higher than 2.12,  $H_2PO_4^-$ ,  $H_3PO_4$  and  
 316  $HPO_4^{2-}$  coexist in the phosphoric acid solution with the relative fraction of the first one much higher than  
 317 the other two ions.

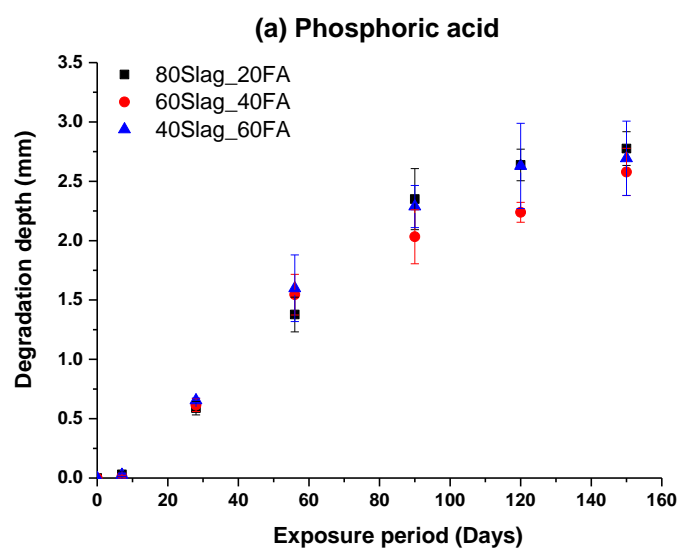
318 For sulphuric acid, there are also two functions left ( $pK_{a1}$  very small indicating a very strong acid  
 319 which completely dissociates in aqueous solutions,  $pK_{a2} = 1.92$ ) in which case  $SO_4^{2-}$  is the main species  
 320 in the sulphuric acid solution.



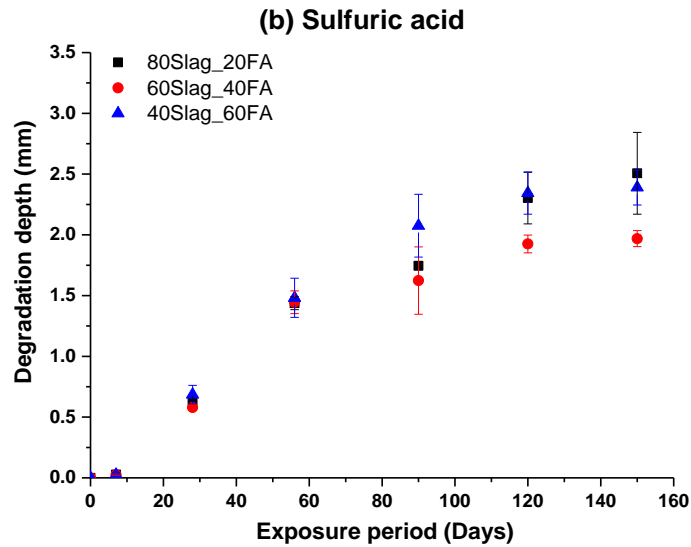
323 However, due to the partial dissociation of phosphoric acid compared to strong sulphuric acid which  
 324 dissociates completely in aqueous solution, the concentration of phosphoric acid molecule is higher  
 325 than that of sulphuric acid with an identical  $pH$  [72]. Hence, the amount of hydronium ions that can be

326 liberated in the phosphoric acid is higher than that of sulphuric acid. This higher concentration of  
327 available hydroniums in phosphoric acid solution is possibly responsible for the higher rate of  
328 degradation kinetic observed in this study. Similar results were seen in other studies [56, 73] which  
329 showed that at the same pH conditions, weak poorly and not-fully dissociated acids would be more  
330 aggressive than strong highly dissociated acids towards cementitious materials.

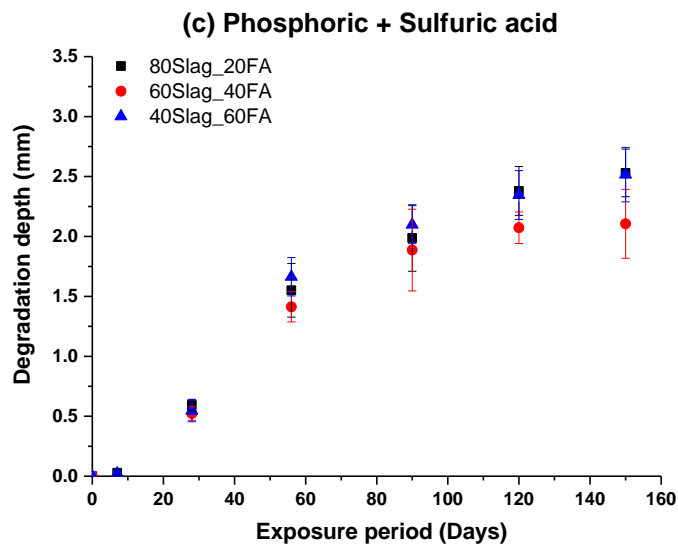
331 For all acid exposure conditions, 60Slag\_40FA seemed to have slightly smaller averaged  
332 degradation depths compared to the other formulations (though considering some standard deviations,  
333 it could be considered as equivalent to the others). Besides, similar degradation depths were obtained  
334 for 80Slag\_20FA and 40Slag\_60FA samples, especially in the case of the sulphuric acid and the two  
335 mixed acid condition. This result indicates that the effect of GGBFS/FA ratios on the relative degradation  
336 performance of AAMs is significant, corresponding well with other studies [17, 23]. In addition, it is also  
337 noticed that during the initial degradation process (within 7-day immersion period), there was almost no  
338 degradation depth measured followed by a significant increase in the degradation depth after 7 days  
339 until 56 days. After that, a continuous decreasing rate in the degradation depth development was  
340 observed until the end of exposure. This was also reported in another study which confirmed that after  
341 a certain period, the degradation rate decreased gradually which might be due to a diffusion-controlled  
342 process [21, 46, 51]. Therefore, the whole degradation process of AAMs can be separated into two  
343 parts: the first part is from the beginning to about 56-day of immersion (considered as the early stage)  
344 and the second stage starts from 56-day until the end of immersion (considered as the later stage).



345



346



347

348 **Fig. 4. The degradation depths of all mortar samples during 150-day exposure period in the three acid**  
 349 **environments, (a) phosphoric acid; (b) sulphuric acid and (c) the phosphoric and sulphuric mixed acid.**

350

351 **4. Numerical fitting and long-term predictions of degradation depth**

352 **4.1. Numerical fitting of experimental results**

353 It is possible to divide the degradation process for this study into two stages: an early stage (upto 56  
 354 days) and a later stage (from 56 days to 150 days).

355 Based on the experimental results within the early stage degradation process, Hill function, as a  
 356 numerical model was applied to fitting the experimental observations and simulating the early stage of  
 357 the degradation process. Hill function is used to quantify the degree of cooperative binding between

358 ligands and a macromolecule such as chondrocyte receptors [74]. It reflects a phenomenon that the  
359 response to a specific stimulus may exhibit a threshold behaviour indicating that the response would  
360 not take place until the stimuli reach a certain threshold. In this case, the diffusant hydronium ions  
361 ( $H_3O^+$ ) are regarded as a stimulus and the reaction products of AASF binders, e.g. C-A-S-H and/or N-  
362 A-S-H can be considered as macromolecules. The Hill function is expressed as the following formula:

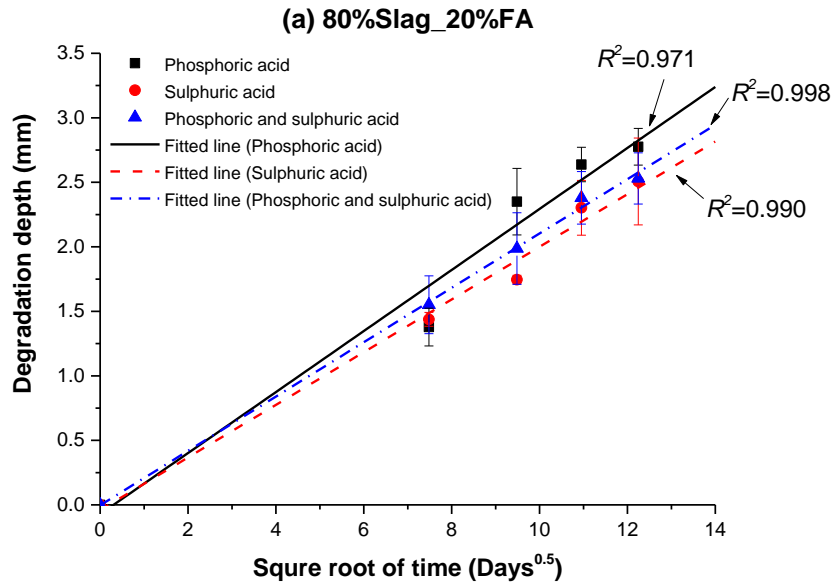
$$363 \quad TDD = \frac{A * t^n}{K^n + t^n} \quad (5)$$

364 where  $A$ ,  $K$  and  $n$  are characteristic values to be determined. ' $K$ ' indicates a certain amount of time  
365 during which no obvious degradation process propagates. ' $n$ ' refers to the rate of speed at which  
366 degradation reaction proceeds sharply reflected by a significant increase in degradation depths. ' $A$ '  
367 represents the potential capacity of further development of degradation depths. While ' $t$ ' represents the  
368 immersion period and  $TDD$  refers to the total degradation depth. Given the limited number of  
369 measurements, the characteristic values ' $K$ ' and ' $n$ ' were fitted using the same value for all samples in  
370 the three different acidic environments as the fitted values are very close except ' $A$ ' values. ' $A$ ' values  
371 varied significantly depending on different mixtures of the mortars and corresponding acid solutions.  
372 Fitted ' $A$ ' values obtained by using non-linear least-square fitting in MatLab are presented in table 6.

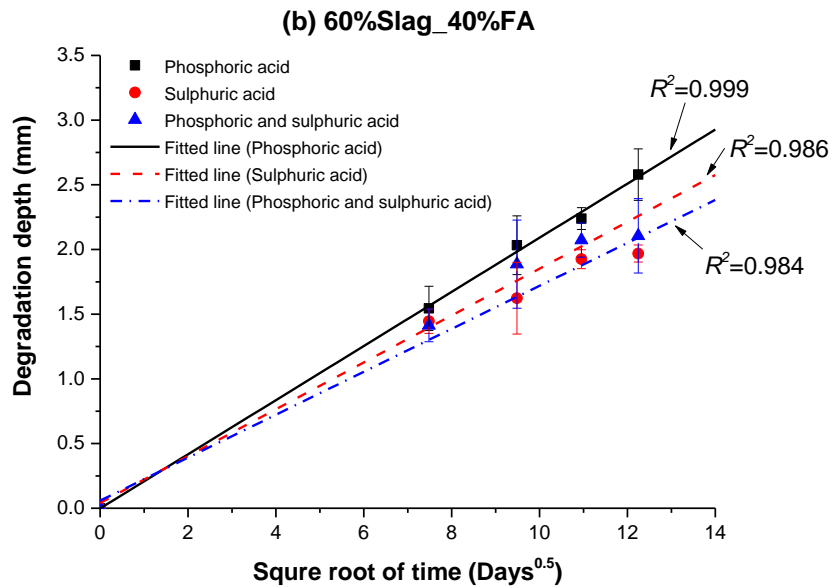
373 In terms of later stage (from 56 days of immersion), a linear fitting of the degradation depth (mm) as  
374 a function of square root of time ( $Days^{0.5}$ ) during immersion was first attempted. Fig. 5 (a)-(c) shows  
375 the best-fitted lines and the obtained  $R^2$  values are all greater than 0.95 as shown in Table 5, indicating  
376 a satisfactory fitting as a diffusion-controlled degradation process [75]. This diffusion-dominated  
377 degradation process is also in good agreement with the previous studies showing that the rate of  
378 deterioration of some cement-based concrete was proportional to the square root of time [76, 77]. Fick's  
379 second law has been widely used to describe the ion transportation caused by diffusion effect because  
380 of a concentration gradient between the surrounding aggressive environments and inner part of  
381 samples, such as sulphate and chloride migration from outside solutions into concretes [78-81]. During  
382 this process, the degradation rate was mainly controlled by the diffusion of ions, such as hydroniums in  
383 this case. In the current study, the 56-day of immersion was considered as the starting point of the  
384 diffusion-controlled later stage. Hence, only the experimental values from the 56-day immersion were  
385 used for further numerical fitting using Fick's second law.

386 Table 5. The fitted coefficient of determination  $R^2$  for the later stage of all mortar samples in the three  
 387 acid solution environments.

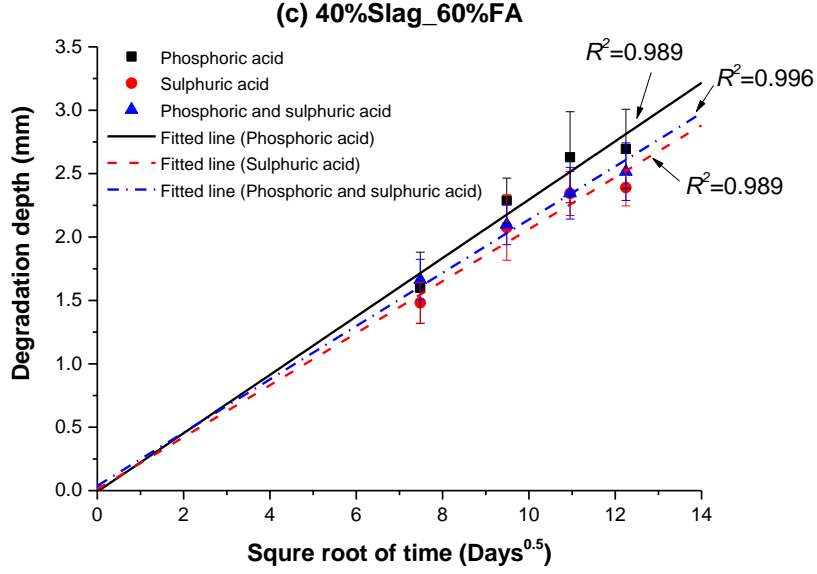
Sample ID	Acid solution types		
	Phosphoric acid	Sulphuric acid	Phosphoric + sulphuric acid
80Slag_20FA	0.971	0.990	0.998
60Slag_40FA	0.999	0.984	0.986
40Slag_60FA	0.989	0.989	0.996



388



389



390  
 391 **Fig. 5. Degradation depth (mm) evolution as a function of the square root of time (Days<sup>0.5</sup>) for each samples;**  
 392 **(a) 80Slag\_20FA; (b) 60Slag\_40FA; (c) 40Slag\_60FA. 'R<sup>2</sup>' values represent coefficients of determination. Solid**  
 393 **points are the experimental results with error bars indicating one standard deviation either side of the mean**  
 394 **value and lines are linearly fitted to showcase the relationship between the degradation depth and square**  
 395 **root of exposure time.**

396 According to the Fick's second law, the differential equation for one-dimensional diffusion is as  
 397 follows:

$$398 \quad \frac{\partial C(x,t)}{\partial t} = D \cdot \frac{\partial^2 C(x,t)}{\partial x^2} \quad (6)$$

399 where  $C(x,t)$  is the concentration of a specific ion ( $H_3O^+$  in our case) expressed as mol/L, and  $D$  is  
 400 the diffusion coefficient ( $m^2/s$ ) of the corresponding ion. If the concentration of hydroniums (reflected  
 401 by the pH value) is assumed to be constant at the surface of the sample, a solution to Fick's second  
 402 law is as follows:

$$403 \quad C(x,t) = C_i + (C_s - C_i) \left[ 1 - \operatorname{erf} \left( \frac{x}{2\sqrt{Dt}} \right) \right] \quad (7)$$

404 where  $C_i$  is the initial (or background) concentration of  $H_3O^+$  (mol/L) in the pore solutions of the samples,  
 405  $C_s$  is the boundary concentration of  $H_3O^+$  (mol/L) at the external surface of the samples. The initial  
 406 concentration value of  $H_3O^+$  ( $C_i$ ) in pore solutions of AAMs is in a range between  $10^{-12}$  and  $10^{-13}$  (i.e. a  
 407 pH ranging from 12 to 13) [22] which is many orders of magnitude less than that of  $C_s$  (i.e.  $10^{-2.5}$  leading

408 to a pH of 2.5). Thus, it is reasonable to assume  $C_i = 0$  in this study. Then, the time-dependent ion  
 409 concentration in samples was obtained as:

$$410 \quad C(x,t) / C_s = \left[ 1 - \operatorname{erf} \left( \frac{x}{2\sqrt{Dt}} \right) \right] \quad (8)$$

411 where 'erf' is the error function (a special function related to the integral of a normal probability function).  
 412 As shown in Fig. 2b, the total degradation depth (**TDD**) is the distance between the sample original  
 413 external boundary and the surface where pH=8.3 (i.e. the colour of phenolphthalein changes from pink  
 414 or magenta to no colour). Letting  $C(x, t) = 10^{-8.3}$ ,  $C_s = 10^{-2.5}$ , the **TDD** can be expressed as,

$$415 \quad \text{TDD} \approx 6.79\sqrt{D} \cdot \sqrt{t} \quad (9)$$

416 Based on the different  $\text{H}_3\text{O}^+$  concentrations at the sample surface, a series of **TDD** can be obtained  
 417 which are shown below in Eq. (6)-(8). It is worth noting that the apparent diffusion coefficient here is not  
 418 the real diffusion coefficient of a species (e.g.  $\text{H}_3\text{O}^+$ ) in water. Instead, it is a parameter which covers  
 419 many factors such as acid types, tortuosity and porosity of the binders. It is assumed to be constant for  
 420 a certain mixture of alkali-activated mortar sample in a specific acid solution regardless of different pH  
 421 values. The various pH values are assumed to only influence the boundary conditions in the Fick's  
 422 second law in this study. Changed boundary conditions because of different pH are shown below:

423 If pH = 1,

$$424 \quad \text{TDD} \approx 7.71\sqrt{D} \cdot \sqrt{t} \quad (10)$$

425 If pH = 2,

$$426 \quad \text{TDD} \approx 7.11\sqrt{D} \cdot \sqrt{t} \quad (11)$$

427 If pH = 3,

$$428 \quad \text{TDD} \approx 6.45\sqrt{D} \cdot \sqrt{t} \quad (12)$$

429 The apparent diffusion coefficients ( $D$ ) of all samples immersed in three different acidic solutions  
 430 were obtained by substituting the experimental results into Eq. (9) and using nonlinear least-square  
 431 best-fit analysis in MATLAB. Diffusion coefficient  $D$  has a unit of length/square root of time ( $\text{mm/s}^{1/2}$ ).  
 432 The degradation depth is measured in  $\text{mm}$  and the immersion period has a unit of second ( $\text{s}$ ). The final  
 433 obtained diffusion coefficients for all samples in the three acidic solutions are also shown in Table 6.

434 The successful fitting using the simplified model again confirmed that the degradation depth during later  
 435 stage process is diffusion-controlled.

436 Table 6. Numerically fitted apparent diffusion coefficients ' $D$ ' ( $1 \times 10^{-8}$  mm<sup>2</sup>/s) and ' $A$ ' values (mm) in the  
 437 Hill function of all samples immersed in the three acid solutions. ' $K$ ' and ' $n$ ' values are '36' and '5'  
 438 respectively for all samples regardless of different acid solutions and therefore are not listed.

Sample ID	Acid solution types					
	Phosphoric acid		Sulphuric acid		Phosphoric + sulphuric acid	
Parameters	$D$	$A$	$D$	$A$	$D$	$A$
80Slag_20FA	1.32	1.90	1.00	1.65	1.08	1.74
60Slag_40FA	1.04	1.70	0.74	1.42	0.86	1.54
40Slag_60FA	1.32	1.92	1.07	1.72	1.15	1.78

439

440 At the beginning of early stage, the degradation process seemed to be delayed, presented as an  
 441 induction phase. According to the fitting results, all mortar samples regardless of GGBFS/fly ratios and  
 442 different types of acid solutions had the same duration, expressed as ' $K$ ' = 36 in the Hill function. This  
 443 indicates that the duration of induction stage is not mainly determined by chemical compositions of  
 444 AAMs (such as GGBFS/FA ratios and different alkalinities) and acid types. According to Lloyd et al.  
 445 [46], the early stage of degradation was a chemical-controlled process, which was highly dependent on  
 446 pH levels of acid solutions. Thus, it is reasonable to assume that the duration of early stage in this study  
 447 should be similar because all pH values of the acid solutions were kept the same. On the other hand,  
 448 however, the fitted ' $A$ ' values in Hill functions are different for the three mixtures of mortars in the three  
 449 acidic media. This indicates that the possible degradation depth at the point of transition from the early  
 450 stage to later stage differs. In this study, 40Slag\_60FA had the greatest ' $A$ ' value indicating the greatest  
 451 degradation depth at the end of early stage regardless of the acid exposure conditions. However, the  
 452 lowest capillary sorptivity, water absorption and VPV of 40Slag\_60FA imply that it should have the  
 453 smallest degradation depth without considering the difference in the chemical compositions of all  
 454 mixture binders. This result is in agreement with another study which revealed that the chemical  
 455 compositions and components of materials are more predominant than microstructures (i.e. capillary  
 456 sorptivity or water absorption) for acid resistance [6]. This also points out that less Ca does not  
 457 necessarily lead to higher resistance with the experimental condition used in this study. More chemical  
 458 analysis is required in order to explain the results in the future study. Moreover, the sample with greater  
 459 ' $A$ ' values also exhibits larger diffusion coefficients  $D$ , suggesting consistent results for the entire  
 460 degradation process (as shown in Table 6).

461 Based on the meaning of Hill function, the hindered degradation process at early stage might be  
462 attributed to the fact that  $\text{H}_3\text{O}^+$  are firstly consumed by hydroxyls following the neutralisation reaction:  
463  $\text{H}_3\text{O}^+ + \text{OH}^- \rightarrow 2\text{H}_2\text{O}$ . It was already reported that the pH of AASF pore solution is in a range of 13.77-  
464 14.76 (depending on alkali-activators used, GGBFS/FA ratios, etc.) which is even higher than that of  
465 the pore solution for OPC-based binders ( $\text{pH} > 12$ ) [82]. Therefore, in the initial degradation stage, there  
466 are many hydroxyls available in the pore solution to consume  $\text{H}_3\text{O}^+$  and maintain a high pH level. Thus  
467 no obvious degradation depths could be measured at this stage [83, 84]. This mechanism is to some  
468 extent analogous to the 'sacrificial medium' effect provided by the high amount of Portlandite ( $\text{Ca}(\text{OH})_2$ )  
469 in OPC-based binders. Portlandite plays an important role in 'consuming' most hydroniums with  
470 hydroxyls via neutralisation effect when samples were submerged in aggressive acid solutions [9, 85].  
471 In that case, the overall pH level of the pore solutions in OPC-based concrete can remain stable for a  
472 certain time.

473 Furthermore, another possible reason for the absence of degradation depths is that at the very  
474 beginning of the acidic attacks, the reaction products precipitated on the surface of the samples and  
475 clogged the surface pores. Therefore, the ingress of acid solutions is impeded. At pH between 2.0 and  
476 3.0, the main anion from the phosphoric acid and sulphuric acid solution is supposed to be  $\text{H}_2\text{PO}_4^-$  and  
477  $\text{SO}_4^{2-}$  respectively. Therefore, the main reaction products due to decalcification process in AAMs is  
478 probably monocalcium phosphate  $\text{Ca}(\text{H}_2\text{PO}_4)_2$  or  $\text{Ca}(\text{H}_2\text{PO}_4)_2 \cdot \text{H}_2\text{O}$  for phosphoric acid solution and  
479 gypsum ( $\text{CaSO}_4 \cdot 2\text{H}_2\text{O}$ ) for sulphuric acid solution with possible chemical reactions:

- 480 • Phosphoric acid:  $\text{Ca}^{2+} + \text{H}_2\text{PO}_4^- \rightarrow \text{Ca}(\text{H}_2\text{PO}_4)_2$  (calcium dihydrogen phosphate);  
481  $\text{Ca}^{2+} + \text{H}_2\text{PO}_4^- + \text{H}_2\text{O} \rightarrow \text{Ca}(\text{H}_2\text{PO}_4)_2 \cdot \text{H}_2\text{O}$  (calcium dihydrogen phosphate monohydrate)  
482 • Sulphuric acid:  $\text{Ca}^{2+} + \text{SO}_4^{2-} + 2\text{H}_2\text{O} \rightarrow \text{CaSO}_4 \cdot 2\text{H}_2\text{O}$  (gypsum)

483  $\text{Ca}(\text{H}_2\text{PO}_4)_2$  and  $\text{Ca}(\text{H}_2\text{PO}_4)_2 \cdot \text{H}_2\text{O}$  both have a solubility of 2.0 g and the water solubility of  
484  $\text{CaSO}_4 \cdot 2\text{H}_2\text{O}$  is 0.255 g in 100 ml water (20 °C). This means that some reaction products are assumed  
485 to precipitate on the surface of samples, even clogging surface pores. It can be more obvious when the  
486 acid solutions are calcium-saturated before each renewal. This is evidenced by some white compounds  
487 detectable on the surface of the samples after 56-day immersion period when the sample was naturally  
488 dried under the ambient environment (Fig. 6). This is in consistent with the case reported by J. Shen et  
489 al. [86] that in some extreme conditions, the surface pores could be clogged because of the formations  
490 of some reaction products. Hence, during the reaction-controlled early stage, it is probably the clogging

491 effect caused by the reaction products that led to a delayed degradation evolution in the early stage.  
492 This result is also consistent with the finding in the study that sulphuric acid-induced attack mainly  
493 occurs at the sample surfaces if there is no flow of fluid with the formation of gypsums (molar volume:  
494  $73.84 \text{ cm}^3/\text{mol}$ ) on the sample surface when the surrounding pH is at 2.0 [58]. A study also has reported  
495 a reaction-controlled degradation process in the early stage of exposition for AAMs [46]. However, as  
496 specific reaction mechanisms are not fully explained, especially for AAMs in phosphoric acid solutions,  
497 more research is therefore necessary. The accumulation of the precipitated reaction products on the  
498 surface might be another factor that results in the transition from early stage to later stage as  
499 hydroniums had to diffuse through this product layer first before entering the sample matrix.



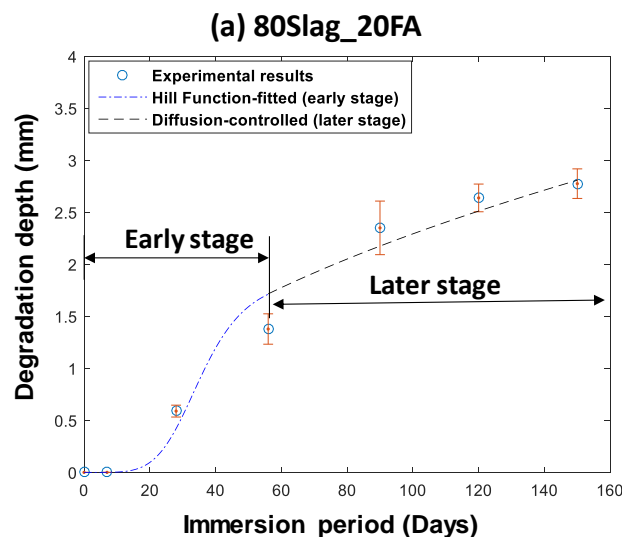
500

501 **Fig. 6. The white reaction products precipitated on the sample surface clogging the surface pores after 56-day**  
502 **immersion period (The picture was taken after the sample was taken out from the acid solution and dried**  
503 **under ambient condition for upto 3 hours).**

504 In terms of later stage fitted by using Fick's second law with the diffusion coefficients shown in Table  
505 6, it is evident that the 60%Slag\_40%FA sample had the lowest diffusion coefficient ( $1.04 \times 10^{-8} \text{ mm}^2/\text{s}$ )  
506 in phosphoric acid solution. On the other hand, the 40%Slag\_60%FA and 80%Slag\_20%FA sample  
507 had a similar highest diffusion coefficient at around  $1.32 \times 10^{-8} \text{ mm}^2/\text{s}$ . In the sulphuric and the  
508 phosphoric and sulphuric mixed acid, 60%Slag\_40%FA sample also had the least diffusion coefficient,  
509  $0.74 \times 10^{-8} \text{ mm}^2/\text{s}$  and  $0.86 \times 10^{-8} \text{ mm}^2/\text{s}$  respectively. While the sample 40%Slag\_60%FA had the  
510 greatest diffusion coefficient, respectively  $1.07 \times 10^{-8} \text{ mm}^2/\text{s}$  and  $1.15 \times 10^{-8} \text{ mm}^2/\text{s}$  in the sulphuric and  
511 the phosphoric and sulphuric mixed acid. Apparently, the 60%Slag\_40%FA sample performed the best  
512 with the lowest diffusion coefficient compared to the other sample mixtures in all acid solutions. The

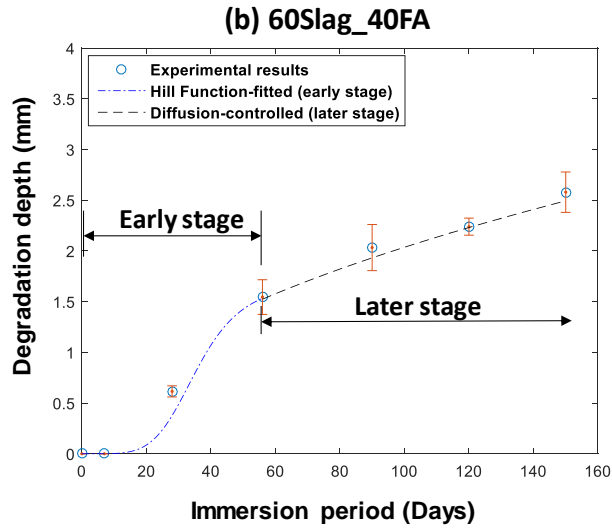
513 40%Slag\_60%FA sample, which exhibited the greatest degradation depth, had the largest diffusion  
514 coefficient accordingly among the tested samples in all solutions. The diffusion-controlled later stage  
515 can be due to the mechanically stable degraded layer which is less soluble. It is known as a residue gel  
516 rich in Si and Al which can act as a protection layer, hence limiting further ingress of hydroniums [87].  
517 Besides, it can also be partially ascribed to the precipitations of reaction products such as calcium salts  
518 which is already discussed in the early stage part.

519 Fig. 7-9 show the overall degradation process including the two stages to compare the degradation  
520 process for various mixtures of samples in different acid solutions. To conclude, the observed  
521 degradation process in this study can be separated into two major stages including the early stage and  
522 later stage. In the early stage, the empirical Hill function was applied to fitting the experimental data  
523 which showed that at the very beginning of the degradation, there was almost no degradation depths  
524 for at least several days. Then there was an obvious degradation depth (approximately 0.5 mm) after  
525 28-day exposure to acid solutions which indicates a significant increase in degradation rate. The highest  
526 increasing rate of the degradation depth occurred at around 36 days of immersion, corresponding to  
527 the parameter ' $K$ ' = 36 in Hill function for all samples in the three different acid media. This value can  
528 be regarded as a turning point after which the degradation process gradually converted into the later  
529 stage. In the later stage, the degradation process was diffusion-controlled showing a linear increment  
530 in degradation depths as a function of square root of immersion period (Fig. 5). The growth in  
531 degradation depths in this stage was apparently limited, likely due to the existence of mechanically  
532 sound degraded layer and formation of newly-formed reaction products in the degraded layer which  
533 hindered further penetrations of hydronium ions [46].

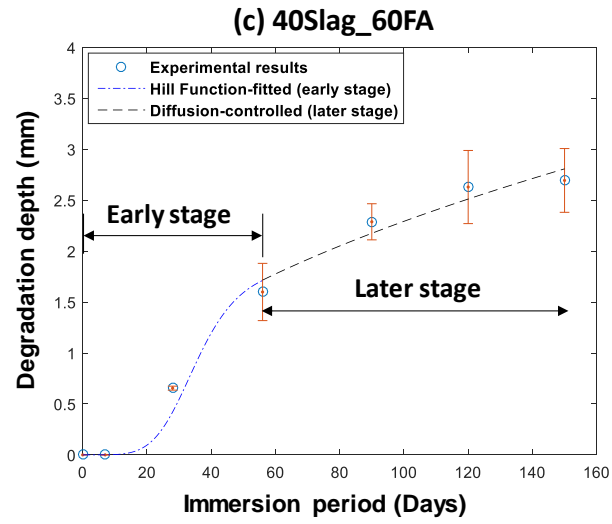


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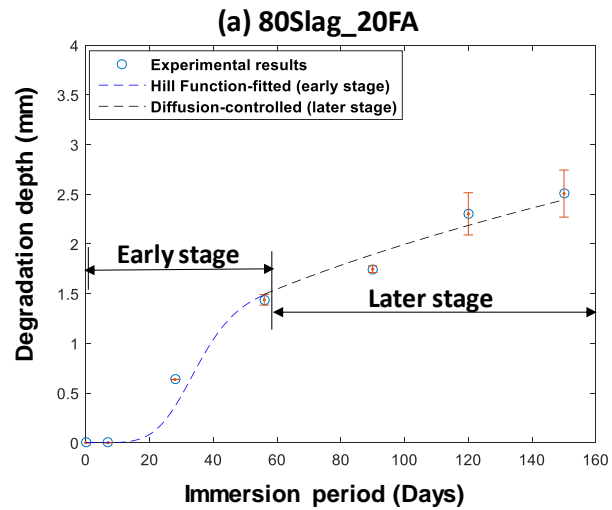


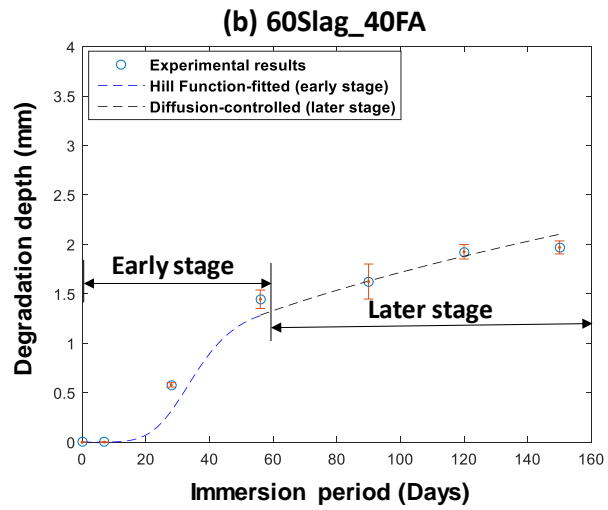
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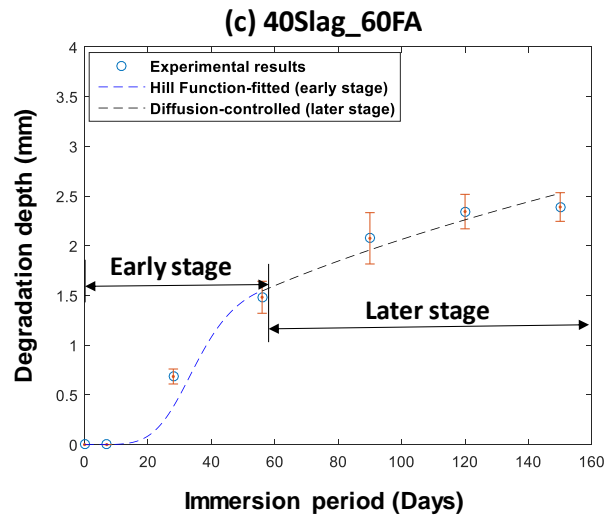
537 **Fig. 7. Time-dependent degradation depths of different samples in the phosphoric acid during the immersion**  
538 **period. (a) 80Slag\_20FA; (b) 60Slag\_40FA; (c) 40Slag\_60FA.**

539



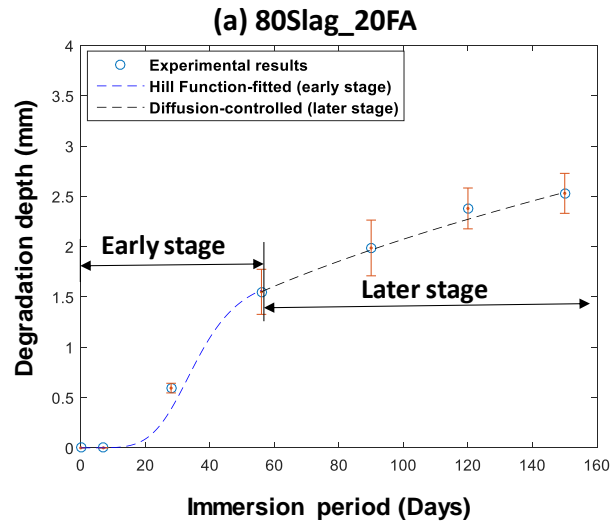


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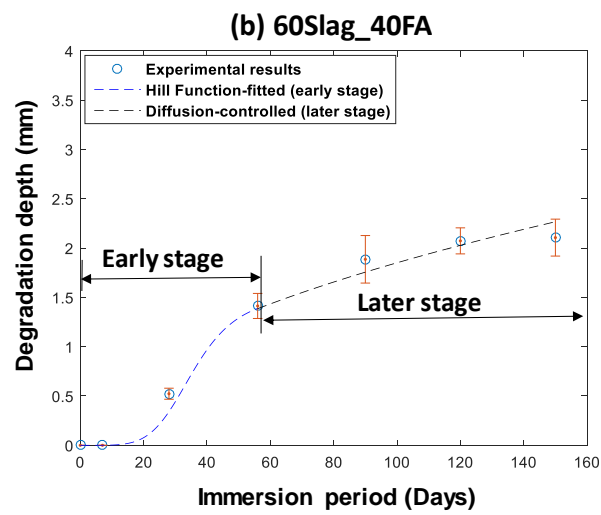


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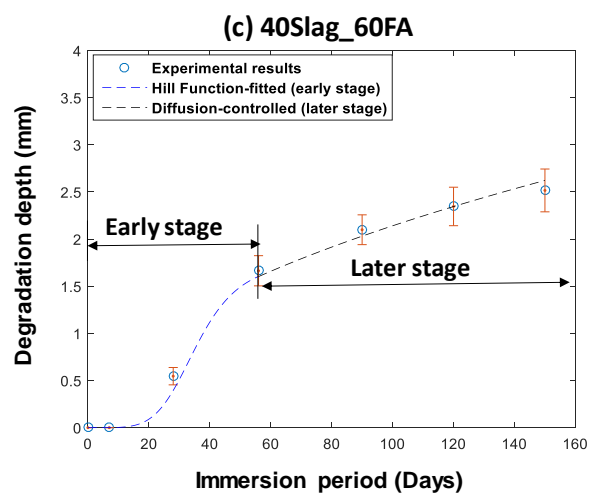
542 Fig. 8. Time-dependent degradation depths of different samples in the sulphuric acid during the immersion  
 543 period. (a) 80Slag\_20FA; (b) 60Slag\_40FA; (c) 40Slag\_60FA.



544



545



546

547 Fig. 9. Time-dependent degradation depths of different samples in the phosphoric and sulphuric mixed acid  
 548 during the immersion periods. (a) 80Slag\_20FA; (b) 60Slag\_40FA; (c) 40Slag\_60FA.

549 When comparing the different samples, the peculiarities of the microstructures and compositions of  
550 the AASF mortars in the study can be responsible for their different acid resistance capabilities [88, 89].  
551 In the study, the 80%Slag\_20%FA sample had the highest initial VPV and water absorption as well as  
552 water sorptivity (Table 4). The sorptivity can reveal the transport mechanisms of acid solutions in the  
553 mortar samples [6]. Combined with higher VPV and water absorption, greater sorptivity suggests a  
554 porous structure with a high connectivity and many finer interconnected voids. All of these lead to a  
555 much easier ingress of acid solutions and aggressive ions into the matrix binders compared to other  
556 mixtures of mortars. Thus, within a certain period, far more hydronium ions with water flowed into the  
557 samples which explained why the 80%Slag\_20%FA had a relatively larger degradation depth. On the  
558 other hand, the 40%Slag\_60%FA sample had a denser porous structure with lower VPV, water  
559 absorption and water sorptivity. According to N.K. Lee et al. [89], an increase in fly ash content leads  
560 to more sodium aluminosilicate hydrate (N-A-S-H) gel and less C-A-S-H, and the former one is less  
561 dense compared to the latter. Therefore, the sample with a higher amount of fly ash replacing slag  
562 contains more N-A-S-H, developing a more porous matrix which reduced the resistance towards ion  
563 transport [44]. Therefore,  $H_3O^+$  attacked the bulk matrix of the samples easier which was responsible  
564 for the greater degradation depth compared to the other mixtures of the samples. The 60%Slag\_40%FA  
565 sample seemed to overcome the disadvantages of the other two peers and made a great compromise  
566 between the pore networks and the geopolymerisation products. It has a certain amount of calcium  
567 which results in the formation of a denser C-A-S-H type gel along with a relatively compact porous  
568 microstructure.

569

#### 570 **4.2. Predictions of long-term performance between AAMs and OPC based mortars**

571 Yuan et al. [51] carried out an experiment and conducted long-term simulation based on Kawai's [58]  
572 90-day experiments where OPC-based mortars (w/b: 0.35 and initial compressive strength cured after  
573 28 days was 47.2 MPa) were subjected to sulphuric acid attack with a pH at 2.0 for 24 months. Then a  
574 generally believed relationship between the degradation depth and exposure time was used to model  
575 the degradation process (Method 1 as discussed in the Kawai's study [58]) [21]. The relationship is  
576 almost the same as the simplified model for later-stage degradation which also highlights a linear  
577 increase in degradation depth of concrete due to acid attacks including sulphuric acid against the square  
578 root of time as follows:

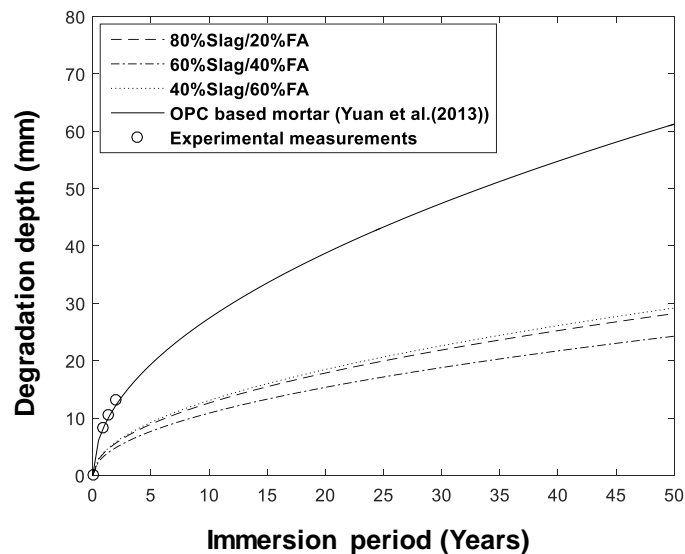
579 
$$TDD = b \cdot \sqrt{t} \quad (13)$$

580 where, **TDD** is the total degradation depth (mm) as described before,  $t$  represents the exposure time  
581 (month) in acidic solution and  $b$  is a constant. This equation indicates that the degradation kinetic is  
582 controlled by the diffusion rate of acid under the assumption that degradation products remain on the  
583 surface [51]. Since the samples in this study were also statically subjected to acidic attacks without  
584 shearing forces from splashing or running water, the particles were also assumed to precipitate and  
585 remain on the surface. Based on Eq. (13), Yuan et al.[51] calculated the value of constant  $b$  which is  
586 2.5 mm/month<sup>1/2</sup> and the degradation depth of this OPC-based mortar was then predicted. After 50-year  
587 immersion, **it is estimated that** the degradation depth can be as much as 61.24 mm.

588 As the alkali-activated mortar samples in this study were also immersed in sulphuric acid with a  
589 similar pH condition (pH = 2.5 ± 0.5), the corresponding derived diffusion coefficients for each sample  
590 mixture are assumed to be constant. The only difference is the boundary condition which changes into  
591 Eq. (11). Then Eq. (11) and derived diffusion coefficients for sulphuric acid immersion were used to  
592 predict the degradation depths after 50-year immersion period. The predicted numerical results are  
593 compared to that of OPC-based mortars mentioned before, as shown in Fig. 10. **After** 50-year exposure,  
594 the increasing order of degradation depths are 60%Slag\_40%FA, 80%Slag\_20%FA and  
595 40%Slag\_60%FA with the degradation depth at 24.29, 28.23 and 29.20 mm respectively. Apparently,  
596 the degradation depths of all alkali-activated mortars are much less than that of the OPC-based mortar  
597 sample. As a result, the degradation depth can be decreased by around 60.3%, 53.9% and 52.3% if  
598 the OPC-based tested samples are replaced by 60%Slag\_40%FA, 80%Slag\_20%FA and  
599 40%Slag\_60%FA respectively in this study.

600 **It is worth noting that the 56-day compressive strength of the AASF mortar samples in this study was**  
601 **higher than the 47.2 MPa compressive strength after 28 days of curing in Kawai's study [58].**  
602 **Considering the continuous cement hydration, the 56-day compressive strength for this OPC mortar**  
603 **should be higher and it is speculated to be around 55.6 MPa according to a formula proposed by Liu et**  
604 **al. [90]. Therefore a reasonable comparison was carried out above. However, it still has to be admitted**  
605 **that the compressive strength difference between the AASF mortars (ranging between 57.7 and 61.4**  
606 **MPa) in this study and the OPC-based counterpart in Kawai's study [58] (55.6 MPa as speculated) is**  
607 **possibly another reason for the less degradation depth of the former ones as compared to the latter**  
608 **since a higher compressive strength usually indicates a denser microstructure. Therefore, further**

609 research with regards to a systematic comparison between the AASF and OPC-based mortars should  
610 be conducted.



611 Fig. 10. The comparison between the numerical predictions based on the present study and the experimental  
612 results as well as corresponding simulation equations derived from Yuan et al. (2013).

### 613 Limitations

614 It should be mentioned that this study mainly focused on the degradation of mortar specimens instead of  
615 concrete which is a composite material composed of fine and coarse aggregates bonded together with cement.  
616 In addition, our theoretical analysis ignored the possible changes in diffusion coefficient of ions due to the  
617 damages of mortar microstructures with degradation progression. Our future will focus on the degradation of  
618 concrete under acid conditions which might provide more representative results and the chemical processes  
619 involved in the early stage of degradation will also be explored.

### 620 5. Conclusions

621 The present study investigated experimentally the degradation depth evolution of AASF mortars  
622 under three aggressive acid solutions. The following conclusions can be summarised:

- 623 • Among all the three types of acids with similar pH values: phosphoric acid, sulphuric acid and  
624 the mixture of phosphoric acid and sulphuric acid, phosphoric acid caused the most severe  
625 degradation to AASF mortars due to its largest amount of available hydroniums;
- 626 • The AASF mortar with a slag/fly ash ratio at 60:40 displayed the best durability performance  
627 after immersion in the three types of acids for 150 days probably due to its higher amount of C-

628 A-S-H (compared to 40%Slag\_60%FA) and a relatively more densified structure (compared to  
629 80%Slag\_20%FA);

- 630 • The degradation of AASF mortars can be divided into two stages: (1) Early stage - a chemical  
631 dominated process which can be described by using Hill function; and (2) Later stage - a  
632 diffusion dominated process which is described by using Fick's second law.
- 633 • Theoretical prediction shows that the reduction in the degradation depth of AASF mortars after  
634 50 years' immersion in sulphuric acid (pH=2.0) could be in a range between 52% - 60%  
635 compared to that of the OPC-based mortar.

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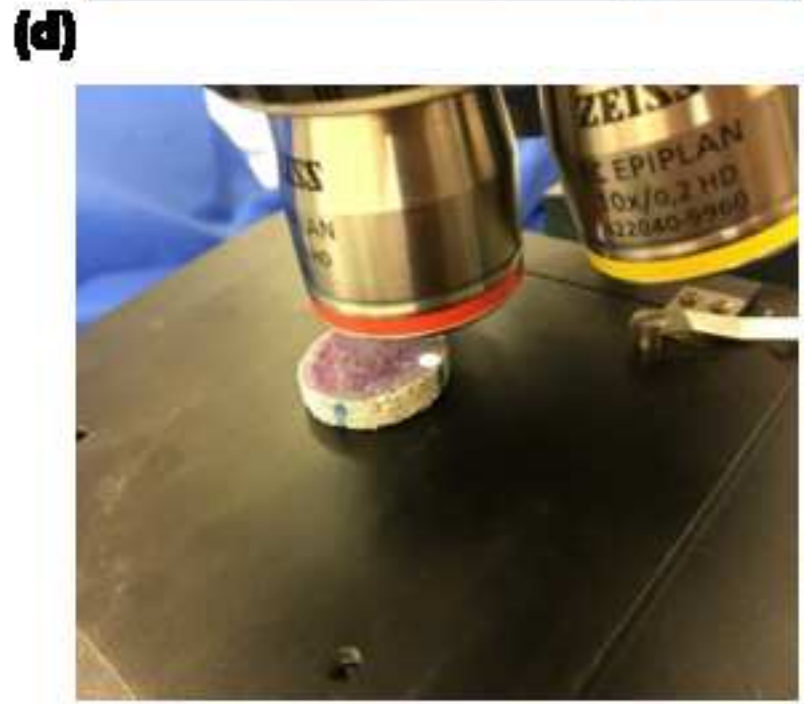
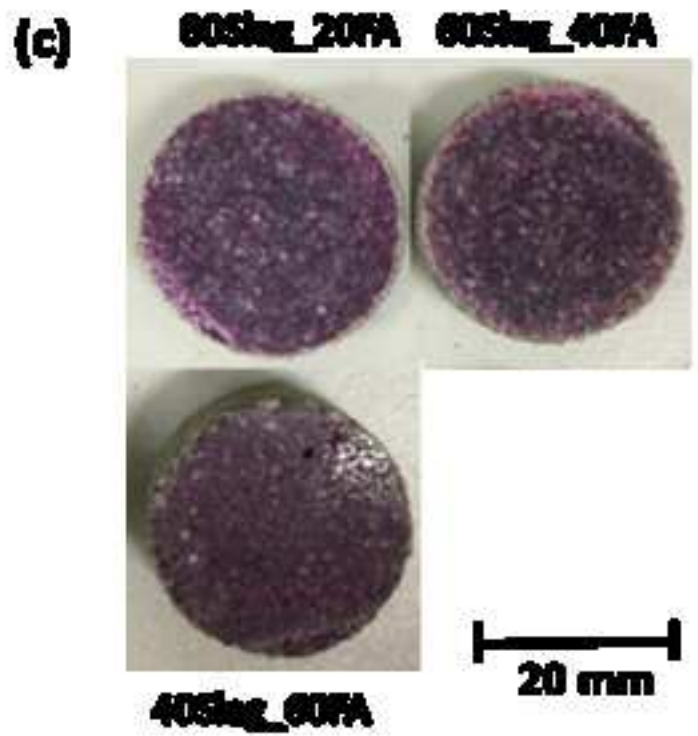
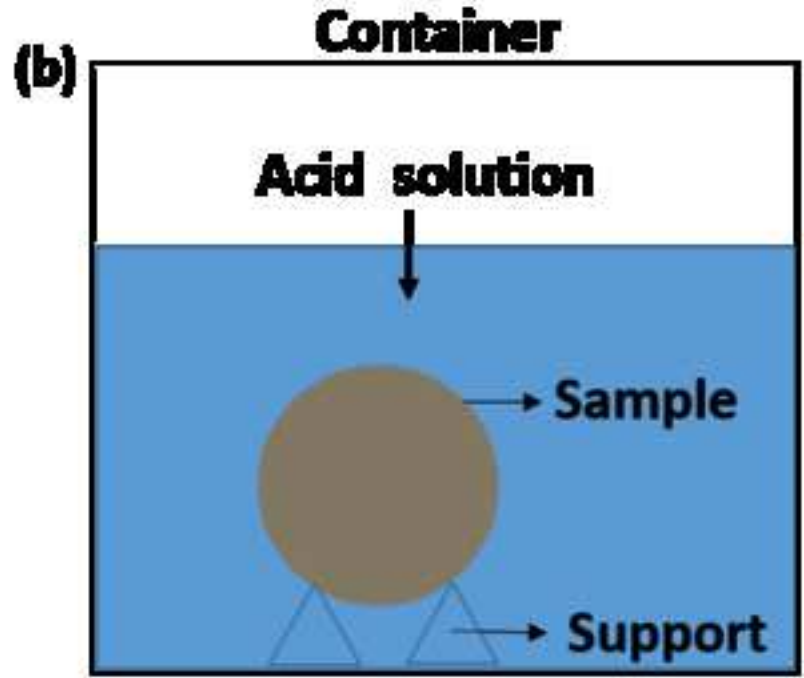
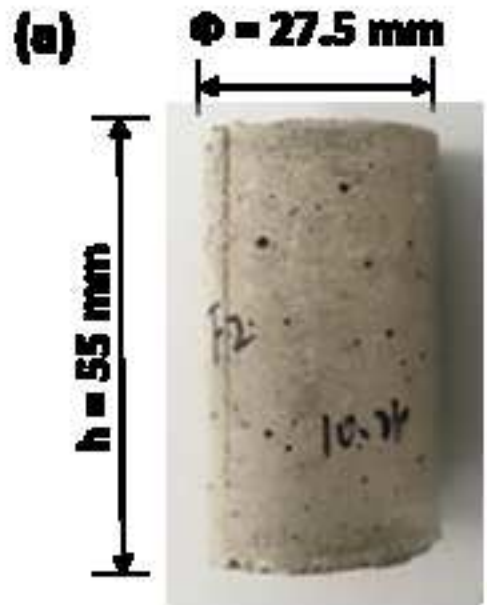
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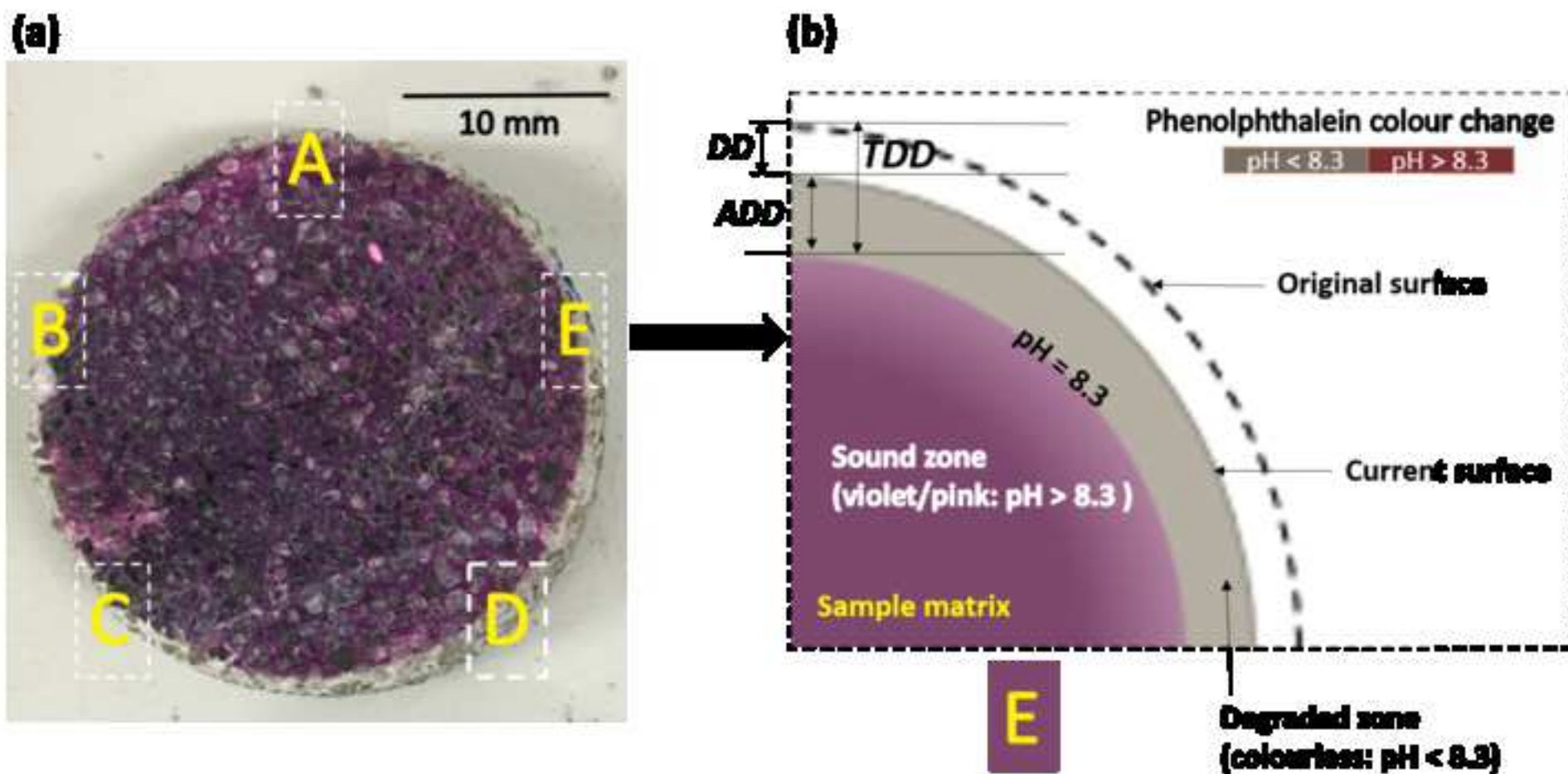
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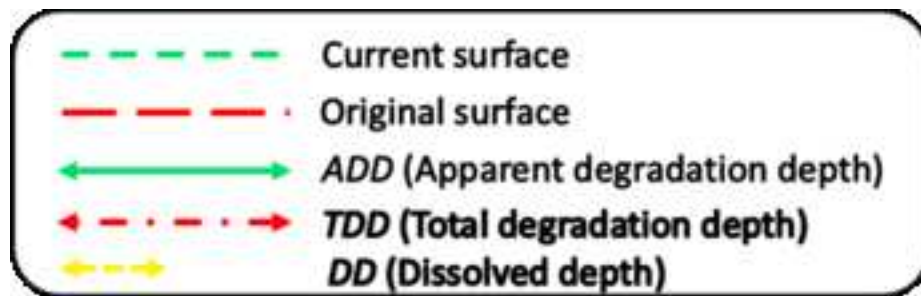
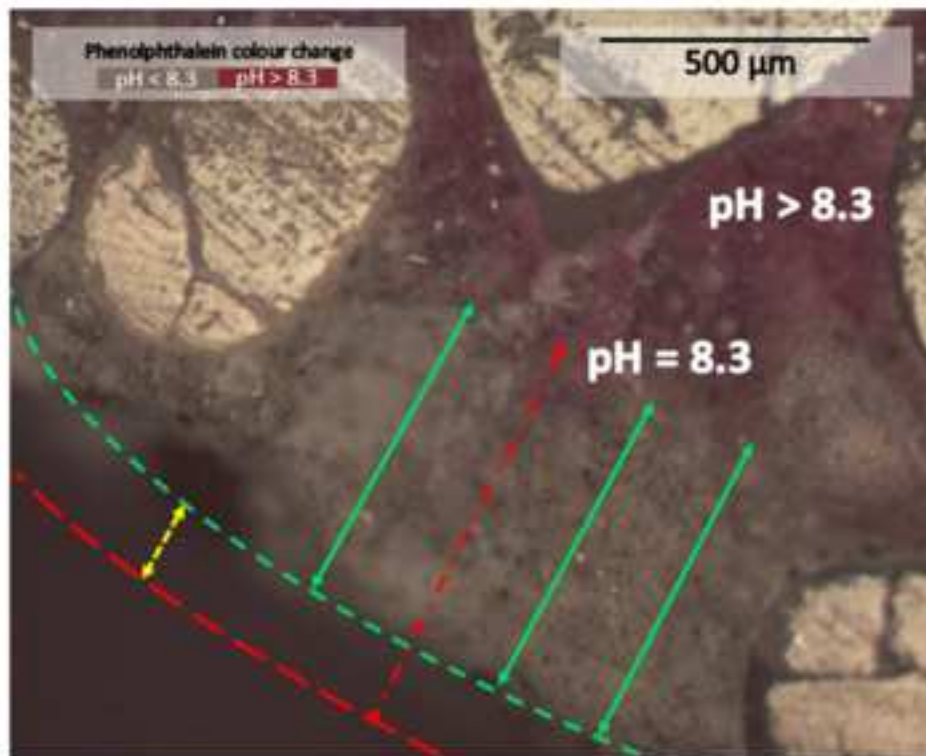
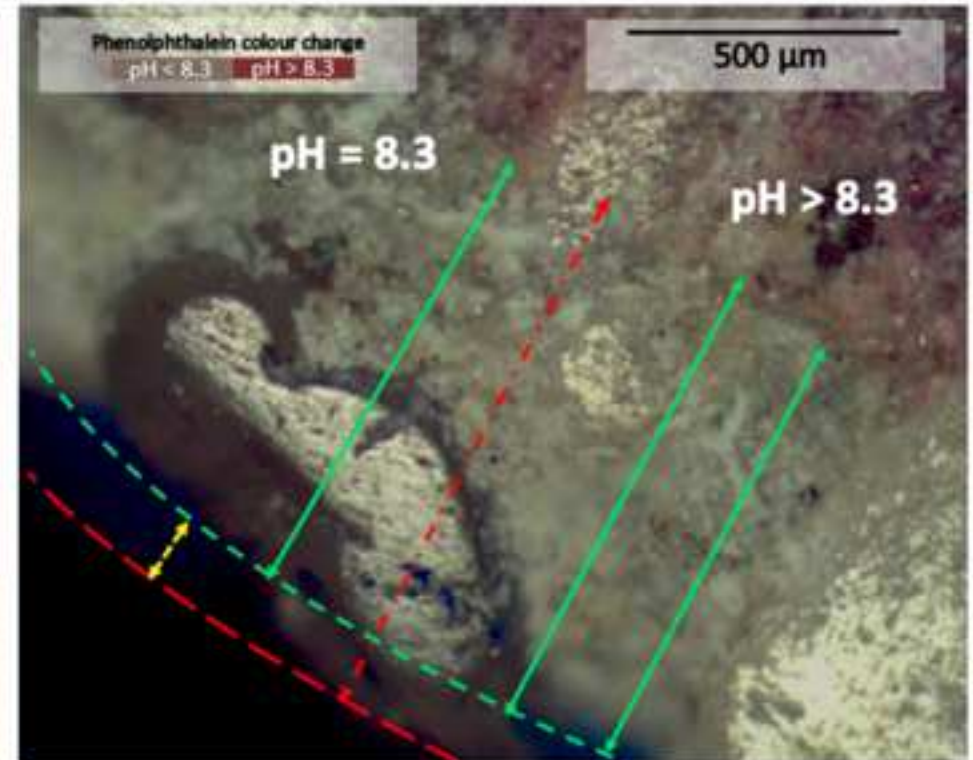
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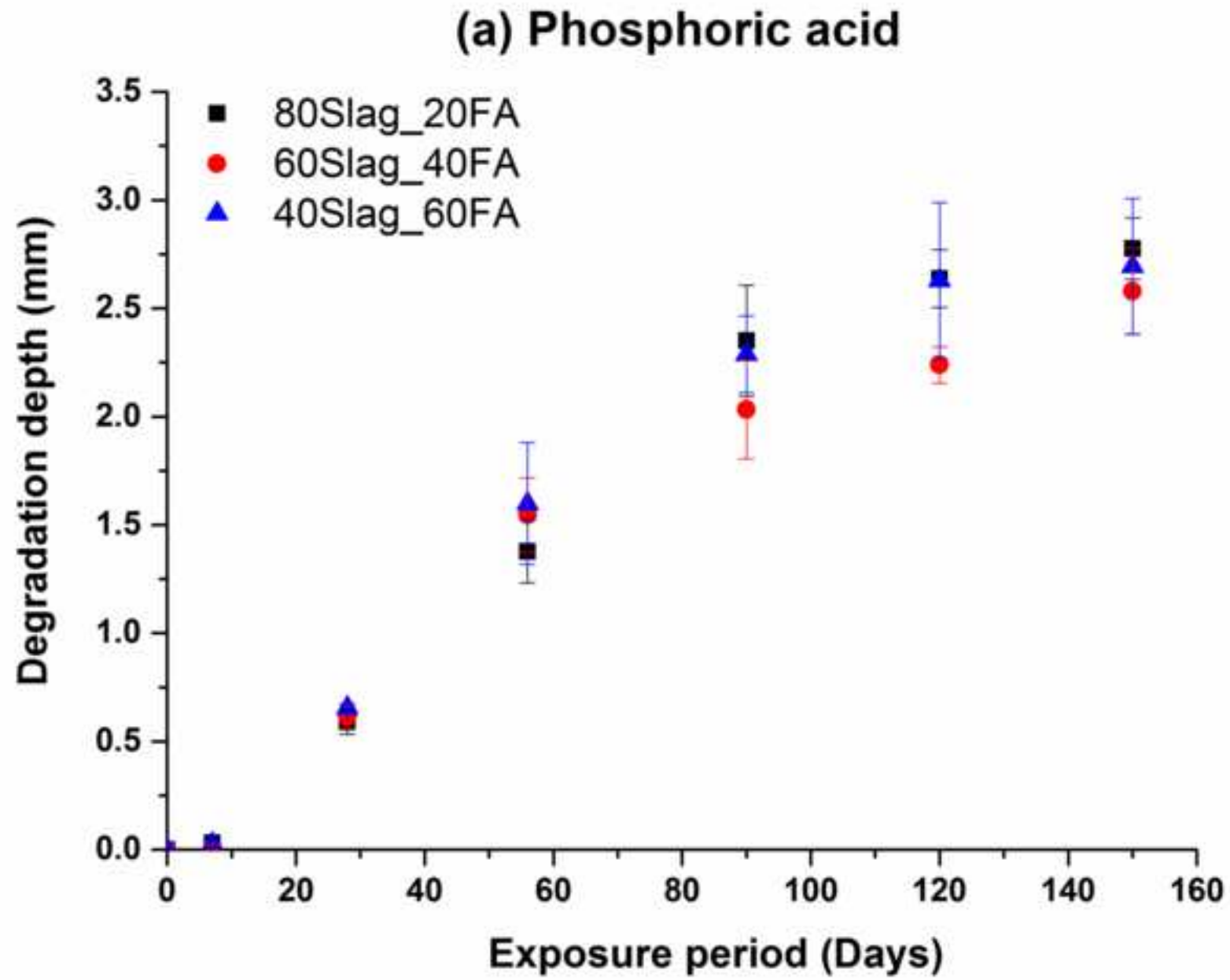
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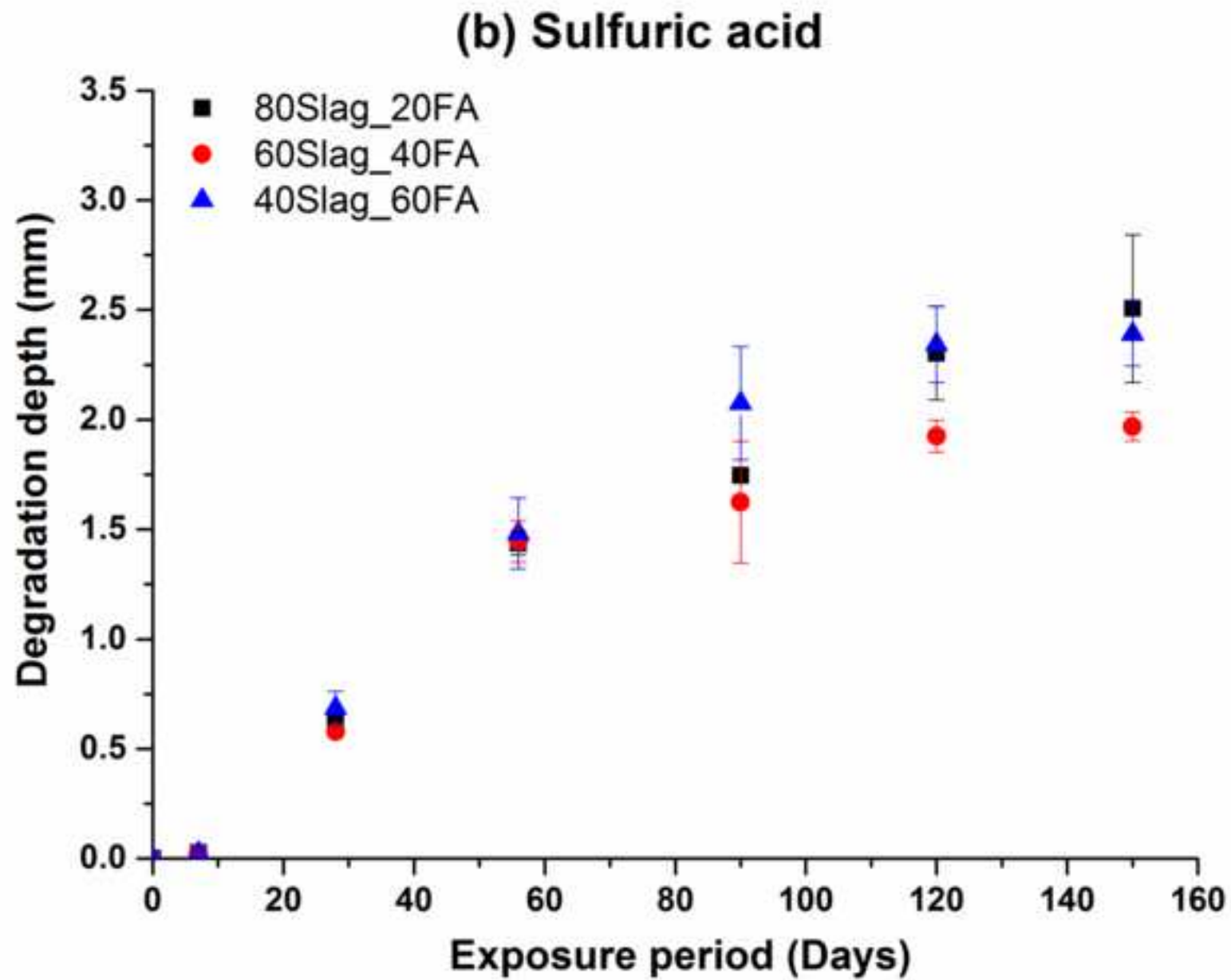
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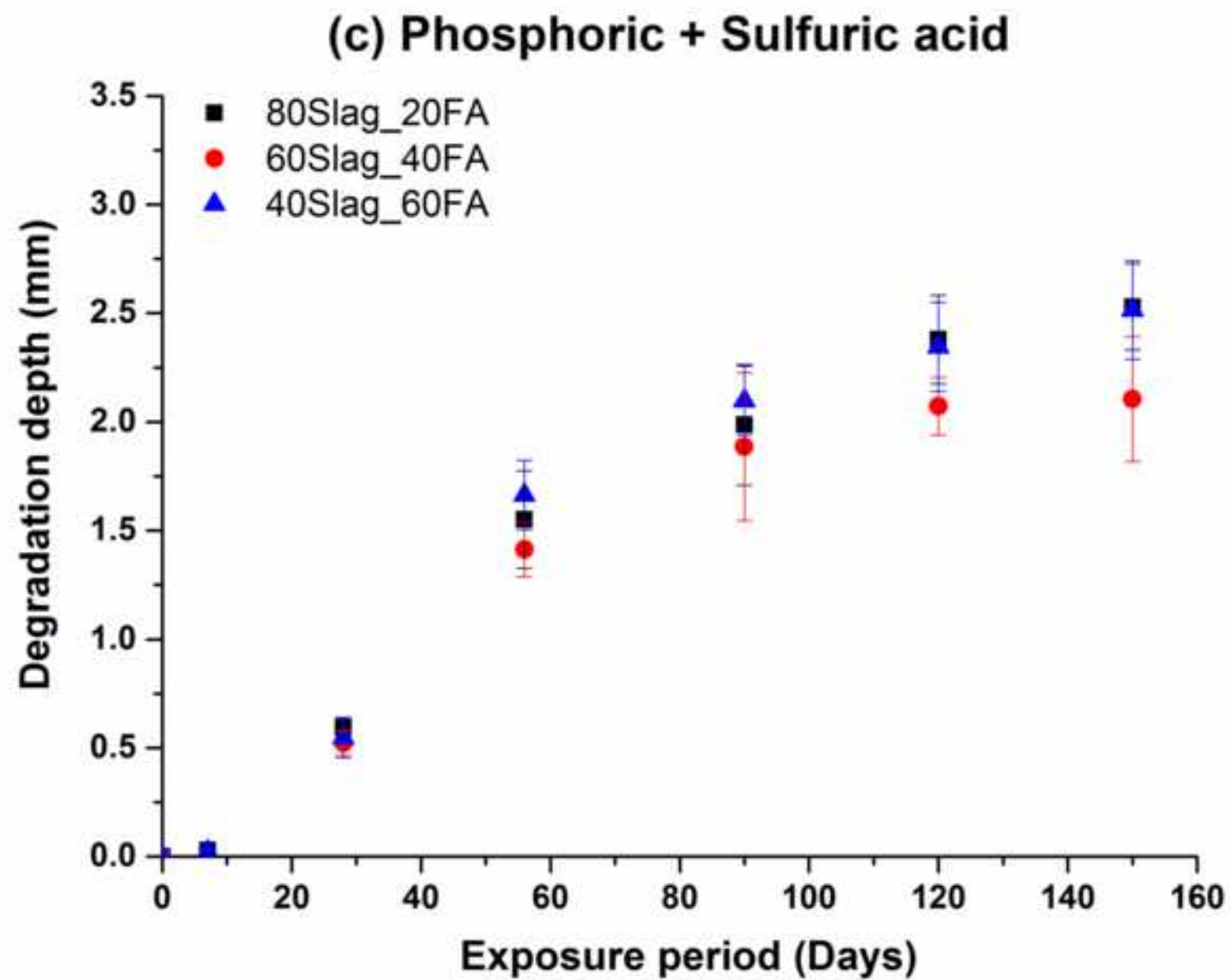


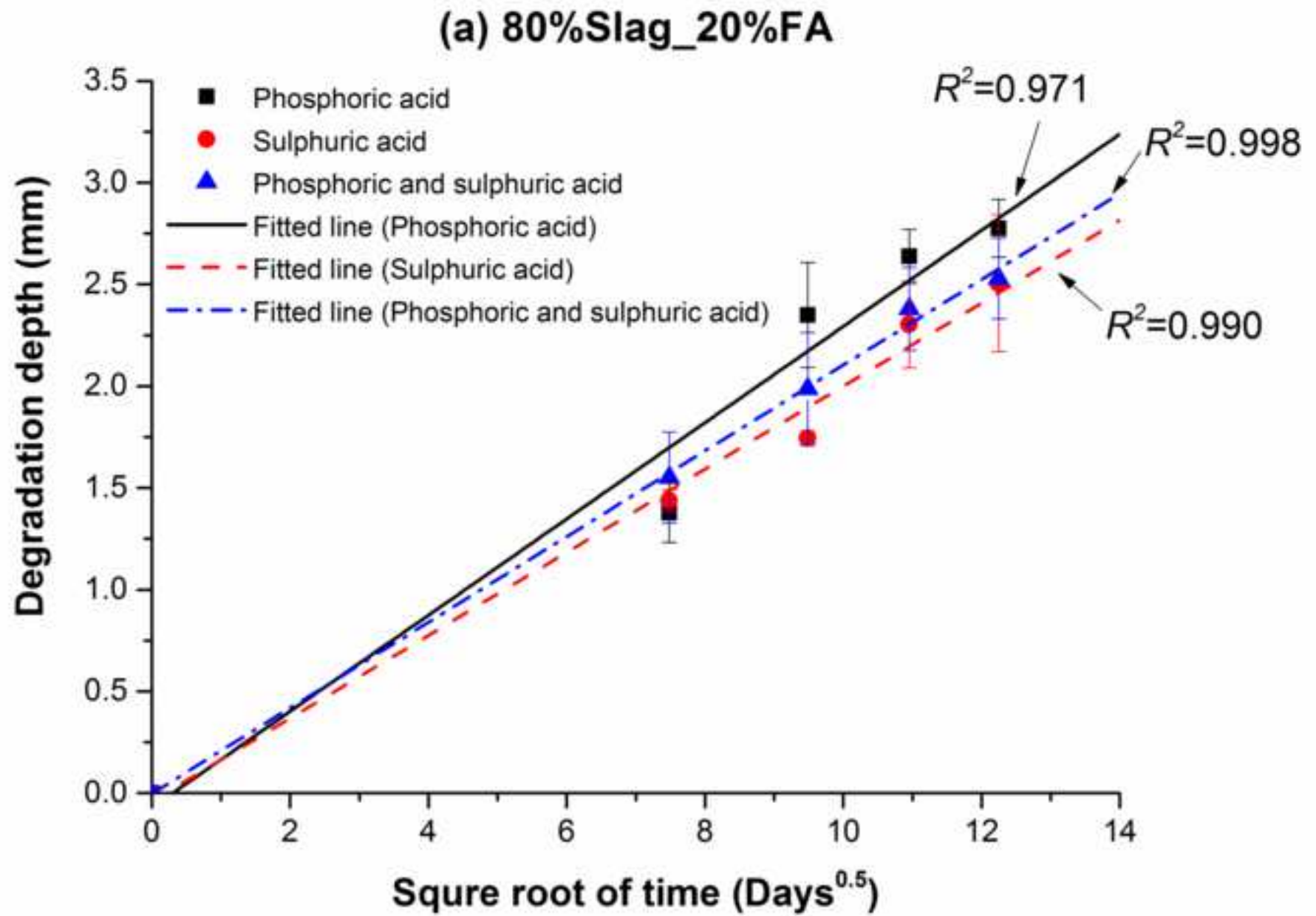


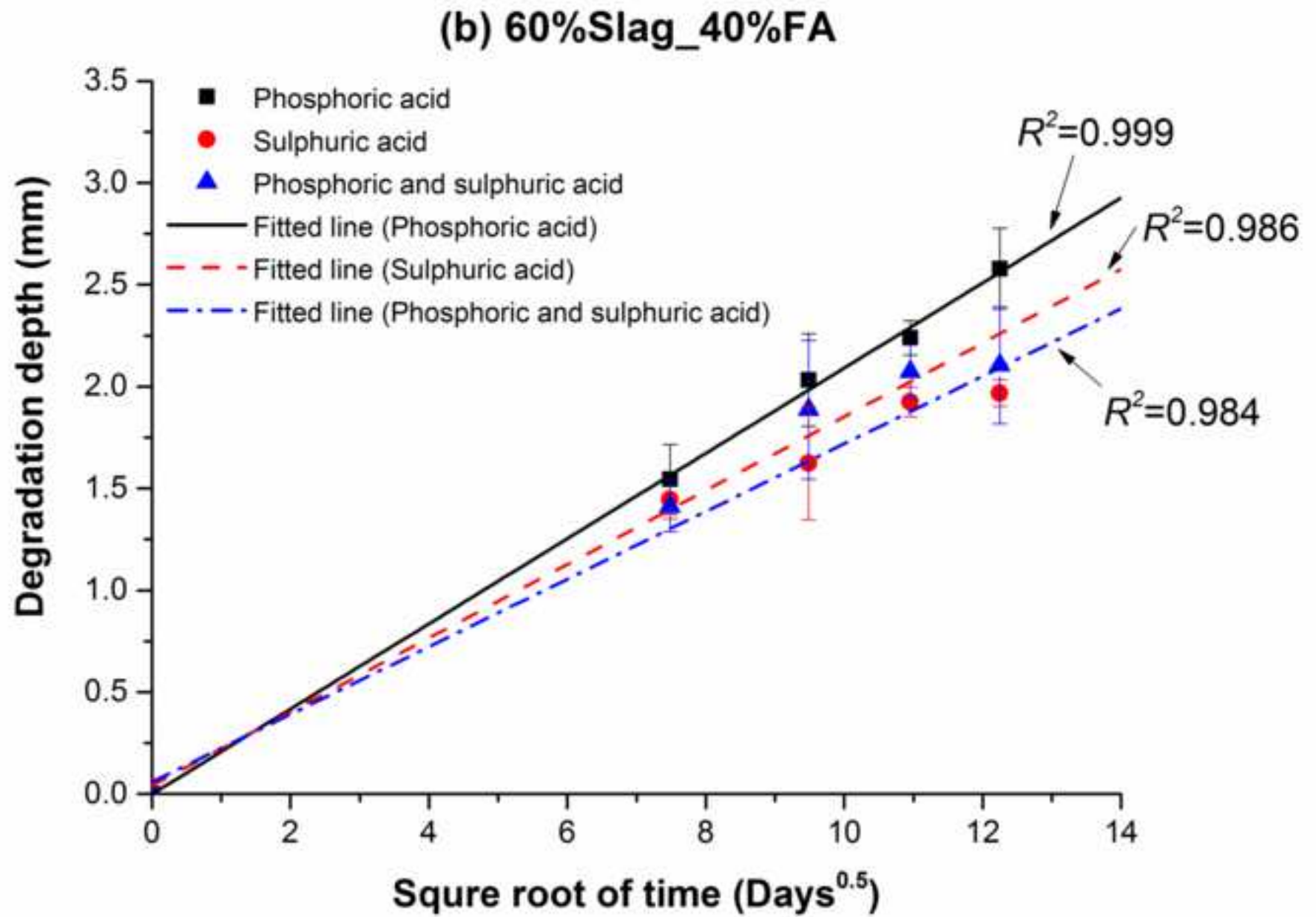
**(a) 805lag\_20FA P+5 (28 days)****(b) 805lag\_20FA P+5 (120 days)**

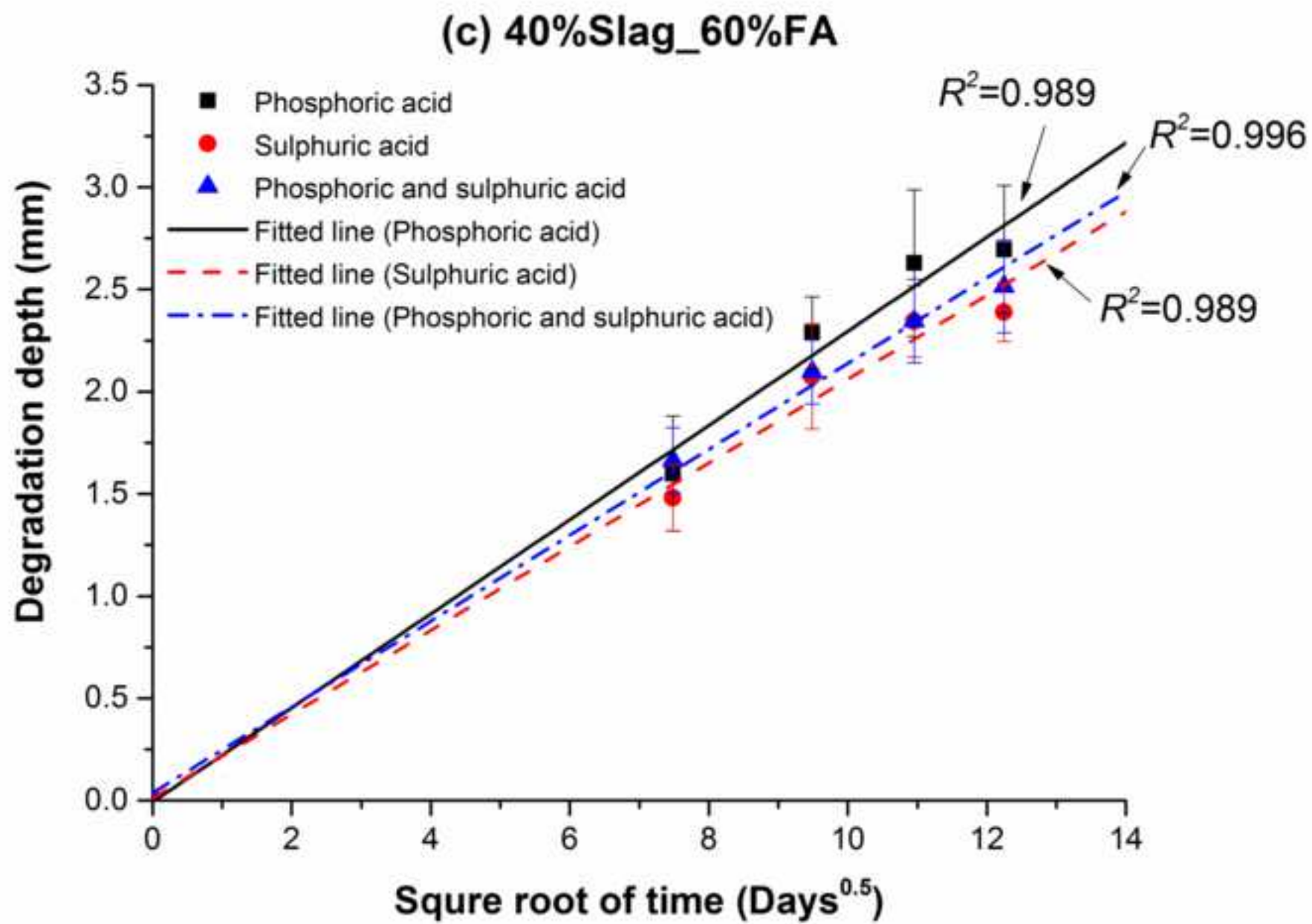








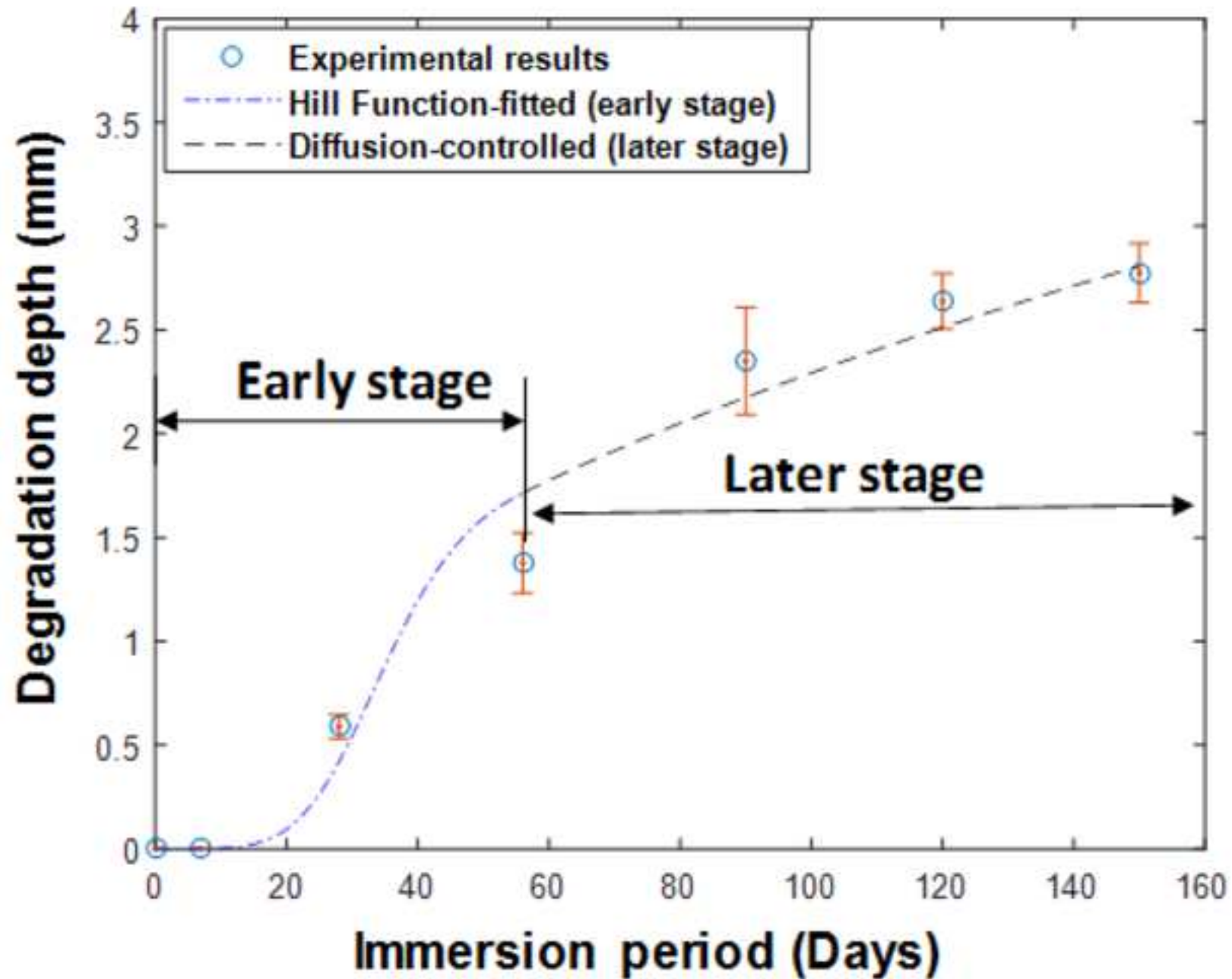


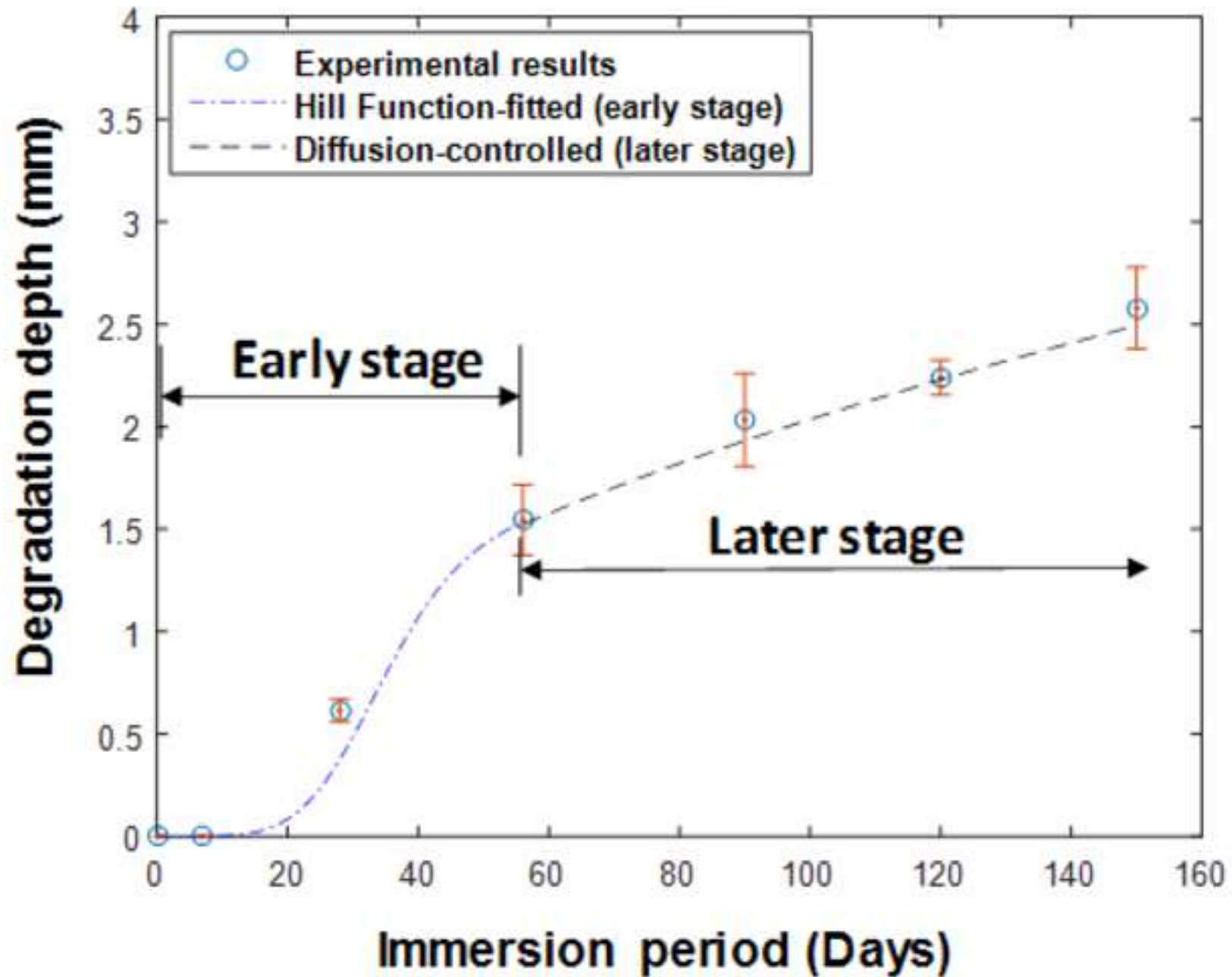


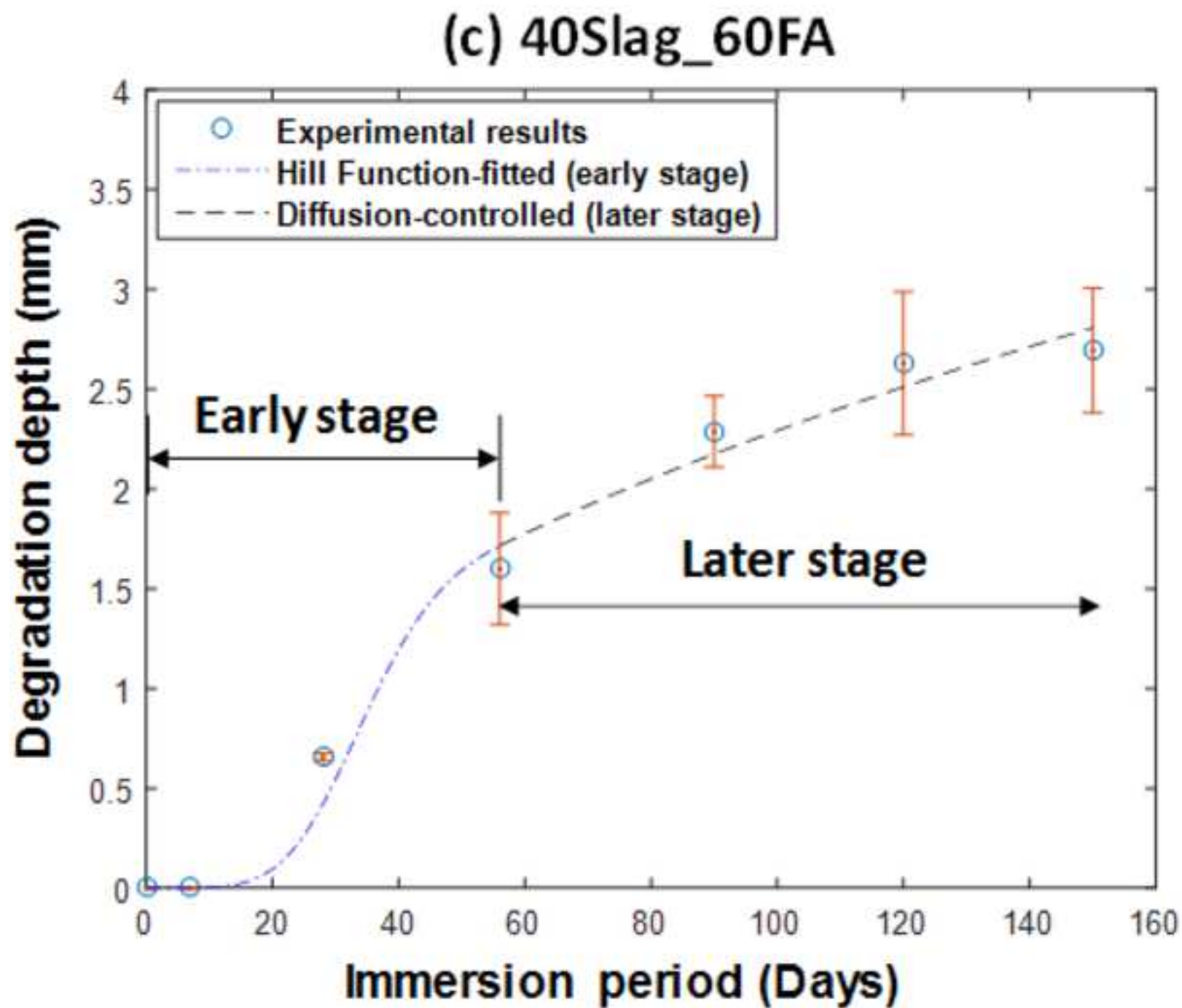


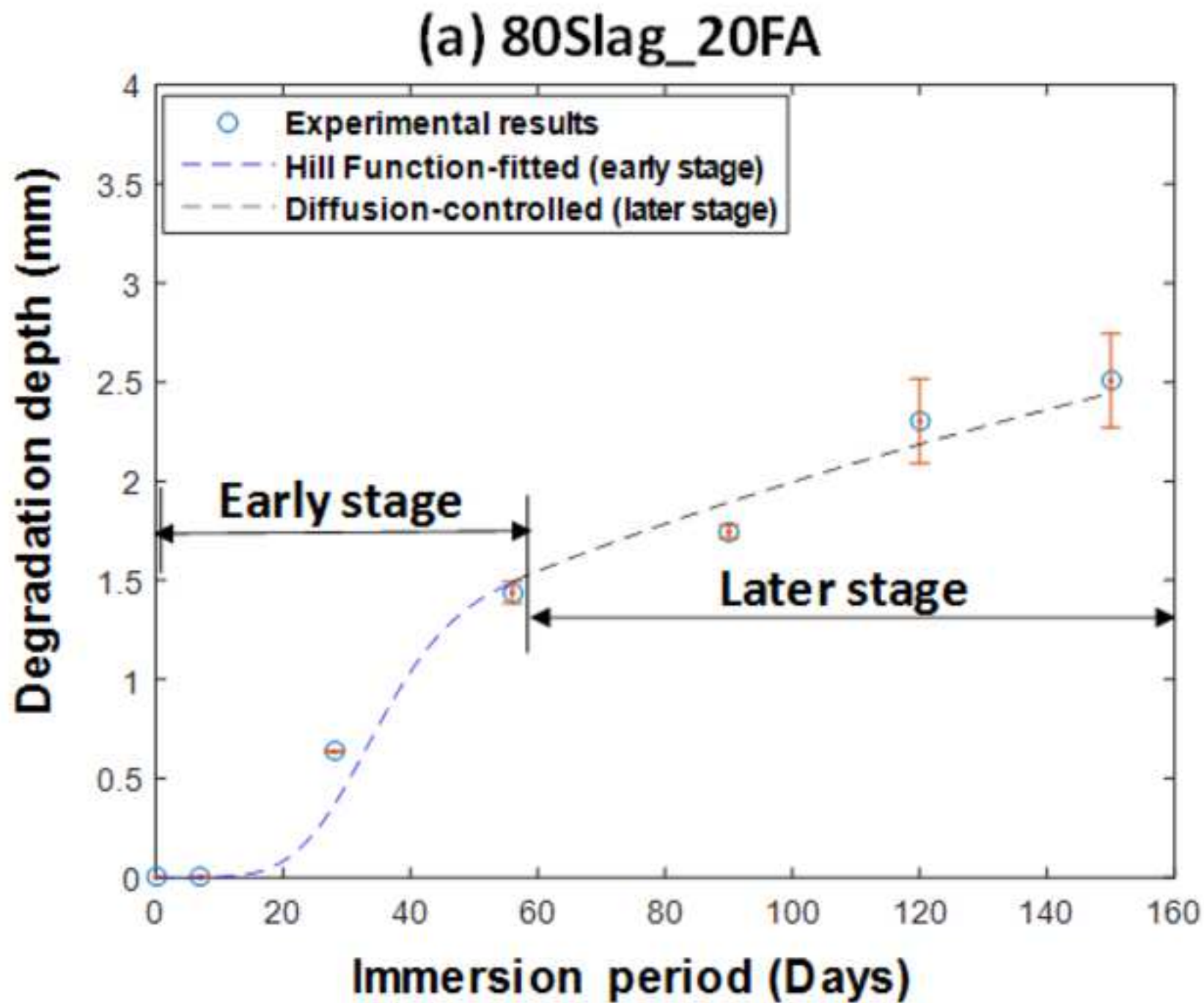
**20 mm**

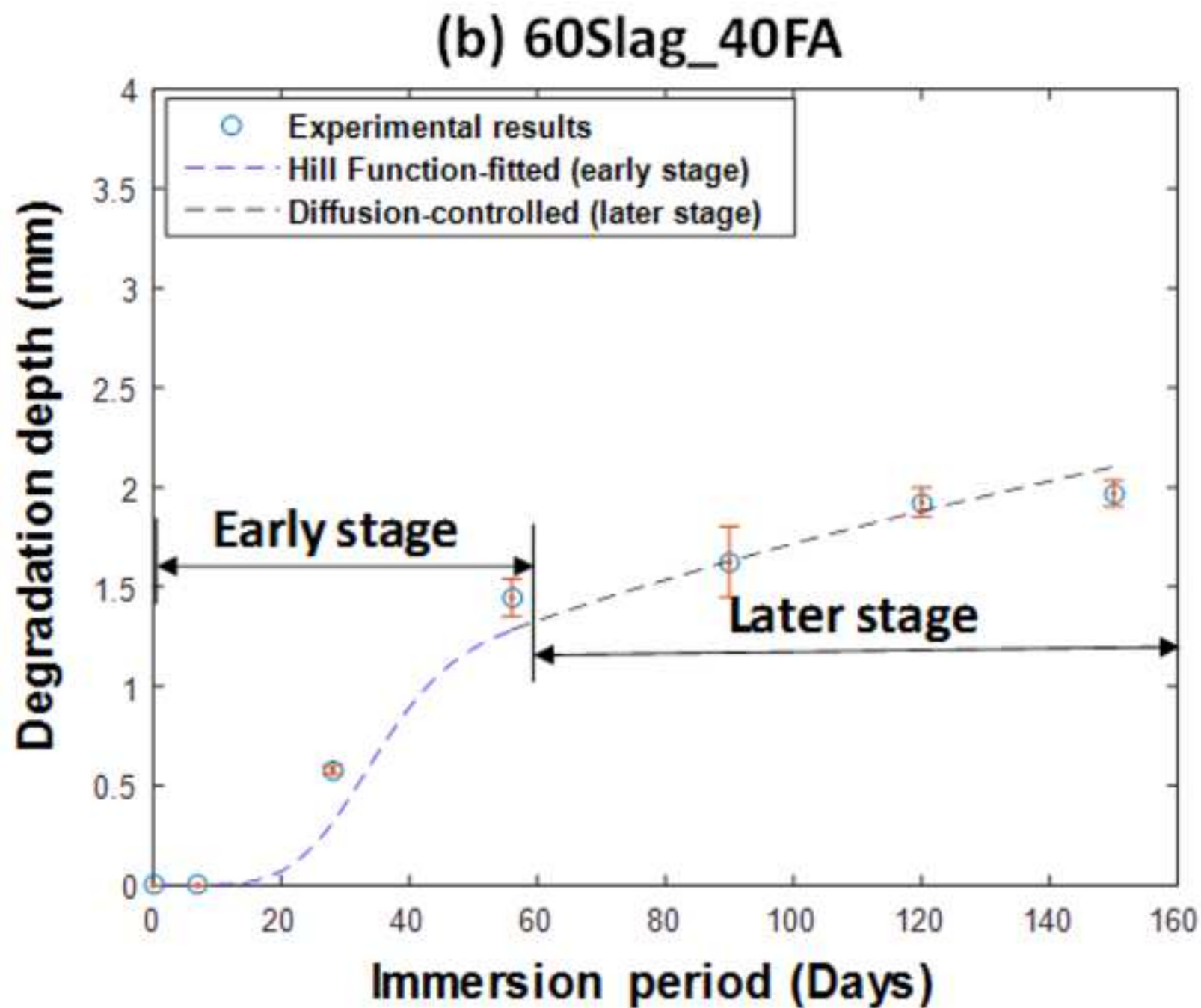
A dimension line with arrows at both ends, indicating a length of 20 mm. The text "20 mm" is centered above the line.

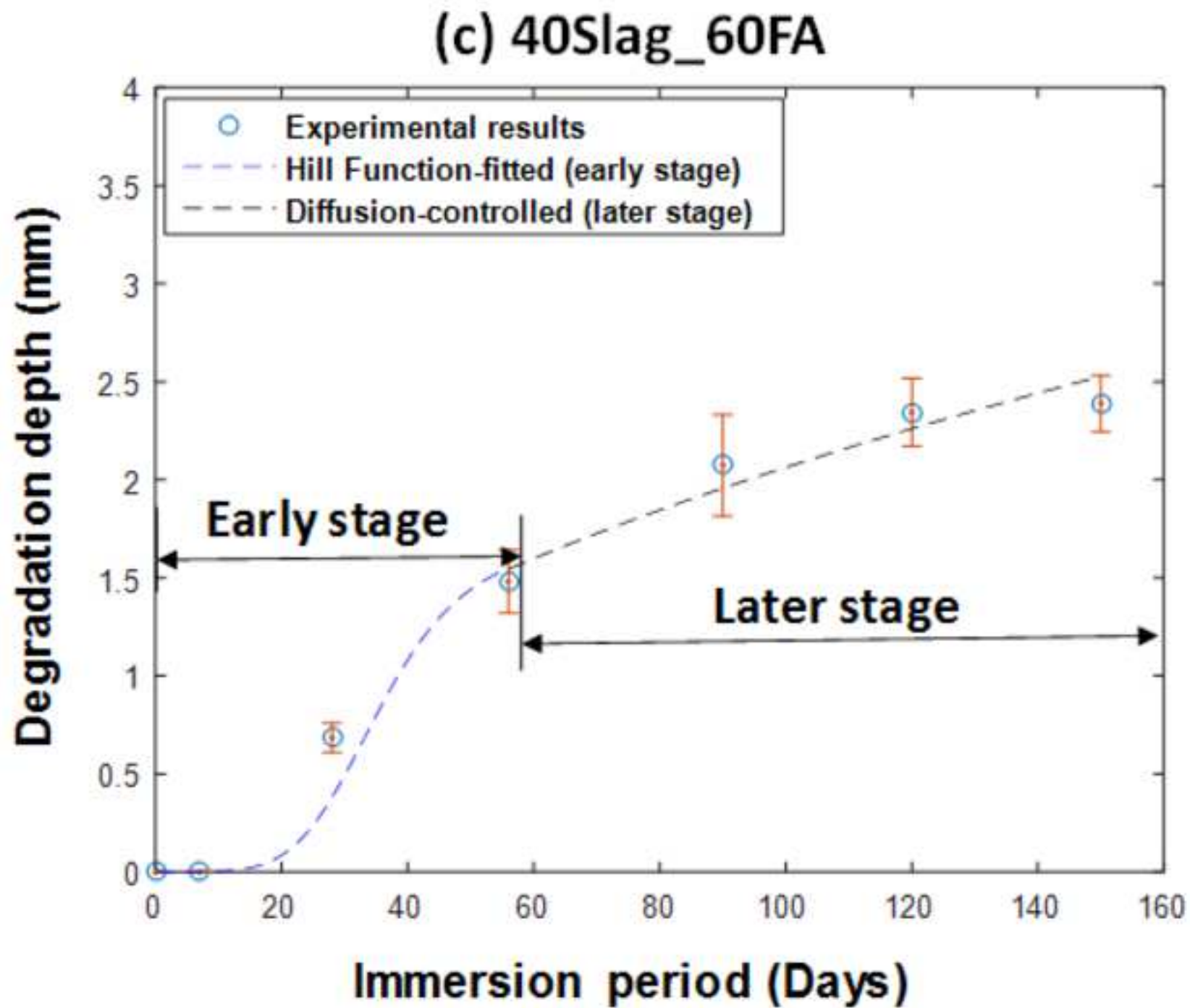
**(a) 80Slag\_20FA**

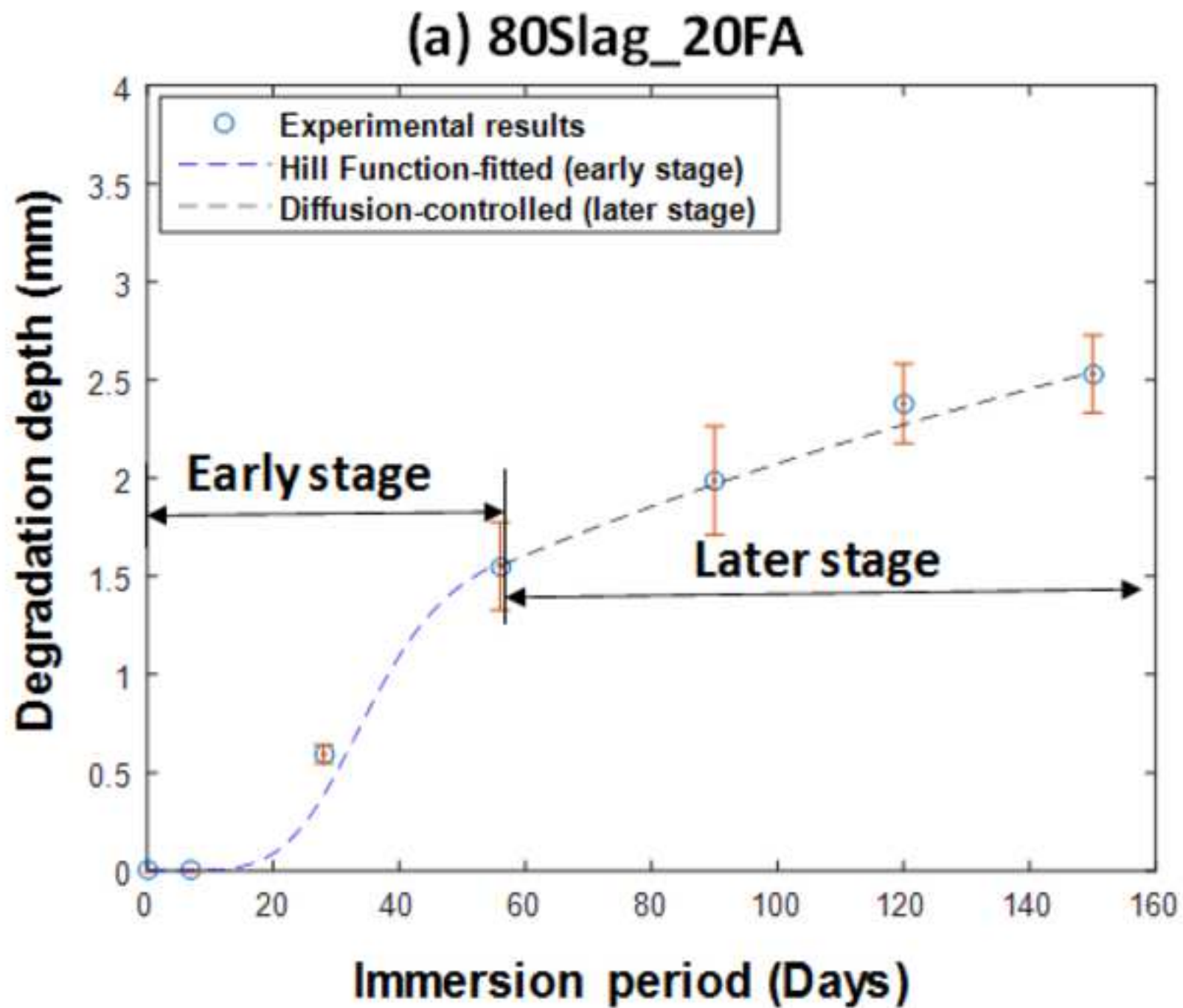
**(b) 60Slag\_40FA**

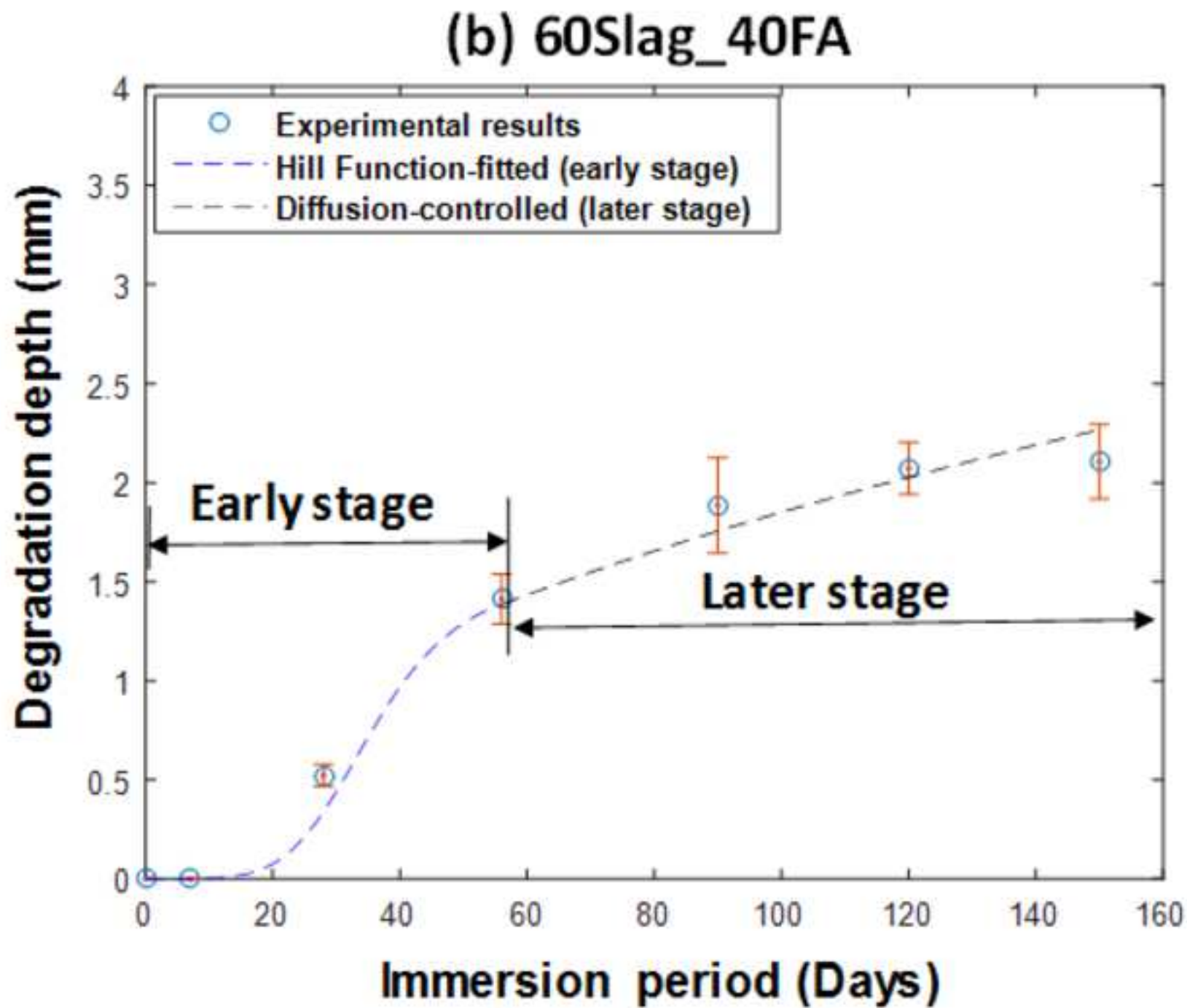












**(c) 40Slag\_60FA**